

Cumulative Indexes of Volumes 43–69: Partially Permuted Title Word Index

- 1,2-Epoxyoctane** 53:B13
1,2-Ethanediol 52:41
1-Butene
 · Acid 64:265
 · Adsorption-Enthalpy 60:147
 · Al₂O₃ 64:265
 · Bronsted-Type 64:265
 · Catalyst 60:147, 64:265
 · Direct-Test 60:147
 · Isomerization 60:147, 64:265
 · Mixed-Oxide 64:265
 · Relationship 64:265
 · Silica-Alumina 60:147
 · Silicon-Dioxide 64:265
 · Site 64:265
 · Solid 64:265
 · Surface-Active 64:265
 · Titanium-Dioxide 64:265
 · Zirconium-Dioxide 64:265
1-Propanol 51:129
2-Methoxyethanol 52:41
2-Propyl-Pentane-Nitrile 59:121
2nd-Virial-Coefficient
 · Dependence 56:73
 · Determination 47:113
 · Pressure-Measurement 47:113
 · Temperature 56:73
4-Cyanopyridine 56:B49
4-Picoline 56:B49
A-Priori-Information 56:167
A-Si-H 58:1
Abrasion 63:85
Absence 43:41
Absorption
 · Activity 57:1
 · Aqueous 60:123
 · Bubbling 67:131
 · Calcium-Sulfite 66:123
 · Capacity 59:243
 · Carbon-Dioxide 67:131
 · Carbon-Monoxide 59:243
 · Chemical-Reaction 57:1, 58:151
 · Column-Plate 57:1
 · Cosorb-Solution 59:243
 · Decomposition 43:75
 · Flat-Fluidized-Photoreactor 45:1
 · Influence 67:131
 · Ionic-Bubble 57:1
 · Light-Energy 45:1
 · Limestone 51:99
 · Marangoni-Instability 58:151
 · Methyl-diethanolamine 60:123
 · Model 66:123
 · Nitrogen-Oxide 43:75
 · Nitrous-Acid-Formation 43:75
 · Oxygen 66:123
 · Polyhydroxyalcohol 60:123
 · Rate 59:243
 · Slurry 51:99
 · Solution 66:123
 · Stirred-Tank 67:131
 · Sulfur-Dioxide 51:99
 · Surfactant 67:131
Accelerated-Film-Technique 67:65
Accumulation-Effect 59:281
Acentric-Factor 66:35
Acetate-Ion 51:1
Acetifier
 · Batch 62:183
 · Closed-System 62:183, 65:201
 · Computer-Simulation 62:183, 65:201
 · Industrial 62:183, 65:201
 · Operating-Condition 62:183, 65:201
 · Operation 62:183
 · Optimum 62:183, 65:201
 · Semi-Continuous-Operation 65:201
Acetobacter-Aceti 54:B15
Acid
 · 1-Butene 64:265
 · Al₂O₃ 64:265
 · Bone-Powder 67:55
 · Bronsted-Type 64:265
 · Catalyst 64:265
 · Correlation 63:189
 · Elaboration 67:55
 · Equivalent 63:189
 · Estimation 63:189
 · Experimental-Study 67:55
 · Gelatin-Production 67:55
 · Humic-Acid 63:189
 · Isomerization 64:265
 · Kinetics 67:55
 · Mixed-Oxide 64:265
 · Modeling 67:55
 · Overall-Scheme 67:55
 · Process 67:55
 · Regenerated 63:189
 · Relationship 64:265
 · Silicon-Dioxide 64:265
 · Site 64:265
 · Solid 64:265
 · Surface-Active 64:265
 · Titanium-Dioxide 64:265
 · Zirconium-Dioxide 64:265
Acidic 60:63
Acidity 64:255
Acrylamide 46:B43
Acrylic 65:249
Acrylonitrile 46:B43
Activated
 · Adsorption 59:205
 · Aqueous-Solution 52:37
 · Carbon 52:37, 59:205
 · Equilibrium 59:205
 · Removal 52:37
 · Stochastic-Model 59:205
 · Tannic-Acid 52:37
Activated-Carbon-Column 58:239
Activated-Sludge 45:B57
Active 53:13
Active-Carbon 44:43
Activity
 · Absorption 57:1
 · Anaerobic-Granule 56:B23
 · Catalyst 52:115
 · Characterization 52:115
 · Chemical-Reaction 57:1
 · Cobalt 52:115
 · Column-Plate 57:1
 · Heavy-Oil-Processing 46:61
 · Hydrocarbon 52:115
 · Impact 56:B23
 · Ionic-Bubble 57:1
 · Organic-Loading 56:B23
 · Oxidation 52:115
 · Oxide 52:115
 · Reactor-Hydrodynamics 56:B23
 · Selectivity 46:61
 · Size 56:B23
 · Stable-Catalyst 46:61
 · Total 52:115
Activity-Coefficient 46:35
Adapted 44:B31
Adaptive 63:65
Addition 49:107
Adsorbent
 · Adsorption-Kinetics 53:147
 · Gravimetric-Determination 53:147
 · Heterogeneity 51:159
 · Influence 53:147
 · Modeling 51:159
 · Particle 53:147
 · Solid-Liquid-Adsorption 51:159
 · Transfer 53:147
Adsorption
 · Activated 59:205
 · Adsorption-Data 65:81
 · Adsorption-Energy 64:85
 · Aqueous-Solution 66:223
 · Basic-Dye 66:223
 · Batch-Stirred-Reactor 58:265
 · Blowdown-Policy 48:173
 · Bunch 66:223
 · Calcium-Alginate 65:81
 · Carbon 59:205
 · Cephalosporin-C 52:B71
 · Change 62:73
 · Charge 62:73
 · Column 65:81
 · Component 64:85
 · Copper 65:81
 · Copper(II) 58:265
 · Correlation 64:85
 · Cracking 54:115
 · Deactivation 54:115
 · Dialysis 62:73
 · Different 66:223
 · Diffusion 54:115
 · Dipeptide 49:B41
 · Dynamic-Approach 65:81
 · Effect 49:B41
 · Equilibrium 48:173, 59:205
 · Equilibrium-Isotherms 46:B93
 · Evaluation 65:81
 · Experimental-Set-Up 49:11

- Generalized-Langmuir-Freundlich-Isotherm-Equation 64:85
- Hexane 54:115
- Immobilization 54:B1
- Immobilized 65:81
- Ion 62:73
- Kinetics 49:11
- Mass-Transfer 54:B1
- Matrix 54:B1
- Membrane 62:73
- Mixed-Gas 64:85
- Modeling 52:B71
- Modified 52:B71
- Moment-Analysis 65:81
- Mordenite 54:115
- Nickel 58:265
- Nonlinear-Analysis 48:173
- Nonlinear-Kinetics 49:B41
- Oligomerization 54:115
- Packed-Bed 65:81
- Palm-Fruit 66:223
- Particle 66:223
- Permeability 62:73
- Pressure-Swing 48:173
- Propene 54:115
- Protein 62:73
- Removal 66:223
- Resin 52:B71
- Reverse-Phase-Column 49:B41
- Reversed-Displacement-Chromatography 46:B93
- Rhizopus-Arrhizus 58:265
- Separation 48:173, 49:B41
- Series-Analysis 58:265
- Solid-Surface 64:85
- Stimulus-Response 65:81
- Stirred-Tank 52:B71
- Stochastic-Model 59:205
- Technique 65:81
- Thermal-Measurement 49:11
- Unfavorable 46:B93
- Zeolite 54:115
- Zoogloea-Ramigera 65:81
- Adsorption-Data** 65:81
- Adsorption-Energy** 64:85
- Adsorption-Enthalpy** 60:147
- Adsorption-Isotherm** 60:181
- Adsorption-Kinetics** 53:147
- Adsorption-Model** 58:21
- Adsorption-Process**
 - Analysis 60:81
 - Apparent 60:81
 - Comparison 56:59
 - Countercurrent 56:59
 - Criterion 60:81
 - Diffusion 60:81
 - Diffusion-Convection 60:81
 - Driving-Force 60:81
 - Equivalence 60:81
 - Extended-Linear-Model 60:81
 - Large-Pore 60:81
 - Material 60:81
 - Modeling 56:59
 - Simulation 56:59
 - Strategy 56:59
- Aerated**
 - Bioreactor 59:187
 - Bubble 59:187
 - Determination 59:187
 - Entrainment 59:187
 - Fermentation 46:B83
 - Heat-Transfer 46:B83
 - Mass-Transfer 59:187
 - Mycelial-System 46:B83
 - Nonaerated 46:B83
 - Parameter 59:187
 - Stirred-Tank-Reactor 46:B83
 - Surface 59:187
- Aeration** 58:59
- Aerobic-Mixed-Culture** 53:B47
- Aerobic-Trickling-Filter** 46:B59
- Aerogel** 64:273
- Aerosol**
 - Characterization 64:239
 - Copper-Modified 64:239
 - Cylindrical-Collector 58:109
 - Decomposition 64:239
 - Deposition 58:109
 - Fibrous-Particle 58:109
 - Flexible 58:109
 - High-Temperature 64:239
 - Higher-Alcohol 64:239
 - Process 64:239
 - Stiff 58:109
 - Synthesis 64:239
 - Theoretical-Study 58:109
 - Zinc-Chromite 64:239
- Affecting** 61:13
- Ag(I)/Ag(II)** 56:1
- Agging** 66:51
- Agitated**
 - Breakage 62:23
 - Flocc 62:23
 - Liquid 62:23
 - Multiple-Turbine 63:53
 - Rotating-Mixer 62:23
 - Suspension 62:23
 - Tank 63:53
 - Transitional-Mixing 63:53
 - Vibrating-Mixer 62:23
- Agitated-Reactor** 47:33
- Agitated-Slurry** 54:199
- Agitator**
 - Gas-Liquid-Dispersion 61:83
 - Helical 52:9
 - Highly-Viscous-Fluid 52:9
 - Hydrodynamic 61:83
 - Mixing-Vessel 61:83
 - Modified-Rushton-Turbine 61:83
 - Power-Consumption 52:9
 - Pseudoplastic-Fluid 52:9
 - Ribbon 52:9
 - Screw 52:9
 - Transfer-Process 61:83
- Air-Non-Newtonian-Liquid-Flow** 59:277
- Air-Water-Flow** 66:131
- Air-Water-Pipe-Flow** 48:197
- Air-Water-System** 53:167
- Air-Core** 56:135
- Airlift-Bioreactor**
 - Animal-Cell 57:B31
 - Gas-Liquid-Circulation 56:B101
 - Liquid-Phase 57:B31
 - Local-Flow-Behavior 57:B31
 - Mass-Transfer 56:B101
 - Non-Newtonian-Fluid 56:B101
 - Potential 57:B31
 - Suspension-Culture 57:B31
 - Viscous 56:B101
- Airlift-Column** 62:35
- Airlift-Fluidized-Bed**
 - Design 49:89, 55:143, 55:145
 - Mass-Transfer 49:89, 55:143, 55:145
 - Modeling 49:89, 55:143, 55:145
 - Operational 55:143
 - Operational-Parameter 49:89, 55:145
 - Optimization 49:89, 55:143, 55:145
 - Parameter 55:143
 - Respect 55:143
- Airlift-Reactors** 65:263
- Airlift-Slurry-Reactor** 62:223
- Airlift-Tube-Reactor** 68:29
- Alcohol**
 - Addition 49:107
 - Aliphatic-Ether 43:25
 - Batch 48:B15
 - Bubble-Column 50:47
 - Bubble-Rise-Velocity 50:47
 - Bubble-Size 50:47
 - Carbon-Dioxide 43:25
 - Concentration 50:47
 - Cryogenic-Liquid 43:25
 - Design-Parameter 49:107
 - Ethanol 48:B15
 - Evaporative-Loss 48:B15
 - Fermentation 48:B15
 - Gas-Hold-Up 50:47
 - Mechanically-Agitated-Three-Phase-Reactor 49:107
 - Modeling 48:B15
 - Nitrous-Oxide 43:25
 - Organic-Acid 50:47
 - Potassium-Chloride 50:47
 - Solubility 43:25
 - Water 43:25
- Alcohol-Solution** 60:117
- Alcoholic-Solution** 55:53
- Alga** 47:B23
- Alginate** 56:B9
- Alginate-Bead** 55:B29
- Algorithm** 65:77
- Aliphatic-Ether** 43:25
- Aliquat-336** 59:303
- Alkaline** 49:B17
- Alkaline-Hydrolysis** 67:19
- Alkane** 66:35
- Alkanolamine** 48:31
- Alkoxide** 55:93
- Alkylation** 53:173
- Alkylhydrazine** 62:97
- Alternative** 45:33
- Alumina** | γ - 57:273
- Al₂O₃** 64:265
- Amberlite**
 - Carrier 58:285
 - Cell 58:285
 - Constant-Interface-Area 58:285
 - Distribution 62:231
 - Equilibrium 62:231
 - Extraction 58:285
 - Kinetics 58:285
 - Mobile 58:285
 - Organic-Solution 62:231
 - Penicillin-G 58:285, 62:231
 - Water 62:231
- Amberlite-252** 66:137
- Amine** 65:47
- Ammonia**
 - Catalysis 67:1
 - Glaserite 67:1
 - Gypsum 67:1
 - Potassium-Sulfate 67:1
 - Production 67:1
 - Stripping 43:B67
 - Sylvinit 67:1
 - Waste-Water-Scrubber-System 43:B67
 - Wetted-Butterfly-Valve 43:B67
- Ammonia-Removal** 66:65
- Amylase** | α -
 - Antibody 65:105
 - Antipeptide 65:105
 - Bacillus-Amyloliquefaciens 65:237
 - Discrimination 65:105
 - Fermentation 44:B51, 65:237
 - High-Temperature 44:B51
 - Isozyme 65:105
 - Oxygen-Transfer 44:B51
 - Rheology 44:B51
 - Starch-Suspension 44:B51
- Amyloglucosidase** 51:B17
- Anaerobic**
 - Comparison 55:B55
 - Control 55:B55
 - Digester 55:B55
 - Dynamics 55:B55
 - Fluidized-Bed-System 54:B25
 - Fruit 54:B25
 - Kinetics 54:B25
 - Mesophilic 55:B55
 - Performance 55:B55
 - Processing 54:B25

- Purification 54:B25
- Sludge 55:B55
- Thermophilic 55:B55
- Waste-Water 54:B25
- Anaerobic-Digestion**
 - Analysis 43:B81
 - Biomass 54:B9
 - Cow-Manure 54:B9
 - Dynamics 43:B81
 - Immobilized 54:B9
 - Kinetics 54:B9
 - Multivariable-Control 43:B81
 - Zeolite 54:B9
- Anaerobic-Granule** 56:B23
- Anaerobic-Stratified-Biofilm** 65:37
- Anaerobic-Treatment** 52:B21
- Anaerobically-Treated** 66:65
- Analogous** 53:89
- Analogy** 61:113
- Analysis**
 - Adsorption-Process 60:81
 - Anaerobic-Digestion 43:B81
 - Apparent 60:81
 - Application 64:1
 - Balance 60:55
 - Ball-Mill 63:141
 - Batch 63:141
 - Batch-Condition 44:B47
 - Bioartificial 44:B81
 - Biofilter 65:55
 - Boiler 64:179
 - Catalyst 47:105
 - Circuit-Design-Principle 59:15
 - Combined 47:105
 - Comparison 65:55
 - Composite 50:59
 - Composite-Phase 50:59
 - Constant 47:105
 - Conversion 47:105
 - Criterion 60:81
 - Cross-Flow-Filtration 60:55
 - Decay 47:105
 - Diffusion 60:81
 - Diffusion-Convection 60:81
 - Driving-Force 60:81
 - Dynamic-Control 68:41
 - Dynamic-Measurement 64:179
 - Dynamics 43:B81
 - Energy-Density 50:59
 - Enzyme-Catalysis 44:B47
 - Equivalence 60:81
 - Exit 47:105
 - Extended-Linear-Model 60:81
 - Fine-Wet-Grinding 63:141
 - Fixed-Bed-Reactor 47:105
 - Flotation 59:15
 - Force 60:55
 - Fractal 64:45
 - Gas-Solids-Injector 45:137
 - Implantable 44:B81
 - Insulin-Production 44:B81
 - Integral-Reactor 63:45
 - Kinetic-Model 63:45
 - Large-Pore 60:81
 - Linear-Transport-Phenomena 64:45
 - Magnetized-Fluidized-Bed 50:59
 - Material 60:81
 - Membrane-Partitioned-Electrode-Reactor 47:25
 - Methanol-to-Gasoline-Process 63:45
 - Model 47:25, 65:55
 - Multivariable-Control 43:B81
 - Natural-Object 64:1
 - Neural-Network 68:41
 - Nonlinear-System 68:41
 - Optimal-Structure 68:41
 - Pancreas 44:B81
 - Partially-Scaled-Fractal 64:1
 - Practical-Approach 64:179
 - Space-Time-Trajectory 47:105
 - Stability 50:59, 68:41
 - Temperature 47:105
 - Theoretical-Study 60:55
 - Transient 60:55
 - Two-Phase-Flow 45:137
- Analytical-Solution** 59:161
- Animal** 62:121
- Animal-Cell** 57:B31
- Anionic-Species** 66:85
- Annular-Swirling-Decay** 52:137
- Anodic-Oxidation** 56:1
- Anomalous-Effect** 63:195
- Anthracene-Oil** 48:191
- Anthraquinone** 63:37
- Antibiotic-Separation** 65:63
- Antibody** 65:105
- Antigen-Coupled** 54:B33
- Antipeptide** 65:105
- Aphron** 65:1
- Apparent** 60:81
- Apparent-Yield** 53:B41
- Apparent-Yield-Stress** 45:B49
- Application**
 - Acentric-Factor 66:35
 - Agitated-Vessel 48:41
 - Alcohol-Solution 60:117
 - Alkane 66:35
 - Analysis 64:1
 - Antibiotic-Separation 65:63
 - Biochemical 62:193
 - Biofilter 65:133
 - Bioreactor 43:B19
 - Calculation 61:27
 - Coefficient 65:63
 - Concentration 65:21
 - Continuous-Stirred-Tank-Reactor 65:63
 - Corresponding-States 66:35
 - Critical-Constant 66:35
 - Denitrification 65:133
 - Design 43:B19
 - Dynamic-Modeling 65:133
 - Electrical-Tomography 56:127
 - Emission-Tomography 56:109
 - Engineering 56:127
 - Enzyme 52:B49
 - Equation-of-State 67:27
 - Estimation 51:77
 - Evaluate 65:63
 - Experimental-Technique 48:41
 - Extension 67:27
 - Fast-Fourier-Transform 51:77
 - Fixed-Bed-Reactor 51:77
 - Flow 62:193
 - Fluidized 66:227
 - Gas-Solid-Reaction 63:79
 - Gas-Bubble 48:41
 - Generalized-Approach 65:133
 - Generalized-Maxwell-Stefan-Equation 57:145
 - Half-Order 63:79
 - High-Pressure 61:27
 - Highly-Viscous-Liquid 48:41
 - Hydrodynamical 62:193
 - Hydrolysis 66:227
 - Interaction 62:193
 - Isotropic-Turbulence 43:B19
 - Kinetic-Parameter 51:77, 65:63
 - Kolmogorov-Theory 43:B19
 - Krone-Doolittle-Equation 60:117
 - Light-Hydrocarbon 57:145
 - Liquid 48:41, 62:193
 - Long-Chain 66:35
 - Lysine-Production 62:207
 - Macedo-Litovitz-Equation 60:117
 - Mass-Transfer 48:41, 65:63
 - Mathematical-Model 43:B19
 - Measurement 48:41
 - Membrane 57:145
 - Methyl-Acetate 66:227
 - Mini-Hydrocyclone 65:21
 - Model 61:27, 63:79
 - Moving-Boundary-Problem 63:79
 - Natural-Object 64:1
 - Near-Critical-Region 67:27
 - Neural-Network 62:207
 - Obstacle 52:B49
 - Opportunity 52:B49
 - Partially-Scaled-Fractal 64:1
 - Particle 62:193
 - Patel-Teja-Equation 67:27
 - Permeation 57:145
 - Process 56:109, 56:127
 - Reaction 63:79
 - Reaction-Distillation-Column 66:227
 - Redox-Potential 49:73
 - Reducing-Agent 49:73
 - Selection 49:73
 - Separation 57:145
 - Silicalite-1 57:145
 - Simulation 65:133
 - Suitable 66:35
 - Suspension 65:21
 - Technique 56:127
 - Three-Parameter 67:27
 - Triglyceride 60:117
 - Vapor-Liquid-Equilibrium 61:27
 - Vat-Dye 49:73
 - Viscosity 60:117
 - Volume 63:79
 - Waste-Treatment 52:B49
 - Waste-Water 65:133
 - Wong-Sandler-Mixing-Rule 67:27
 - Yeast 65:21
- Application-Time** 62:155
- Applied**
 - Bioreactor 51:B35
 - Calculation 48:111
 - Control 51:B35
 - Expert-System 51:B35
 - Industrial-Scale 51:B35
 - Semiempirical-Equation-of-State 48:111
 - Vapor-Liquid-Equilibrium 48:111
- Approximate** 59:161
- Approximate-Method** 59:293
- Aqueous**
 - Absorption 60:123
 - Decontamination 57:53
 - Dispersion 67:97
 - Effluent 57:53
 - Freezing 57:53
 - Influence 67:97
 - Methyl-diethanolamine 60:123
 - pH 67:97
 - Polyhydroxylalcohol 60:123
 - Rheology 67:97
 - Salt-Polyethylene-Glycol-System 46:B31
 - Stability 67:97
 - Temperature 67:97
 - Titanium-Dioxide 67:97
 - Two-Phase-Extraction 46:B31
 - Ultrasonic-Bath 57:53
- Aqueous-Phase** 59:297
- Aqueous-Solution**
 - Acetate-Ion 51:1
 - Activated 52:37
 - Adsorption 66:223
 - Basic-Dye 66:223
 - Bubble-Formation 49:65
 - Bunch 66:223
 - Carbon 52:37
 - Carbon-Dioxide 46:1
 - Chemical-Reaction 46:1
 - Closely-Spaced 49:65
 - Desorption 46:1
 - Different 66:223
 - Electrodialysis 51:1
 - Nitrate-Ion 51:1

- Orifice 49:65
- Palm Fruit 66:223
- Particle 66:223
- Permselectivity 51:1
- Potassium-Carbonate 46:1
- Prediction 51:1
- Removal 52:37, 66:223
- System 46:1
- Tannic-Acid 52:37
- Arbitrary** 56:33
- Arbitrary-Parameter** 48:183
- ARMAX** 50:B45
- Arrangement** 55:15
- Artificial** 64:63
- Ash-Liberation** 59:23
- Aspergillus-Niger**
 - Citric-Acid-Production 62:215
 - Determination 62:215
 - Free- β -Galactosidase 52:B1
 - Hydrolysis 52:B1
 - Immobilized- β -Galactosidase 52:B1
 - Lactose 52:B1
 - Maintenance-Coefficient 62:215
 - Modeling 52:B1
 - Simulation 52:B1
 - Yield 62:215
- Assessment**
 - Batch 59:143
 - Calorimetry 59:143
 - Cooling-Policy 59:143
 - Crystal-Growth-Rate-Function 55:69
 - Crystallization 59:143
 - Crystallization-Kinetics-Data 55:69
 - Model 55:69
 - Seeding 59:143
 - Size-Dependent 55:69
 - System 55:69
- Atmospheric-Condition** 48:197
- Attainable-Region** 54:175
- Autocatalytic-Reaction** 66:231
- Autoclave-Reactor** 67:175
- Autoinductive** 61:139
- Automobile** 53:47
- Autothermal-Reactor-System** 62:103
- Axial** 44:B57
- Axial-Dispersion**
 - Different 52:63
 - Fiber 58:245
 - Fixed-Bed 52:63
 - Flow-Direction 64:345
 - Gas-Liquid-Solid-Fluidized-Bed 44:51, 44:52
 - Gas-Solid-Cocurrent-Downflow-System 64:345
 - Gas-Solid-Cocurrent-Upflow-System 64:345
 - Liquid 44:51, 44:52
 - Liquid-Flow 52:63
 - Metallic-Foam 52:63
 - Packed 52:63
 - Packed-Bed 58:245
 - Reticulated 52:63
 - Solid 64:345
 - Structure 52:63
- Axial-Dispersion-Coefficient** 49:17
- Axial-Dispersion-with-Reaction** 45:49
- Axial-Mixing**
 - Fine-Particle 47:47
 - Fluidized-Bed 44:1, 47:47
 - Solid 44:1
 - Turbulent 44:1
- Axially-Agitated** 67:139
- Azeotropic-Distillation** 43:59
- Azeotropic-Mixture** 54:87
- Bacillus-Amyloliquefaciens** 65:237
- Bacillus-Macerans-314** 61:247
- Bacillus-Subtilis** 59:303
- Back-Extraction** 59:297
- Backmixing** 48:71
- Backmixing-Effect** 44:B57
- Backward-Extraction** 60:63
- Bacterial** 54:207
- Bacterial-Adaptation** 56:B115
- Bacterial-Aggregate** 44:B1
- Baffle**
 - Agitated-Vessel 58:135
 - Behavior 59:33
 - Equipped 58:135
 - Flexible 59:33
 - Flotation-Column 59:33
 - Heat-Transfer 58:135
 - Jacketed 58:135
 - Nonstandard 58:135
 - Simulation 59:33
- Baffled** 66:1
- Balance** 60:55
- Balancing** 65:123
- Ball-Mill** 63:141
- Barium-Chloride** 49:167
- Basic-Dye** 66:223
- Batch**
 - Acetifier 62:183
 - Alcohol 48:B15
 - Analysis 63:141
 - Assessment 59:143
 - Bacterial 54:207
 - Ball-Mill 63:141
 - Biosynthesis 51:B43
 - Calorimetry 59:143
 - Chemical-Plant 44:167
 - Chemical-Reaction 52:107
 - Closed-System 62:183
 - Comparison 65:195
 - Complex-Selective-Medium 52:B35
 - Computer-Simulation 62:183
 - Continuous 54:207
 - Continuous-Chromatography 51:B43
 - Cooling-Policy 59:143
 - Crystallization 59:143
 - Dextran 51:B43
 - Dextranucrase 51:B43
 - Enzymatic-Hydrolysis 65:187, 65:195
 - Enzymatic-Kinetics 65:187
 - Ethanol 48:B15
 - Evaporative-Loss 48:B15
 - Fermentation 48:B15, 52:B35
 - Fermenter 51:B57
 - Fine-Wet-Grinding 63:141
 - Flow 52:107
 - Glyceraldehyde-3-Phosphate-Dehydrogenase 52:B35
 - Hydrolysis 65:187
 - Industrial 62:183
 - Large-Scale 51:B43
 - Leaching 54:207
 - Leuconostoc-Mesenteriodes 51:B43
 - Mathematical-Modeling 54:207
 - Mixing 51:B57
 - Modeling 48:B15, 52:B35, 61:157
 - Multipurpose 44:167
 - Operating-Condition 62:183
 - Operation 62:183
 - Optimum 62:183
 - Performance 65:195
 - Production 52:B35
 - Protein 65:187, 65:195
 - Pulsatile 52:107
 - Purification 51:B43
 - Recombinant-Escherichia-Coli 52:B35
 - Scheduling 44:167
 - Seeding 59:143
 - Stirred-Reactor 65:187, 65:195
 - Stirred-Tank-Reactor 52:107
 - Torus-Reactor 65:195
 - Ultrafiltration 61:157
 - Unstirred 51:B57
 - Wheat 65:187, 65:195
- Batch-Condition** 44:B47
- Batch-Culture** 44:B69
- Batch-Distillation** 54:95
- Batch-Packed** 54:51
- Batch-Process** 63:65
- Batch-Reactor** 59:229
- Batch-Stirred-Reactor** 58:265
- Bed** 51:B17
- Behavior**
 - Baffle 59:33
 - Bubble-Column 53:115
 - Catalyst 43:11
 - Change 43:11
 - Consecutive-Reaction 46:91
 - Deactivation 43:11
 - Flexible 59:33
 - Flotation-Column 59:33
 - Fluidized-Bed 50:87
 - High-Throughput 53:115
 - Liquid 50:87
 - Mixture 43:11
 - Model 43:11
 - Monosized-Crystal 50:87
 - Nonuniform-Catalyst 46:91
 - Pore-Size 43:11
 - Radial-Profile 53:115
 - Reaction 43:11
 - Selectivity 46:91
 - Simulation 59:33
 - Single-Pellet 43:11
 - Sodium-Perborate 50:87
 - Support 43:11
 - Supported-Catalyst 43:11
 - Voidage 53:115
- Bed** 45:165
- Benzyl-Chloride** 53:107
- Bessel-Function** 44:B25
- BF₃H₃PO₄** 53:173
- BHK** 58:65
- Biaxial-Stretching** 51:113
- Bidimensional**
 - Gas-Hold-Up 47:135, 50:143
 - Spouted-Bed 47:135, 50:143
 - Three-Phase 50:143
 - Two-Phase 47:135
- Bidisperse** 55:81
- Bimolecular-Chemical-Reaction** 64:129
- Bimolecular-Reaction| Slow-»** 43:127
- Binary-Exchange-Data** 44:113
- Binary-Liquid-Mixture** 48:1
- Binary-Mixture** 52:41
- Bioartificial** 44:B81
- Biocatalyst** 44:B41
- Biocatalytic-Transformation** 51:B1
- Biochemical** 62:193
- Bioconversion**
 - Acrylamide 46:B43
 - Acrylonitrile 46:B43
 - Dynamic-Response 43:B1
 - Ethanol 43:B1
 - Highly-Compact 46:B43
 - Immobilized-Cell-Packed-Bed-Bioreactor 43:B1
 - Multiphasic-Reactor 46:B43
 - Perturbation 43:B1
 - Process-Parameter 43:B1
 - Sugar 43:B1
- Biodegradation** 56:B91
- Biofilm-Reactor**
 - Carbon-Oxidation 65:165
 - Denitrification 65:227
 - Feed-Concentration 65:165
 - Kinetics 65:227
 - Multi-Substrate 65:165
 - Nitrification 65:165

- Packed-Bed 65:165
- Rotating-Disk 65:227
- Sinusoidal-Perturbations 65:165
- Upflow 65:165
- Biofilter**
 - Analysis 65:55
 - Application 65:133
 - Comparison 65:55
 - Denitrification 65:133
 - Dynamic-Modeling 65:133
 - Generalized-Approach 65:133
 - Model 65:55
 - Simulation 65:133
 - Waste-Water 65:133
- Biokinetics** 49:B1
- Bioleaching**
 - Adapted 44:B31
 - Bacterial-Adaptation 56:B115
 - Ferrous-Sulfide 56:B115
 - Kinetics 56:B115
 - Mechanism 56:B115
 - Nonferrous-Sulfide 44:B31
 - Thiophilic-Bacteria 44:B31
- Biological**
 - Axial 44:B57
 - Backmixing-Effect 44:B57
 - Loop-Reactor 44:B57
 - Microbial-Film 44:B87
 - Modeling 44:B57
 - Packed-Bed 44:B57
 - Rate-Equation 44:B87
 - Recycle 44:B57
- Biological-Batch-Reactor** 56:B43
- Biological-Deactivation** 62:155
- Biological-Fluidized-Bed** 52:B21
- Biological-Growth-Process** 51:B25
- Biomass**
 - Anaerobic-Digestion 54:B9
 - Charcoal-Oil-Water-Mixture 60:49
 - Cow-Manure 54:B9
 - Deashing 60:49
 - Energetical-Valorization 60:49
 - Immobilized 54:B9
 - Kinetics 54:B9
 - Liquid-Fuel 60:49
 - Zeolite 54:B9
- Biomass-Retention** 44:B1
- Bioparticle** 65:117
- Bioprocess** 65:109
- Bioreaction** 50:B23
- Bioreactor**
 - Aerated 59:187
 - Aeration 58:59
 - Application 43:B19
 - Applied 51:B35
 - Bubble 59:187
 - Cell 56:B15
 - Control 51:B35
 - Design 43:B19, 51:B63, 55:B73, 57:B1
 - Determination 59:187
 - Diffusional-Characteristics 55:B35
 - Effect 56:B15
 - Entrainment 59:187
 - Equation 51:B63, 55:B73
 - Equipped 57:B1
 - Expert-System 51:B35
 - Fluid 55:B73
 - Fluidized-Bed 61:241
 - Gas-Transfer 57:B1
 - Gel 55:B35
 - High-Rate 57:B1
 - Hollow-Fiber 51:B63, 55:B73
 - Hydrodynamics 62:175
 - Immobilized-Enzyme-System 61:241
 - Impeller 58:59
 - Industrial-Scale 51:B35
 - Isotropic-Turbulence 43:B19
 - Kolmogorov-Theory 43:B19
 - Magnetically-Stabilized 61:241
 - Mass-Transfer 59:187, 61:241, 62:175
 - Mathematical-Model 43:B19
 - Membrane 62:175
 - Michaelis-Menten-Kinetics 51:B63
 - Oxygen-Transfer 56:B15
 - Parameter 59:187
 - Particle 56:B15
 - Performance 55:B35, 57:B1
 - Physical-Presence 56:B15
 - Power-Law 55:B73
 - Self-Aspirating 58:59
 - Solid 56:B15
 - Surface 59:187
 - Swelling 55:B35
 - Tool 61:241
 - Venturi-Injector 57:B1
 - Vortex 62:175
 - Wave 62:175
 - Zero-Order-Limit 51:B63
- Biosorption** 60:181
- Biosynthesis**
 - β -Cyclodextrin 61:247
 - Bacillus-Macerans-314 61:247
 - Batch 51:B43
 - Continuous-Chromatography 51:B43
 - Crude-Enzyme 61:247
 - Cyclodextrin 61:247
 - Dextran 51:B43
 - Dextranucrase 51:B43
 - Glucosyltransferase 61:247
 - Large-Scale 51:B43
 - Leuconostoc-Mesenteriodes 51:B43
 - Property 61:247
 - Purification 51:B43
- Biotechnology** 50:B9
- Biotransformation**
 - D-Sorbitol 45:B5
 - Entrapped 45:B5
 - Fine-Chemical-Production 61:53
 - γ -Butyrobetaine 61:53
 - Gluconobacter-Suboxydan 45:B5
 - L-Carnitine 61:53
 - L-Sorbose 45:B5
 - Polyacrylamide-Gel 45:B5
 - Process-Integration 61:53
- Biphasic-System** 51:B1
- Biporous** 59:177
- Blend** 47:63
- Block** 61:233
- Blowdown-Policy** 48:173
- Boiler**
 - Analysis 64:179
 - Dynamic-Measurement 64:179
 - Experimental-Study 66:159
 - Finned-Tube 66:159
 - Gas-Solid-Separator 66:159
 - Impact 66:159
 - Practical-Approach 64:179
- Bone-Powder** 67:55
- Borate** 63:27
- Boundary-Condition**
 - Outlet 57:299, 57:303
 - Slurry-Bubble-Column 57:299, 57:303
 - Solid 57:299, 57:303
- Boundary-Integral-Element-Method** 47:169
- Boundary-Integral-Solution-Method** 45:49
- Boundary-Layer**
 - Biocatalyst 44:B41
 - Cross-Flow 66:201
 - Experimental-Determination 44:B41
 - Interaction 66:201
 - Mass-Transfer 44:B41
 - Particle-Turbulence 66:201
 - Spherical-Particle 44:B41
 - Tube 66:201
 - Turbulent 66:201
- Boundary-Layer-Separation** 49:55
- Boundary-Value-Problem** 57:27
- Bounded** 66:27
- Box-Counting** 64:169
- Branching** 64:77
- Break-Up** 44:27
- Breakage** 62:23
- Breakage-Phenomena** 63:85
- Bromide** 67:19
- Bromine** 61:13
- Bronsted-Acid-Strength** 64:273
- Bronsted-Type** 64:265
- Bubble**
 - Aerated 59:187
 - Bioreactor 59:187
 - Capacitance 56:95
 - Determination 59:187
 - Distributor 56:95
 - Entrainment 59:187
 - Fluidized-Bed 56:95
 - Formation 56:95
 - Imaging 56:95
 - Mass-Transfer 59:187
 - Parameter 59:187
 - Real-Time 56:95
 - Surface 59:187
- Bubble-Column**
 - Alcohol 50:47
 - Analogous 53:89
 - Batch-Packed 54:51
 - Behavior 53:115
 - Bubble-Rise-Velocity 50:47
 - Bubble-Size 50:47
 - Concentration 50:47
 - Description 53:89
 - Gas-Liquid-Property 59:91
 - Gas-Solid-Fluidized-Bed 53:89
 - Gas-Hold-Up 50:47
 - Gas-Phase-Dispersion 59:91
 - Heat-Transfer 47:91
 - High-Throughput 53:115
 - Hydrodynamic-Investigation 47:91
 - Hydrodynamics 53:89
 - Liquid-Solid-Mass-Transfer 54:51
 - Liquid-Dispersion 53:151
 - Organic-Acid 50:47
 - Potassium-Chloride 50:47
 - Powder 47:91
 - Radial-Profile 53:115
 - Small-Particle 47:91
 - Vertical-Misalignment 53:151
 - Viscous-Liquid 47:91
 - Voidage 53:115
- Bubble-Column-Reactor**
 - Airlift-Slurry-Reactor 62:223
 - Characteristics 62:223
 - Citric-Acid 53:B35
 - Comparative-Evaluation 62:223
 - Fermentation-Broth 53:B35
 - Flow-Pattern 48:141
 - Gas-Liquid-Mass-Transfer 62:223
 - Gas-Hold-Up 50:1
 - Hydrodynamic 62:223
 - Morphological-Property 53:B35
 - Newtonian-Fluid 50:1
 - Non-Newtonian-Fluid 50:1
 - Prediction 50:1
 - Pressure-Drop 48:153
 - Rheological-Property 53:B35
 - Stirred-Tank-Reactor 53:B35
 - Submerged 53:B35

- Transport-Phenomena 48:141, 48:153
- Bubble-Formation** 49:65
- Bubble-Growth** 63:149
- Bubble-Rise-Velocity** 50:47
- Bubble-Size**
 - Alcohol 50:47
 - Bubble-Column 50:47
 - Bubble-Rise-Velocity 50:47
 - Concentration 50:47
 - Flux 67:71
 - Frequency 67:71
 - Gas 67:71
 - Gas-Liquid-Bioreactor 49:B13
 - Gas-Hold-Up 50:47
 - Maximum 49:B13
 - Membrane 67:71
 - Organic-Acid 50:47
 - Permeation 67:71
 - Potassium-Chloride 50:47
 - Sparged 67:71
 - Stable 49:B13
 - Tubular 67:71
 - Ultrafiltration 67:71
- Bubble-Size-Distribution** 50:B29
- Bubbling** 67:131
- Bubbling-Bed-Reactor** 66:193
- Bulk-Copolymerization** 48:71
- Bunch** 66:223
- Burning-Coke** 54:35
- Butanol**
 - Cell 46:B11
 - Continuous-Fermentation 46:B1, 46:B11
 - Deactivation 65:159
 - Experimental-Result 46:B1
 - Immobilized 46:B11, 65:159
 - Immobilized-Cell 46:B1
 - Integration 46:B1, 46:B11
 - Lipozyme 65:159
 - Mathematical-Modeling 46:B11
 - Pervaporation 46:B1, 46:B11
 - Simulation 46:B11
 - Temperature 65:159
 - Water-Content 65:159
- Butyrobetaine** | γ -> 61:53
- C-Terminal-Region** 65:257
- Cadmium**
 - Alga 47:B23
 - Cell-Size-Distribution 47:B23
 - Cell-Surface-Area 65:13
 - Chelated 53:183
 - Chlorella-Vulgaris 47:B23
 - Green 62:81
 - Green-Microalgae 65:13
 - Influence 47:B23
 - Kinetic-Behavior 53:183
 - Mass-Transfer 53:183
 - Microalgae 62:81
 - Solution 53:183
 - Unicellular 62:81, 65:13
- Uptake 62:81, 65:13
- Zinc 47:B23
- Calcined** 47:1
- Calcined-Limestone** 47:11
- Calcium**
 - Alginate 56:B9
 - Determination 56:B9
 - Diffusion-Coefficient 56:B9
 - Fly-Ash 66:171
 - Glucose 56:B9
 - Hydroxide 66:171
 - Identification 56:B9
 - Malic-Acid 56:B9
 - Maximum 66:171
 - Membrane 56:B9
 - Mixture 66:171
 - Model 56:B9
 - Removal 66:171
 - Structural-Property 66:171
 - Sulphur-Dioxide 66:171
 - Yield 66:171
- Calcium-Alginate** 65:81
- Calcium-Oxide** 46:119
- Calcium-Sulfite** 66:123
- Calculating** 56:27
- Calculation**
 - Application 61:27
 - Applied 48:111
 - Burning-Coke 54:35
 - Catalyst 54:35
 - Coke 55:125
 - Comparison 55:125, 61:21
 - Deactivation 55:125
 - Drainage-Rate 50:69
 - Filter-Cake 50:69
 - High-Pressure 61:27
 - Kinetics 54:35, 55:125
 - Method 55:125
 - Mixer 47:141
 - Model 61:21, 61:27
 - Motionless 47:141
 - Prediction 61:21
 - Regeneration 54:35
 - Residence-Time 47:141
 - Semiempirical-Equation-of-State 48:111
 - Temperature-Ramp 54:35
 - Trajectory 47:141
 - Two-Phase-Flow-Model 50:69
 - Vapor-Liquid-Equilibrium 48:111, 61:21, 61:27
- Calf-Rennet** 56:B87
- Calorimetry** 59:143
- Capacitance** 56:95
- Capacitance-Probe** 52:1
- Capacity** 59:243
- Capillary-Gap-Cell** 43:107
- Carbon**
 - Activated 52:37, 59:205
 - Adsorption 59:205
 - Aqueous-Solution 52:37
 - Branching 64:77
 - Diffusion-Limited 64:77
 - Equilibrium 59:205
 - Gasification 64:77
 - Interpretation 57:137
 - Langmuir-Kinetics 57:137
 - Mass-Transfer 57:137
 - Model 64:77
 - Modeling 64:77
 - Molecular-Sieve 57:137
 - Pore 64:77
 - Removal 52:37
 - Stochastic-Model 59:205
 - Tannic-Acid 52:37
- Carbon-Dioxide**
 - Absorption 67:131
 - Alcohol 43:25
 - Aliphatic-Ether 43:25
 - Aqueous-Solution 46:1
 - Bubbling 67:131
 - Carbon-Monoxide 68:63
 - Chemical-Reaction 46:1
 - Comparison 61:227
 - Conventional 61:227
 - Correlation 66:217
 - Corresponding-States 66:217
 - Cryogenic-Liquid 43:25
 - Desorption 46:1
 - Difference 68:63
 - Diglycolamine 44:107
 - Extraction 61:227
 - Grape 61:227
 - Hydrocarbon 66:217
 - Inactivation 52:B29
 - Influence 67:131
 - Kinetics 44:107
 - Leuconostoc-Dextranicum 52:B29
 - Liquid 61:227
 - Methanation 68:63
 - Morpholine 44:107
 - Nitrous-Oxide 43:25
 - Normal-Paraffin 52:55
 - Oil 61:227
 - Potassium-Carbonate 46:1
 - Pressure 52:B29
 - Reaction 44:107
 - Recovery 61:227
 - Seed 61:227
 - Selectivity 68:63
 - Solubility 43:25, 52:55
 - Solvent-Extraction 61:227
 - Stirred-Tank 67:131
 - Supercritical 61:227
 - Surfactant 67:131
 - System 46:1, 66:217
 - Vapor-Liquid-Equilibrium 66:217
 - Water 43:25
- Carbon-Formation** 46:129
- Carbon-Monoxide**
 - Absorption 59:243
 - Automobile 53:47
 - Capacity 59:243
 - Carbon-Dioxide 68:63
 - Catalysis 64:283
 - Catalytic-Converter 53:47
 - Copper-Cerium-Dioxide 64:283
 - Cosorb-Solution 59:243
 - Difference 68:63
 - Exhaust-Gas 53:47
 - Fluorite 64:283
 - Methanation 68:63
 - Modeling 53:47
 - Monolithic 53:47
 - Oscillatory-Feeding 53:47
 - Oxidation 64:283
 - Oxide 64:283
 - Oxygen 53:47
 - Performance 53:47
 - Rate 59:243
 - Selectivity 68:63
 - Transition-Metal-Promoted 64:283
- Carbon-Oxidation** 65:165
- Carrier**
 - Amberlite 58:285
 - Block 61:233
 - Cell 58:285
 - Constant-Interface-Area 58:285
 - Emulsion 63:127, 66:11
 - Ethanol 61:233
 - Extraction 58:285
 - Facilitated 63:127, 66:11
 - Fructose 61:233
 - Kinetics 58:285
 - Liquid 63:127, 66:11
 - Membrane 63:127, 66:11
 - Mobile 58:285
 - Modeling 63:127, 66:11
 - Penicillin-G 58:285
 - Production 61:233
 - Saccharomyces-Cerevisiae 61:233
 - Wood 61:233
- Cascade** 50:109
- Case-Study** 44:119
- Catafractionation** 56:11
- Catalase** | **Immobilized**-> 55:B41
- Catalysis**
 - Ammonia 67:1
 - Carbon-Monoxide 64:283
 - Cobalt-Salt 43:33
 - Copper-Cerium-Dioxide 64:283
 - Fluorite 64:283
 - Glaserite 67:1
 - Gypsum 67:1
 - Liquid-Phase 43:33
 - Normal-Octane 43:33
 - Overall-Kinetics 43:33
 - Oxidation 43:33, 64:283
 - Oxide 64:283
 - Potassium-Sulfate 67:1
 - Product-Distribution 43:33

- Production 67:1
- Sylvinite 67:1
- Transition-Metal-Promoted 64:283
- Catalyst**
 - 1-Butene 60:147, 64:265
 - Acid 64:265
 - Active 53:13
 - Activity 52:115
 - Adsorption-Enthalpy 60:147
 - Aging 66:51
 - Alkylation 53:173
 - Al₂O₃ 64:265
 - Analogy 61:113
 - Analysis 47:105
 - Behavior 43:11
 - BF₃H₃PO₄ 53:173
 - Bidisperse 55:81
 - Borate 63:27
 - Bronsted-Type 64:265
 - Burning-Coke 54:35
 - Calculation 54:35
 - Cerium-Oxide 64:225
 - Change 43:11
 - Characteristics 64:225
 - Characterization 52:115
 - Chemical-Vapor-Deposition 53:13
 - Cobalt 52:115
 - Combined 47:105
 - Commercial 58:7
 - Constant 47:105
 - Convection 61:113
 - Convective-Flow 55:81
 - Conversion 47:105, 54:41
 - Copper(II) 57:273
 - Cracking 58:7
 - Cylinder 61:113
 - Deactivation 43:11, 46:109, 58:7
 - Decay 47:105
 - Dehydrogenation 46:109
 - Design 53:1, 64:69
 - Diffusion 53:1, 61:113
 - Direct-Test 60:147
 - Effectiveness 55:81
 - Exit 47:105
 - Factor 53:1
 - First-Order-Reaction 54:41
 - Fixed-Bed-Reactor 47:105, 54:41
 - Fluidized-Bed-Reactor 60:131
 - Forced-Convection 57:101
 - Fractal 64:69
 - γ -Alumina 57:273
 - Geometry 61:113
 - Heterogeneous-Reactor 54:41
 - Hydrocarbon 52:115
 - Hydrogenation 63:27
 - Industrial 57:273
 - Intraparticle 53:1
 - Intraparticle-Convection 54:41
 - Intrinsic-Kinetics 57:273
 - Isomerization 60:147, 64:265
 - Isopropylbenzene 58:7
 - Isothermal 54:41
 - Kinetic-Modeling 58:7
 - Kinetics 54:35
 - Large-Pore 54:41
 - Macropore 55:81
 - Mathematical-Modeling 60:131
 - Metal-Oxide 64:295
 - Methane 57:273
 - Methylcyclohexane 46:109
 - Mixed-Oxide 64:265
 - Mixture 43:11
 - Model 43:11
 - Modeling 53:13
 - Mole-Change 57:101
 - Morphology 64:69
 - Nanocrystalline 64:225
 - Naphthalene 53:173, 63:27
 - Nonstoichiometric 64:225
 - Oxidation 52:115, 57:273, 64:295
 - Oxide 52:115, 57:273, 64:203
 - Particle 53:1, 61:113
 - Phase 53:13
 - Platinum-Aluminum 63:27
 - Pore-Size 43:11
 - Porous 57:101
 - Preparation 53:13, 64:203
 - Profile 53:13
 - Propene 53:173
 - Pt-Sn/Al₂O₃ 46:109
 - Reaction 43:11, 57:101, 61:113
 - Reaction-Kinetics 53:1
 - Recent-Advances 64:203
 - Reforming 66:51
 - Regeneration 54:35
 - Relationship 64:265
 - Silica-Alumina 58:7, 60:147
 - Silicon-Dioxide 64:265
 - Single-Pellet 43:11
 - Site 64:265
 - Slab 61:113
 - Solid 64:265
 - Soot 64:295
 - Space-Time-Trajectory 47:105
 - Steam 66:51
 - Support 43:11, 57:273, 64:203
 - Supported-Catalyst 43:11
 - Surface-Active 64:265
 - Synthesis 64:225
 - Technique 53:13
 - Temperature 47:105
 - Temperature-Ramp 54:35
 - Three-Phase-System 53:173
 - Titanium-Dioxide 64:265
 - Total 52:115
 - Unsteady-State 60:131
 - Zirconium-Dioxide 64:265
- Catalytic-Afterburner** 52:79
- Catalytic-Bed-Reactor** 44:97
- Catalytic-Converter** 53:47
- Catalytic-Cracking** 44:53
- Catalytic-Method** 58:33
- Catalytic-Partial-Oxidation** 66:193
- Catalytic-Process** 60:111
- Catalytic-Property** 64:247
- Catalytic-Reaction**
 - Analytical-Solution 59:161
 - Approximate 59:161
 - Artificial 64:63
 - Devils-Comb 64:63
 - Effectiveness-Factor 59:161
 - Fractal 64:63
 - Microwave-Radiation 49:79
 - Parallel 59:161
 - Presence 49:79
 - Simulation 64:63
- Catalytic-Transfer** 51:B51
- Catalytic-Wall-Reaction** 62:51
- Catalytically-Stabilized-Thermal-Burner** 50:123
- Cavitation** 55:B67
- Celestine-Method** 66:79
- Cell**
 - Amberlite 58:285
 - Bioreactor 56:B15
 - Butanol 46:B11
 - Carrier 58:285
 - Column 59:1
 - Constant-Interface-Area 58:285
 - Continuous-Fermentation 46:B11
 - Effect 56:B15
 - Extraction 58:285
 - Flotation 59:1
 - Immobilized 46:B11
 - Integration 46:B11
 - Kinetics 58:285
 - Large-Scale 59:1
 - Mathematical-Modeling 46:B11
 - Mobile 58:285
 - Oxygen-Transfer 56:B15
 - Particle 56:B15
 - Penicillin-G 58:285
 - Performance 59:1
 - Pervaporation 46:B11
 - Physical-Presence 56:B15
 - Pilot-Plant-Data 59:1
 - Prediction 59:1
 - Simulation 46:B11
 - Solid 56:B15
- Cell-Culture** 58:65
- Cell-Immobilization** 46:B21
- Cell-Size-Distribution** 47:B23
- Cell-Surface-Area** 65:13
- Cellobiohydrolase** 59:315
- Cellulose** 45:B27
- Cephalosporin-C** 52:B71
- Cerium-Oxide** 64:225
- Cetyltrimethylammonium** 67:19
- Chain-of-Rotator** 46:29
- Change**
 - Adsorption 62:73
 - Behavior 43:11
 - Catalyst 43:11
 - Charge 62:73
 - Deactivation 43:11
 - Dialysis 62:73
 - Ion 62:73
 - Membrane 62:73
 - Mixture 43:11
 - Model 43:11
 - Permeability 62:73
 - Pore-Size 43:11
 - Protein 62:73
 - Reaction 43:11
 - Single-Pellet 43:11
 - Support 43:11
 - Supported-Catalyst 43:11
- Chaos**
 - Bimolecular-Chemical-Reaction 64:129
 - Chemical-Engineering 64:v
 - Control 64:141
 - Deterministic-Analysis 64:149
 - Fractal 64:v
 - Helical-Coil-Reactor 64:129
 - Horizontal-Pipe 64:149
 - Interfacial-Stretching 64:129
 - Intermittent-Flow-Regime 64:149
 - Linear-Controller 64:141
 - Nonlinear-Controller 64:141
 - Polymerization-Reaction 64:141
 - Pressure-Fluctuation 64:149
 - **Chaotic-Flow**
 - Chemical-Reaction 64:117
 - Kenics-Static-Mixer 67:153
 - Three-Dimensional 67:153
- Chaperonin** 65:151
- Characteristics**
 - Adsorption-Isotherm 60:181
 - Airlift-Slurry-Reactor 62:223
 - Biosorption 60:181
 - Bubble-Column-Reactor 62:223
 - Catalyst 64:225
 - Cerium-Oxide 64:225
 - Comparative-Evaluation 62:223
 - Comparison 60:181
 - Continuous-Stirred-Tank-Bioreactor 55:B47
 - Elevated 54:63
 - Ethanol 54:63
 - Fed 55:B47
 - Fluidized-Bed 43:67
 - Gas 54:63
 - Gas-Liquid-Ejector 53:67

- Gas-Liquid-Mass-Transfer 62:223
- Heat-Transfer-Rate 51:7
- Heavy-Metal 60:181
- Hold-Up 43:67
- Hydrodynamic 62:223
- Hydrodynamics 43:95, 53:67
- Inhibitory-Substrate 55:B47
- Liquid-Side 58:251
- Local 53:67
- Mass-Transfer 43:95, 53:67, 54:63, 58:251
- Methanol 54:63
- Nanocrystalline 64:225
- Nonstoichiometric 64:225
- Operation 51:7
- Packed-Bubble-Column 43:95
- Packing 58:251
- Phase 43:67
- Pressure 54:63
- Stability 55:B47
- Structured 58:251
- Synthesis 64:225
- Temperature 54:63
- Three-Phase 43:67
- Tubular-Reactor 51:7
- Upper-Limit 55:B47
- Zoogloea-Ramigera 60:181
- Characterization**
 - Activity 52:115
 - Aerosol 64:239
 - Antigen-Coupled 54:B33
 - Aphron 65:1
 - Box-Counting 64:169
 - Capacitance-Probe 52:1
 - Catalyst 52:115
 - Circulating 64:107
 - Cobalt 52:115
 - Colloidal 65:1
 - Copper-Modified 64:239
 - Decomposition 64:239
 - Dimension 64:169
 - Embedding 64:169
 - Flow 64:107
 - Flow-Regime 64:169
 - Fluidized-Bed 64:107
 - Gas 65:1
 - Gas-Bubble 52:1
 - High-Temperature 64:239
 - Higher-Alcohol 64:239
 - Homogeneous 54:B33
 - Hydrocarbon 52:115
 - Immunoassay 54:B33
 - Liposome 54:B33
 - Multifractal 64:107
 - Multiphase-Reactor 64:169
 - Oxidation 52:115
 - Oxide 52:115
 - Polyclonal-Antibody 54:B33
 - Process 64:239
 - Protein 65:1
 - Recovery 65:1
 - Stirred-Tank-Reactor 52:1
 - Subsequent 65:1
 - Synthesis 64:239
 - Total 52:115
 - Zinc-Chromite 64:239
- Charcoal** 57:9
- Charcoal-Oil-Water-Mixture** 60:49
- Charge** 62:73
- Chelated** 53:183
- Chemical-Engineering**
 - Biotechnology 50:B9
 - Chaos 64:v
 - Fractal 64:v
 - Fuzzy-Calculus 54:155
 - Knowledge 54:155
 - Revitalization 54:155
 - Role 50:B9
 - **Chemical-Engineering-Research**
 - Netherlands 53:v
 - Poland 58:vii
 - South-Africa 54:ix
- Chemical-Equilibrium** 54:187
- Chemical-Equilibrium-Analysis** 51:B1
- Chemical-Method** 67:167
- Chemical-Plant** 44:167
- Chemical-Reaction**
 - Absorption 57:1, 58:151
 - Activity 57:1
 - Aqueous-Solution 46:1
 - Batch 52:107
 - Carbon-Dioxide 46:1
 - Chaotic-Flow 64:117
 - Column-Plate 57:1
 - Convective-Diffusive-Mass-Transfer 68:11
 - Couette-Flow 68:11
 - Description 57:115
 - Desorption 46:1
 - Dusty-Gas 57:115
 - Flow 52:107
 - Gas-Solid-Fluidized-Bed-Reactor 58:223
 - Gas-Flow 58:223
 - Integral-Spectral-Approach 68:11
 - Interfacial 57:205
 - Ionic-Bubble 57:1
 - Marangoni-Instability 58:151
 - Mass-Transfer 57:205
 - Mass-Transport 57:115
 - Mathematical-Formulation 68:11
 - Model 57:115
 - Modeling 58:223
 - Nonideal-Phenomena 57:205
 - Numerical-Illustration 68:11
 - Porous-Medium 57:115
 - Potassium-Carbonate 46:1
 - Pulsatile 52:107
 - Reconsideration 58:223
 - Role 57:205
 - Stirred-Tank-Reactor 52:107
 - System 46:1
 - Variation 58:223
- Chemical-Reactor**
 - Bounded 66:27
 - Control 66:27
 - Micromixing 58:183
 - Natural 59:169
 - Nonlinear-Oscillation 59:169
 - Nonlinearity 66:27
 - Oscillatory-Reaction 66:27
 - Performance 59:169
 - Turbulent 58:183
- Chemical-Vapor-Deposition** 53:13
- Chemical-Vapor-Deposition-Reactor**
 - Compressible 54:137
 - Diffusion 57:127
 - Fluid 54:137
 - Horizontal 54:137, 57:39
 - Hot-Wall 57:39
 - Low-Pressure 57:39
 - Modeling 57:39
 - Multicomponent 57:127
 - Multiple-Wafer 57:127
 - Phenomena 57:127
 - Stability 54:137
 - Thermal 57:39
 - Transport-Property 54:137
 - Tubular 57:39
 - Variable 54:137
- Chemo-Autotrophic-Biogas** 58:71
- Chitosan** 65:93
- Chlorella-Vulgaris** 47:B23
- Chlorine-Dioxide** 60:101
- Choice** 52:B59
- Chromatographic-Behavior** 49:B29
- Chromatography**
 - Bioreaction 50:B23
 - Continuous-System 50:B23
 - Economical-Optimization 64:307
 - Extraction 64:307
 - Fluidized 64:307
 - Ion-Exchange 64:307
 - Modeling 64:307
 - Separation 50:B23
 - Simplified 64:307
 - Whey-Protein 64:307
- Circuit-Design-Principle** 59:15
- Circular-Tube** 55:103
- Circulating**
 - Characterization 64:107
 - Cyclone-Reactor 45:9
 - Efficiency 45:9
 - Flow 64:107
 - Fluidized-Bed 64:107
 - Gas 45:9
 - Heat-and-Mass-Transfer 45:9
 - Multifractal 64:107
 - Reactor-Wall 45:9
 - Single 45:9
- Citric-Acid** 53:B35
- Citric-Acid-Production** 62:215
- Citrus** 56:B37
- Closed-System**
 - Acetifier 62:183, 65:201
 - Batch 62:183
 - Computer-Simulation 62:183, 65:201
 - Industrial 62:183, 65:201
 - Operating-Condition 62:183, 65:201
 - Operation 62:183
 - Optimum 62:183, 65:201
 - Semi-Continuous-Operation 65:201
- Closely-Spaced** 49:65
- Closure-Problem** 58:161
- Coal**
 - Comprehensive 57:295
 - Computation 57:295
 - Control-Strategy 59:133
 - Evaluation 59:133
 - Gasifier 59:133
 - Hydrogenation 58:53
 - Implementation 59:133
 - Influence 58:53
 - Kinetics 58:53
 - Mo-Catalyzed 58:53
 - Model 57:295
 - Moving-Bed 59:133
 - Nature 58:53
 - Porous 58:53
 - Specific-Energy 57:295
- Coalescing-Property** 55:1
- Coarse** 67:37
- Coaxial** 63:11
- Cobalt** 52:115
- Cobalt-Salt** 43:33
- Cocurrent** 63:93
- Cocurrent-Upflow-Bioreactor** 62:237
- Cod** 56:B43
- Coefficient**
 - Antibiotic-Separation 65:63
 - Application 65:63
 - Column 55:B1
 - Continuous-Stirred-Tank-Reactor 65:63
 - Enzyme 55:B1
 - Evaluate 65:63
 - Extraction 55:B1
 - Kinetic-Parameter 65:63
 - Mass-Transfer 55:B1, 65:63
 - Sieve-Plate 55:B1
- Coke** 55:125
- Colloidal** 65:1
- Colloidal-Dispersion** 56:143
- Column**
 - Adsorption 65:81
 - Adsorption-Data 65:81
 - Ammonia-Removal 66:65

- Anaerobically-Treated 66:65
- Calcium-Alginate 65:81
- Cell 59:1
- Coefficient 55:B1
- Copper 65:81
- Dynamic-Approach 65:81
- Enzyme 55:B1
- Evaluation 65:81
- Extraction 55:B1
- Flotation 59:1
- Homoionic-Zeolite 66:65
- Immobilized 65:81
- Ion-Exchange 66:65
- Large-Scale 59:1
- Mass-Transfer 55:B1
- Moment-Analysis 65:81
- Packed 66:65
- Packed-Bed 65:81
- Performance 59:1
- Piggery-Manure 66:65
- Pilot-Plant-Data 59:1
- Prediction 59:1
- Sieve-Plate 55:B1
- Stimulus-Response 65:81
- Technique 65:81
- Zoogloea-Ramigera 65:81
- Column-Plate** 57:1
- Combined** 47:105
- Combustion** 50:123
- Commercial** 58:7
- Comparative-Evaluation** 62:223
- Comparative-Study** 60:75
- Comparison**
 - A-Si-H 58:1
 - Adsorption-Isotherm 60:181
 - Adsorption-Process 56:59
 - Anaerobic 55:B55
 - Analysis 65:55
 - Batch 65:195
 - Biofilter 65:55
 - Biosorption 60:181
 - Calculation 55:125, 61:21
 - Carbon-Dioxide 61:227
 - Characteristics 60:181
 - Chemical-Method 67:167
 - Coke 55:125
 - Control 55:B55
 - Conventional 61:227
 - Countercurrent 56:59
 - Deactivation 55:125
 - Density-Independent 61:213
 - Deposition 58:1
 - Digester 55:B55
 - Dynamics 55:B55
 - Engulfment 45:25
 - Enzymatic-Hydrolysis 65:195
 - Extraction 61:227
 - Extraction-Column 46:137
 - Grape 61:227
 - Heavy-Metal 60:181
 - Interaction-by-Exchange-with-the-Mean 45:25
 - Kinetics 55:125
 - Liquid 61:227
 - Liquid-Test-System 46:137
 - Measurement 67:167
 - Mechanically-Agitated 46:137
 - Mesophilic 55:B55
 - Method 55:125
 - Micromixing 45:25
 - Mixing-Rules 61:213
 - Mixing-Time 67:167
 - Model 45:25, 61:21, 65:55
 - Modeling 56:59
 - Modified-Kurihara-Mixing-Rule 61:213
 - Oil 61:227
 - Performance 55:B55, 65:195
 - Physical-Method 67:167
 - Plasma-Enhanced 58:1
 - Prediction 61:21
 - Protein 65:195
 - Recovery 61:227
 - Seed 61:227
 - Simulation 56:59
 - Single-Drop-Experiment 46:137
 - Sludge 55:B55
 - Solvent-Extraction 61:227
 - Stirred-Reactor 65:195
 - Strategy 56:59
 - Supercritical 61:227
 - Thermophilic 55:B55
 - Torus-Reactor 65:195
 - Two-Reactor-Arrangement 58:1
 - Vapor-Liquid-Equilibrium 61:21
 - Wheat 65:195
 - Zoogloea-Ramigera 60:181
- Competing-Reaction** 61:41
- Complex**
 - Distillation-Column 47:119
 - Enzymatic-Hydrolysis 52:B13
 - Enzyme 52:B13
 - Mixture 52:B13
 - Modeling 52:B13
 - Potato-Pulp 52:B13
 - Setting 47:119
 - Simulation 52:B13
- Complex-Reaction-System** 46:23
- Complex-Rectification-Column** 45:149
- Complex-Selective-Medium** 52:B35
- Component** 64:85
- Composite** 50:59
- Composite-Phase** 50:59
- Comprehensive** 57:295
- Compressible** 54:137
- Computation**
 - Bessel-Function 44:B25
 - Coal 57:295
 - Comprehensive 57:295
 - Efficient 44:B25
 - High-Pressure 60:1
 - Integral 44:B25
 - Model 57:295
 - Specific-Energy 57:295
 - Thermodynamic-Interpretation 60:1
 - Vapor-Liquid-Equilibrium 60:1
- Computational** 59:39
- Computer-Aided-Analysis** 46:47
- Computer-Assisted-Image-Analysis** 49:141
- Computer-Simulation**
 - Acetifier 62:183, 65:201
 - Batch 62:183
 - Closed-System 62:183, 65:201
 - Industrial 62:183, 65:201
 - Operating-Condition 62:183, 65:201
 - Operation 62:183
 - Optimum 62:183, 65:201
 - Semi-Continuous-Operation 65:201
- Concentration**
 - Alcohol 50:47
 - Aliquat-336 59:303
 - Application 65:21
 - Autoclave-Reactor 67:175
 - Bacillus-Subtilis 59:303
 - Bubble-Column 50:47
 - Bubble-Rise-Velocity 50:47
 - Bubble-Size 50:47
 - Cosolvent 59:303
 - Enzyme 59:303
 - Gas-Hold-Up 50:47
 - High-Temperature 67:175
 - Measurement 60:161
 - Mini-Hydrocyclone 65:21
 - Organic-Acid 50:47
 - Potassium-Chloride 50:47
 - Purification 59:303
 - Reversed-Micelle 59:303
 - Separation 59:303
 - Solid 60:161, 67:175
 - Suspension 65:21
 - Three-Phase-Reactor 60:161
 - Ultrasonic-Measurement 67:175
 - Ultrasonic-Technique 60:161
 - Yeast 65:21
- Concentration-Dependent** 43:1
- Concomitant-Product** 46:B53
- Condensation** 49:177
- Condition**
 - 4-Cyanopyridine 56:B49
 - 4-Picoline 56:B49
 - Arrangement 55:15
 - Fully-Developed-Flow 55:15
 - High-Yield 56:B49
 - Laminar 55:15
 - Numerical-Study 55:15
 - Process 56:B49
 - Wavy-Walled-Pipe 55:15
- Configuration-Factor** 45:75
- Conical**
 - Contactor 51:45
 - Expansion 51:45
 - Gas-Flow 56:19
 - Geometry 62:113
 - Hydrodynamics 62:113
 - Influence 62:113
 - Pressure-Drop 51:53
 - Section 62:113
 - Shallow 62:113
 - Simplified-Model 56:19
 - Spouted-Bed 51:45, 51:53, 56:19, 62:113
- Connectionist-System** 54:125
- Consecutive-Reaction** 46:91
- Constancy** 49:17
- Constant**
 - Analysis 47:105
 - Catalyst 47:105
 - Combined 47:105
 - Continuous-Flow-Reactor 45:B1
 - Conversion 47:105
 - Decay 47:105
 - Enzyme-Activity 45:B1
 - Exit 47:105
 - Fixed-Bed-Reactor 47:105
 - Space-Time-Trajectory 47:105
 - Temperature 47:105
- Constant-Biomass-Hold-Up** 45:B35
- Constant-Interface-Area** 58:285
- Constrained-Optimization** 59:229
- Construction** 56:B75
- Consumption** 62:149
- Contactor**
 - Conical 51:45
 - Expansion 51:45
 - Gas-Liquid-Parameter 52:121
 - Measurement 52:121
 - Mechanically-Agitated 52:121
 - Spouted-Bed 51:45
- Continuous** 54:207
- Continuous-Annular-Chromatography** 55:B19
- Continuous-Chromatography** 51:B43
- Continuous-Collocation-Polynomial** 51:83
- Continuous-Couette-Flow-Device** 48:101
- Continuous-Crystallizer** 46:B35
- Continuous-Ethanol-Production** 50:B17
- Continuous-Fermentation**
 - Butanol 46:B1, 46:B11
 - Cell 46:B11
 - Experimental-Result 46:B1
 - Immobilized 46:B11
 - Immobilized-Cell 46:B1

- Integration 46:B1, 46:B11
- Mathematical-Modeling 46:B11
- Pervaporation 46:B1, 46:B11
- Simulation 46:B11
- Continuous-Flow-Reactor** 45:B1
- Continuous-Flow-Stirred-Tank-Reactor** 62:143
- Continuous-Fluidized-Bed** 55:B29
- Continuous-Stirred-Reactor** 53:B47
- Continuous-Stirred-Tank-Bioreactor**
 - Characteristics 55:B47
 - Control 56:B69
 - Degrading 50:B1, 62:67
 - Fed 55:B47
 - Global 56:B69
 - Inhibitory-Substrate 50:B1, 55:B47
 - Operational-Range 50:B1
 - Phenol 62:67
 - Range 62:67
 - Stability 55:B47, 62:67
 - Upper-Limit 55:B47
- Continuous-Stirred-Tank-Reactor**
 - Activated-Carbon-Column 58:239
 - Antibiotic-Separation 65:63
 - Application 65:63
 - Coefficient 65:63
 - Estimation 58:239
 - Evaluate 65:63
 - Experiment 58:239
 - Intraparticle-Kinetic-Parameter 58:239
 - Kinetic-Parameter 65:63
 - Mass-Transfer 65:63
 - Simulation 58:239
 - Solid-Liquid-Adsorption 58:239
- Continuous-System** 50:B23
- Continuous-Transport** 53:B1
- Control**
 - Adaptive 63:65
 - Anaerobic 55:B55
 - Applied 51:B35
 - Batch-Process 63:65
 - Bioreactor 51:B35
 - Bounded 66:27
 - Chaos 64:141
 - Chemical-Reactor 66:27
 - Choice 52:B59
 - Comparison 55:B55
 - Continuous-Stirred-Tank-Bioreactor 56:B69
 - Development 63:65
 - Digester 55:B55
 - Dynamics 55:B55, 67:103
 - Enzyme-Activity 51:B11
 - Expert-System 51:B35
 - Fed-Batch 52:B59
 - Fermentation 52:B59
 - Flexible 63:65
 - Global 56:B69
 - Industrial-Scale 51:B35
 - Linear-Controller 64:141
 - Mesophilic 55:B55
 - Mineral-Process 59:71
 - Model 50:159
 - Modeling 50:95, 59:71
 - Neural-Network 63:65
 - Nonlinear-Controller 64:141
 - Nonlinear-System 67:103
 - Nonlinearity 66:27
 - Optimization 52:B59
 - Oscillatory-Reaction 66:27
 - Performance 55:B55
 - Polymer 50:95
 - Polymerization-Reaction 64:141
 - Prediction 50:159
 - Reaction-Engineering 50:95
 - Set-Point-Weighting 50:159
 - Simplified 50:159
 - Sludge 55:B55
 - Steady-State 67:103
 - Stirred-Bioreactor 51:B11
 - Thermophilic 55:B55
 - Tomographic-Imaging 59:71
 - Unstable 67:103
 - Variable 52:B59
- Control-Strategy** 59:133
- Controlled**
 - 1-Propanol 51:129
 - Alkoxide 55:93
 - Fine 51:129, 55:93
 - High-Temperature-Range 55:93
 - Hydrolysis 51:129, 55:93
 - Particle 51:129, 55:93
 - Spherical 51:129, 55:93
 - Synthesis 51:129, 55:93
 - Tetrabutoxide 51:129
 - Zirconia 51:129, 55:93
 - Zirconium 51:129, 55:93
- Controlled-Hydrolysis** 44:133
- Convection** 61:113
- Convective-Coefficient** 57:285
- Convective-Diffusion**
 - Catalytic-Wall-Reaction 62:51
 - Duct 62:51
 - Electrolytic 68:69
 - Externally-Imposed 68:69
 - Fluid 62:51
 - Force-Field 68:69
 - Homogeneous 62:51
 - Inside 62:51
 - Numerical-Solution 68:69
 - Power-Law 62:51
 - Single 62:51
- Convective-Diffusive-Mass-Transfer** 68:11
- Convective-Diffusive-Transport** 61:63
- Convective-Flow** 55:81
- Convective-Mass-Transfer** 62:43
- Conventional**
 - Carbon-Dioxide 61:227
 - Comparison 61:227
 - Extraction 61:227
 - Grape 61:227
 - Hydrolysis 59:253
 - Liquid 61:227
 - Microwave-Heating 59:253
 - Oil 61:227
 - Recovery 61:227
 - Seed 61:227
 - Solvent-Extraction 61:227
 - Stirred-Tank-Reactor 59:253
 - Sucrose 59:253
 - Supercritical 61:227
- Conversion**
 - Alternative 45:33
 - Analysis 47:105
 - Catalyst 47:105, 54:41
 - Catalytic-Process 60:111
 - Combined 47:105
 - Constant 47:105
 - Decay 47:105
 - Exit 47:105
 - First-Order-Reaction 54:41, 60:111
 - Fixed-Bed-Reactor 47:105, 54:41
 - Flow-Rate 60:111
 - Heterogeneous-Reactor 54:41
 - Hydrocarbon 45:33
 - Intraparticle-Conversion 54:41
 - Irreversible-Reaction 60:111
 - Isothermal 54:41
 - Kinetic-Model 45:33
 - Large-Pore 54:41, 60:111
 - Material 60:111
 - Methanol 45:33
 - Modeling 45:33
 - Operating-Temperature 60:111
 - Plug-Flow-Reactor 60:111
 - Space-Time-Trajectory 47:105
 - Temperature 47:105
- Convex-Hull** 54:187
- Cooling-Policy** 59:143
- Copolymer** 65:249
- Copper** 65:81
- Copper(II)**
 - Adsorption 58:265
 - Batch-Stirred-Reactor 58:265
 - Catalyst 57:273
 - γ -Alumina 57:273
 - Industrial 57:273
 - Intrinsic-Kinetics 57:273
 - Methane 57:273
 - Nickel 58:265
 - Oxidation 57:273
 - Oxide 57:273
- Rhizopus-Arrhizus 58:265
- Series-Analysis 58:265
- Support 57:273
- Copper-Cerium-Dioxide** 64:283
- Copper-Modified** 64:239
- Core-Annulus** 68:51
- Corn**
 - Drying 59:221, 60:39
 - Experimental-Study 59:221
 - Flotation 59:221
 - Flotation-Bed 60:39
 - Fluidized 60:39
 - Fluidized-Bed 59:221
 - Kinetics 59:221, 60:39
 - Modeling 60:39
- Correct**
 - Mathematical-Description 66:149, 66:151
 - Model 66:149, 66:151
 - Packed-Column 66:149, 66:151
- Corrected-Fick's-Law** 61:123
- Correlated** 64:7
- Correlation**
 - Acid 63:189
 - Adsorption 64:85
 - Adsorption-Energy 64:85
 - Carbon-Dioxide 66:217
 - Component 64:85
 - Corresponding-States 55:139, 66:217
 - Dimension 64:157
 - Equivalent 63:189
 - Estimation 63:189
 - Experimental-Data 43:B43
 - Four-Parameter 55:139
 - Gas-Liquid-Contactor 64:157
 - Generalized-Langmuir-Freundlich-Isotherm-Equation 64:85
 - Heat-Transfer 55:39
 - Horizontal-Pipe 55:39
 - Humic-Acid 63:189
 - Hydrocarbon 66:217
 - Linear-Type 43:B43
 - Liquid-Solid-Flow 55:39
 - Mass-Transfer-Coefficient 63:157
 - Mathematical-Model 43:B43
 - Michaelis-Menten-Kinetics 43:B43
 - Mixed-Gas 64:85
 - Polar-Substance 55:139
 - Product-Inhibition 43:B43
 - Pulsed-Baffled-Reactor 63:157
 - Regenerated 63:189
 - Scale-Up 63:157
 - Solid-Surface 64:85
 - System 66:217
 - Ultrafiltration-Membrane-Reactor 43:B43
 - Vapor-Liquid-Equilibrium 66:217

- Vapor-Pressure 55:139
- Correlation-Constant** 60:97
- Corresponding-States**
 - Acentric-Factor 66:35
 - Alkane 66:35
 - Application 66:35
 - Carbon-Dioxide 66:217
 - Correlation 55:139, 66:217
 - Critical-Constant 66:35
 - Four-Parameter 55:139
 - Hydrocarbon 66:217
 - Long-Chain 66:35
 - Polar-Substance 55:139
 - Suitable 66:35
 - System 66:217
 - Vapor-Liquid-Equilibrium 66:217
 - Vapor-Pressure 55:139
- Corrugated-Sheet** 53:55
- Corrugated-Wall** 54:23
- Cosolvent** 59:303
- Cosorb-Solution** 59:243
- Cost** 61:41
- Couette-Flow**
 - Chemical-Reaction 68:11
 - Convective-Diffusive-Mass-Transfer 68:11
 - Convective-Diffusive-Transport 61:63
 - Integral-Spectral-Approach 68:11
 - Mathematical-Formulation 68:11
 - Numerical-Illustration 68:11
 - Wall-Reaction 61:63
- Countercurrent** 56:59
- Countercurrent-Flotation-Circuit** 59:7
- Coupling**
 - Circular-Tube 55:103
 - External 55:103
 - Free-Convection 55:103
 - Heat-Transfer 55:103
 - Immobilized-Enzyme-Reactor 43:B93
 - Kinetic-Process 43:B93
 - Laminar-Flow 55:103
 - Thermodynamic-Equilibrium 43:B93
 - Two-Substrate 43:B93
 - Vertical-Tube 55:103
- Cow-Manure** 54:B9
- Cracking**
 - Adsorption 54:115
 - Catalyst 58:7
 - Commercial 58:7
 - Deactivation 54:115, 58:7
 - Diffusion 54:115
 - Hexane 54:115
 - Isopropylbenzene 58:7
 - Kinetic-Modeling 58:7
 - Mordenite 54:115
 - Oligomerization 54:115
 - Propene 54:115
 - Silica-Alumina 58:7
 - Zeolite 54:115
- Creosote-Based** 45:B13
- Criterion** 60:81
- Critical-Angle** 44:157
- Critical-Condition** 55:45
- Critical-Constant** 66:35
- Critical-Pressure** 59:127
- Critical-Temperature** 54:147
- Cross-Flow**
 - Boundary-Layer 66:201
 - Dilute 60:31
 - Filtration 61:171
 - Flux 61:171
 - Interaction 66:201
 - Internal-Fouling 60:31
 - Latex 60:31
 - Membrane 60:31
 - Microporous-Filtration 60:31
 - Particle 61:171
 - Particle-Turbulence 66:201
 - Permeation 61:171
 - Steady-State 61:171
 - Suspension 60:31
 - Tube 66:201
 - Turbulent 66:201
- Cross-Flow-Filtration** 60:55
- Cross-Section** 56:33
- Crude-Oil**
 - Estimation 45:83, 51:151
 - Fraction 45:83, 51:151
 - Kinematic-Viscosity 51:151
 - Neural-Network 51:151
 - Petroleum 45:83, 51:151
 - Simple-Method 45:83
 - Viscosity 45:83
- Cryogenic-Liquid** 43:25
- Crystal-Growth** 53:125
- Crystal-Growth-Kinetics** 58:215
- Crystal-Growth-Rate-Function** 55:69
- Crystal-Size-Distribution** 46:B35
- Crystallization** 59:143
- Crystallization-Kinetics-Data** 55:69
- Crystallizer**
 - Abrasion 63:85
 - Breakage-Phenomena 63:85
 - Crystal-Growth 53:125
 - Estimation 53:125
 - Mechanically-Stirred 63:85
 - Rate-Function 53:125
 - Size-Dependent 53:125
- Cultivation** 62:121
- Culture**
 - Acetobacter-Aceti 54:B15
 - Estimation 61:35
 - Fed-Batch 61:35
 - Growth 54:B15
 - Kinetic-Model 54:B15
 - 1-Lysine-Production 61:35
 - Modeling 61:35
 - Neural-Network 61:35
 - Online 61:35
 - State 61:35
 - Submerged 54:B15
- Current** 66:1
- Cutting** 56:27
- Cyclic-Regime** 43:B53
- Cyclodextrin** 61:247
- Cyclodextrin| β - \rightarrow** 61:247
- Cyclohexane** 50:165
- Cyclohexene** 50:165
- Cyclone-Reactor**
 - Circulating 45:9
 - Efficiency 45:9, 48:83
 - Gas 45:9
 - Gas-Phase 48:83
 - Heat-and-Mass-Transfer 45:9
 - Heat-Transfer 48:83
 - Isocyanuric-Acid 62:13
 - Measurement 48:83
 - Reactor-Wall 45:9
 - Single 45:9
 - Solid-Phase 48:83
 - Sublimation 62:13
 - Wall 48:83
- Cyclonic-Separator** 56:135
- Cylinder** 61:113
- Cylindrical** 49:55
- Cylindrical-Collector** 58:109
- Cylindrical-Duct** 56:33
- Cylindrical-Geometry** 64:353
- Cylindrical-Probe** 44:141
- D-Sorbitol** 45:B5
- Darcy** 50:33
- Data-Correlation** 59:265
- Deacidification** 55:B29
- Deactivation**
 - Adsorption 54:115
 - Behavior 43:11
 - Butanol 65:159
 - Calculation 55:125
 - Catalyst 43:11, 46:109, 58:7
 - Change 43:11
 - Coke 55:125
 - Commercial 58:7
 - Comparison 55:125
 - Concentration-Dependent 43:1
 - Cracking 54:115, 58:7
 - Dehydrogenation 46:109
 - Diffusion 54:115
 - Fixed-Bed-Catalytic-Reactor 43:1
 - Hexane 54:115
 - Immobilized 65:159
 - Isopropylbenzene 58:7
 - Isothermal 43:1
 - Kinetic-Modeling 58:7
 - Kinetics 55:125
 - Lipozyme 65:159
 - Method 55:125
 - Methylcyclohexane 46:109
- Mixture 43:11
- Model 43:11
- Mordenite 54:115
- Oligomerization 54:115
- Palliate 51:167
- Parallel-Reaction 51:167
- Parametric-Study 43:1, 51:167
- Pore-Size 43:11
- Propene 54:115
- Pt-Sn/Al₂O₃ 46:109
- Reaction 43:11
- Series-Parallel-Reaction 51:167
- Silica-Alumina 58:7
- Single-Pellet 43:11
- Support 43:11
- Supported-Catalyst 43:11
- Temperature 51:167, 65:159
- Time-Sequence 51:167
- Water-Content 65:159
- Zeolite 54:115
- Dead-Zone** 64:353
- Deashing**
 - Biomass 60:49
 - Charcoal 57:9
 - Charcoal-Oil-Water-Mixture 60:49
 - Energetical-Valorization 60:49
 - Liquid-Fuel 60:49
 - Oil-Agglomeration-Process 57:9
 - Operating-Parameter 57:9
- Decay** 47:105
- Decomposition**
 - Absorption 43:75
 - Aerosol 64:239
 - Characterization 64:239
 - Copper-Modified 64:239
 - High-Temperature 64:239
 - Higher-Alcohol 64:239
 - Nitrogen-Oxide 43:75
 - Nitrous-Acid-Formation 43:75
 - Process 64:239
 - Synthesis 64:239
 - Zinc-Chromite 64:239
- Decontamination** 57:53
- Deflected** 43:127
- Degassing-Effect** 66:21
- Degrading**
 - Constant-Biomass-Hold-Up 45:B35
 - Continuous-Stirred-Tank-Bioreactor 50:B1, 62:67
 - Development 45:B35
 - Fluidized-Bed-Bioreactor 45:B35
 - Inhibitory-Substrate 50:B1
 - Operational-Range 50:B1
 - Phenol 45:B35, 62:67
 - Range 62:67
 - Lipozyme 62:67
 - Stability 62:67
- Dehydration** 43:59
- Dehydrogenation**

- Catalyst 46:109
- Cyclohexane 50:165
- Cyclohexene 50:165
- Deactivation 46:109
- Methylcyclohexane 46:109
- Nickel 50:165
- Platinum 50:165
- Pt-Sn/Al₂O₃ 46:109
- Supported-Catalyst 50:165
- Demarcate** 57:261
- Denaturation** 49:B29
- Denitrification**
 - Application 65:133
 - Biofilm-Reactor 65:227
 - Biofilter 65:133
 - Dynamic-Modeling 65:133
 - Generalized-Approach 65:133
 - Kinetics 65:227
 - Rotating-Disk 65:227
 - Simulation 65:133
 - Waste-Water 65:133
- Dense** 64:99
- Density**
 - Bacterial-Aggregate 44:B1
 - Biomass-Retention 44:B1
 - Critical-Pressure 59:127
 - Estimation 59:127
 - Heat 59:127
 - Liquid 59:127
 - Pure-Substance 59:127
 - Structured-Model 44:B1
 - Vaporization 59:127
 - Varying-Size 44:B1
- Density-Independent** 61:213
- Dependence**
 - 2nd-Virial-Coefficient 56:73
 - Heat-Capacity 52:31
 - Liquid 52:31
 - Molecular-Structure 52:31
 - Temperature 52:31, 56:73
- Deposition**
 - A-Si-H 58:1
 - Aerosol 58:109
 - Comparison 58:1
 - Cylindrical-Collector 58:109
 - Fibrous-Particle 58:109
 - Flexible 58:109
 - Plasma-Enhanced 58:1
 - Stiff 58:109
 - Theoretical-Study 58:109
 - Two-Reactor-Arrangement 58:1
- Depth** 51:B17
- Description**
 - Analogous 53:89
 - Bubble-Column 53:89
 - Chemical-Reaction 57:115
 - Dusty-Gas 57:115
 - Fluidized-Bed 61:73
 - Gas-Solid-Fluidized-Bed 53:89
 - Global 61:73
 - Hydrodynamics 53:89
 - Local 61:73
 - Mass-Transport 57:115
 - Model 57:115
 - Modeling 61:73
 - Porous-Medium 57:115
 - Structure 61:73
 - Turbulent 61:73
- Design**
 - Air-Core 56:135
 - Airlift-Fluidized-Bed 49:89, 55:143, 55:145
 - Algorithm 65:77
 - Application 43:B19
 - Bioreactor 43:B19, 51:B63, 55:B73, 57:B1
 - Catalyst 53:1, 64:69
 - Comparative-Study 60:75
 - Continuous-Transport 53:B1
 - Cyclonic-Separator 56:135
 - Deterministic-Chaos 53:75
 - Diffusion 53:1
 - Dry 61:203
 - Efficient 65:77
 - Equation 51:B63, 55:B73, 65:77
 - Equipped 57:B1
 - Extractor 57:229
 - Factor 53:1
 - Fixed-Bed-Reactor 47:B11
 - Fluid 55:B73
 - Fluidized-Bed 53:75, 60:75
 - Fractal 64:69
 - Gas-Transfer 57:B1
 - High-Rate 57:B1
 - Hollow-Fiber 51:B63, 55:B73
 - Hollow-Fiber-Bioreactor 65:77
 - Imaging 56:135
 - Immobilized-Enzyme 53:B1
 - Implication 56:135
 - Importance 61:203
 - Intraparticle 53:1
 - Isotropic-Turbulence 43:B19
 - Kolmogorov-Theory 43:B19
 - Mass-Transfer 49:89, 55:143, 55:145
 - Mathematical-Model 43:B19
 - Maxwell-Stefan-Approach 57:229
 - Michaelis-Menten Kinetics 51:B63
 - Modeling 49:89, 55:143, 55:145, 56:135
 - Morphology 64:69
 - Nonisothermal-Reactor 47:17
 - Operation 53:75
 - Operational 55:143
 - Operational-Parameter 49:89, 55:145
 - Optimization 49:89, 55:143, 55:145
 - Parameter 55:143
 - Particle 53:1
 - Performance 57:B1
 - Power-Law 55:B73
 - Pressure-Drop 61:203
 - Process-Optimization 53:B1
 - Reaction-Kinetics 53:1
 - Reactor 53:B1
 - Respect 55:143
 - Self-Inhibitory-Substrate 47:B11
 - Separator 56:135
 - Strategy 53:B1
 - Tuyere 60:75
 - Variable-Density-System 47:17
 - Venturi-Injector 57:B1
 - Venturi-Scrubber 61:203
 - Zero-Order-Limit 51:B63
- Design-Criteria** 45:B57
- Design-Parameter** 49:107
- Desorption** 46:1
- Determination** 46:119
- Determination**
 - 2nd-Virial-Coefficient 47:113
 - Aerated 59:187
 - Alginate 56:B9
 - Aspergillus-Niger 62:215
 - Bioreactor 59:187
 - Bubble 59:187
 - Calcined 47:1
 - Calcium 56:B9
 - Citric-Acid-Production 62:215
 - Computer-Assisted-Image-Analysis 49:141
 - Configuration-Factor 45:75
 - Convective-Coefficient 57:285
 - Development 49:141
 - Diffusion-Coefficient 56:B9
 - Dissolution 48:119
 - Effective-Diffusivity 57:285
 - End-Use 63:19
 - Entrainment 59:187
 - Fluidized-Bed 48:119
 - Gas 47:1
 - Gas-Absorption 57:67
 - Glucose 56:B9
 - Granulometric-Distribution 49:141
 - Growth 48:119
 - Heat-Transfer 45:75
 - Hydrogen-Chloride 47:1
 - Identification 56:B9
 - Kinetic-Parameter 47:1
 - Kinetics 48:119
 - Limestone 47:1
 - Liquid-Liquid-Dispersion 49:141
 - Maintenance-Coefficient 62:215
 - Malic-Acid 56:B9
 - Mass-Transfer 59:187
 - Mass-Transfer-Coefficient 57:67
 - Membrane 56:B9
 - Model 56:B9
 - Monte-Carlo-Method 45:75
 - Nonparametric-Method 54:1
 - Operating-Condition 63:19
 - Optimization 63:19
 - Packed-Column 57:67
 - Parameter 59:187
 - Particle 54:1
 - Physical-System 57:67
 - Pressure-Measurement 47:113
 - Property 63:19
 - Pure-Gase 57:285
 - Radiative 45:75
 - Reaction 47:1
 - Sequential-Method 63:19
 - Settling 54:1
 - Single-Pellet 57:285
 - Slurry-Bubble-Column 54:1
 - Sodium-Perborate-Tetrahydrate 48:119
 - Solid-Liquid-Dispersion 49:141
 - Solid-Solid-Dispersion 49:141
 - Surface 59:187
 - Technique 57:67
 - Terpolymer 63:19
 - Thermal 45:75
 - Thermogravimetry 47:1
 - Velocity 54:1
 - Yield 62:215
- Deterministic-Analysis** 64:149
- Deterministic-Chaos** 53:75
- Development**
 - Adaptive 63:65
 - Batch-Distillation 54:95
 - Batch-Process 63:65
 - Computer-Assisted-Image-Analysis 49:141
 - Constant-Biomass-Hold-Up 45:B35
 - Control 63:65
 - Degrading 45:B35
 - Determination 49:141
 - Dual-Mode-Tomograph 56:175
 - Enzymatic-Transformation 65:27
 - Experimental-Verification 58:123
 - Flexible 63:65
 - Fluidization 68:7
 - Fluidized-Bed 68:7
 - Fluidized-Bed-Bioreactor 45:B35
 - Granulometric-Distribution 49:141
 - Heat 58:123
 - Liquid-Liquid-Dispersion 49:141
 - Mass-Transfer 58:123
 - Mini-Tapered 68:7
 - Model 48:17, 56:101, 58:123, 65:27
 - Momentum 58:123

- Neural-Network 63:65
- Nonisothermal-Water-Gas-Shift-Reactor 48:17
- Oxidase 65:27
- Particle 68:7
- pH 65:27
- Phenol 45:B35
- Polyphenol 65:27
- Simulation 48:17, 54:95
- Sinapine 65:27
- Solid-Liquid-Dispersion 49:141
- Solid-Liquid-Mixing 56:101
- Solid-Solid-Dispersion 49:141
- Spray-Drying 58:123
- Stability 68:7
- System 68:7
- Temperature 65:27
- Thermogravimetric-Analyzer 68:7
- Three-Component-Imaging 56:175
- Tomographic-Technique 56:101
- Trametes-Versicolor 65:27
- Trend 54:95
- Verification 48:17
- Devils-Comb** 64:63
- Dextran** 51:B43
- Dextranucrase** 51:B43
- Dialysis** 62:73
- Difference**
 - C-Terminal-Region 65:257
 - Carbon-Dioxide 68:63
 - Carbon-Monoxide 68:63
 - Immunogenicity 65:257
 - Intact-Insulin 65:257
 - Methanation 68:63
 - Peptide 65:257
 - Selectivity 68:63
- Different**
 - 1,2-Ethanediol 52:41
 - 2-Methoxyethanol 52:41
 - Adsorption 66:223
 - Amyloglucosidase 51:B17
 - Aqueous-Solution 66:223
 - Axial-Dispersion 52:63
 - Basic-Dye 66:223
 - Bed 51:B17
 - Binary-Mixture 52:41
 - Bunch 66:223
 - Depth 51:B17
 - Fermentation 51:B17
 - Fixed-Bed 52:63
 - Kinematic-Viscosity 52:41
 - Level 51:B17
 - Liquid-Flow 52:63
 - Metallic-Foam 52:63
 - Packed 52:63
 - Palm-Fruit 66:223
 - Particle 66:223
 - Removal 66:223
 - Reticulated 52:63
 - Solid-State 51:B17
 - Structure 52:63
 - Temperature 52:41
 - Temperature-Variation 51:B17
- Diffuser** 49:55
- Diffusion**
 - Adsorption 54:115
 - Adsorption-Process 60:81
 - Analogy 61:113
 - Analysis 60:81
 - Apparent 60:81
 - Catalyst 53:1, 61:113
 - Chemical-Vapor-Deposition-Reactor 57:127
 - Convection 61:113
 - Cracking 54:115
 - Criterion 60:81
 - Cylinder 61:113
 - Deactivation 54:115
 - Design 53:1
 - Diffusion-Convection 60:81
 - Driving-Force 60:81
 - Enzyme-Reaction 56:B61
 - Equivalence 60:81
 - Extended-Linear-Model 60:81
 - Factor 53:1
 - Generalized-Analysis 56:B61
 - Geometry 61:113
 - Hexane 54:115
 - Immobilized 56:B61
 - Internal 56:B61
 - Intraparticle 53:1
 - Large-Pore 60:81
 - Material 60:81
 - Mordenite 54:115
 - Multicomponent 57:127
 - Multienzyme-Reaction 56:B61
 - Multiple-Wafer 57:127
 - Oligomerization 54:115
 - Particle 53:1, 61:113
 - Phenomena 57:127
 - Propene 54:115
 - Reaction 61:113
 - Reaction-Kinetics 53:1
 - Slab 61:113
 - Zeolite 54:115
- Diffusion-Coefficient** 56:B9
- Diffusion-Convection** 60:81
- Diffusion-Equation** 55:135
- Diffusion-Limited** 64:77
- Diffusion-Phenomena** 46:B21
- Diffusional-Characteristics** 55:B35
- Diffusivity**
 - Evaluation 61:7
 - Inversion 61:7
 - Ion-Exchange 61:7
 - Organic-Electrolyte 66:111
 - Reaction-Rate 61:7
 - Solution 61:7
 - Sucrose 61:7
 - Water 66:111
- Digester** 55:B55
- Digestion** 56:B109
- Diglycolamine** 44:107
- Dilute** 60:31
- Dimension**
 - Box-Counting 64:169
 - Characterization 64:169
 - Correlation 64:157
 - Embedding 64:169
 - Flow-Regime 64:169
 - Gas-Liquid-Contactor 64:157
 - Multiphase-Reactor 64:169
- Dimensionless** 65:213
- Dinitrogen-Oxide** 48:31
- Dipeptide** 49:B41
- Direct-Measurement** 47:B35
- Direct-Test** 60:147
- Discontinuous-Boundary-Condition** 47:169
- Discontinuous-Collocation-Polynomial** 51:83
- Discontinuous-Microfiltration-Backwash** 57:247
- Discrimination** 65:105
- Disk** 45:87
- Disordered-System** 49:1
- Dispersion**
 - Aqueous 67:97
 - Element 62:89
 - Evaporator 62:89
 - Influence 62:89, 67:97
 - Liquid 62:89
 - Longitudinal 62:89
 - Mass-Transfer 67:45
 - Modeling 67:45
 - Organic-Compound 67:45
 - pH 67:97
 - Polymer 67:45
 - Rheology 67:97
 - Spiral 62:89
 - Stability 67:97
 - Suspended-Growth-System 44:B15
 - Temperature 67:97
 - Thin-Layer 62:89
 - Titanium-Dioxide 67:97
 - Volatile 67:45
- Dispersion-Free-Interface** 49:35
- Displacement** 49:B29
- Disruption** 55:B67
- Dissolution**
 - Determination 48:119
 - Fluidized-Bed 48:119
 - General 61:161
 - Growth 48:119
 - Kinetic-Invariant-Model 61:161
 - Kinetics 48:119
 - Lactose 53:B25
 - Large-Polydisperse-Particle 61:161
 - Mass-Transfer 66:57
 - Mathematical-Model 53:B25
- Sodium-Perborate-Tetrahydrate 48:119
- Solid 66:57
- Distillation**
 - Continuous-Collocation-Polynomial 51:83
 - Discontinuous-Collocation-Polynomial 51:83
 - Dynamic-Optimization 51:83
 - Mass-Transfer 57:177
 - Modeling 57:177
 - Multicomponent 57:177
 - Multicomponent-Batch-Process 51:83
 - Policy 51:83
- Distillation-Column**
 - Complex 47:119
 - Equation 46:97
 - Ether-Production 57:219
 - Fuel 57:219
 - Heuristics 46:97
 - Operability 44:81
 - Optimum-Sequence 46:97
 - Oscillatory 57:219
 - Packed 57:219
 - Reactive 57:219
 - Rule-of-Thumb 46:97
 - Setting 47:119
 - Transport-Phenomena 57:219
 - Vapor-Liquid 57:219
- Distribution**
 - Amberlite 62:231
 - Baffled 66:1
 - Corrugated-Sheet 53:55
 - Current 66:1
 - Eddy 67:83
 - Electrochemical-Reactor 66:1
 - Equilibrium 62:231
 - Fluidized 60:89
 - Gas 60:89
 - Gas-Flow 53:55
 - High-Pressure 60:89
 - Influence 67:83
 - Liquid 67:83
 - Liquid-Solid-Flow 67:83
 - Liquid-Film 59:259
 - Local 66:1
 - Mass-Transfer 66:1
 - Measurement 53:55
 - Modeling 53:55
 - Non-Maintained 67:83
 - Organic-Solution 62:231
 - Packing 53:55
 - Parallel-Plate 66:1
 - Particle-Size 60:89
 - Penicillin-G 62:231
 - Presence 67:83
 - Residence-Time 59:259
 - Segregation 60:89
 - Solid 60:89, 67:83
 - Staying-Time 67:83
 - Structured 53:55
 - Unbaffled 66:1

- Water 62:231
- Wide 60:89
- Wiped 59:259
- Distributor**
- Bubble 56:95
- Capacitance 56:95
- Fluidized-Bed 56:95
- Formation 56:95
- Imaging 56:95
- Liquid-Distribution 48:49
- Packed-Bed 48:49
- Rational-Description 48:49
- Real-Time 56:95
- Trickle-Flow 48:49
- Double-Salt** 52:89
- Doughnut-Column** 45:87
- Downcomer**
- Efficiency 63:167
- Gas-Liquid-Separator 57:B7
- Gas-Hold-Up 57:B7
- Internal-Loop-Airlift-Reactor 57:B7
- Layout 63:167
- Pattern 63:167
- Relationship 57:B7
- Riser 57:B7
- Tray 63:167
- Downjet-Loop-Reactor** 49:49
- Draft-Tube**
- Entrainment 66:105
- Fluidized-Bed 66:105
- Hydrodynamics 60:155
- Internal-Circulation 66:105
- Mixing 59:273
- Position 60:155
- Slurry-Bubble-Column 60:155
- Solid 66:105
- Suspension 59:273
- Tall-Vessel 59:273
- Drainage-Rate** 50:69
- Dried-Ground-Corn** 43:B103
- Driving-Force** 60:81
- Dry**
- Calcium-Oxide 46:119
- Design 61:203
- Desulfurization 46:119
- Importance 61:203
- Kinetics 46:119
- Pressure-Drop 61:203
- Venturi-Scrubber 61:203
- Dry-Moldy-Bran** 46:B53
- Drying**
- Corn 59:221, 60:39
- Experimental-Study 59:221
- Flotation 59:221
- Flotation-Bed 60:39
- Fluidized 60:39
- Fluidized-Bed 59:221
- Kinetics 59:221, 60:39
- Modeling 60:39
- Protein-Product 58:197
- Dual-Limitation** 48:B9
- Dual-Mode-Tomograph** 56:175
- Dual-Turbine** 67:215
- Duct** 62:51
- Dusty-Gas** 57:115
- Dynamic-Approach** 65:81
- Dynamic-Control** 68:41
- Dynamic-Interface** 56:143
- Dynamic-Liquid-Hold-Up** 62:237
- Dynamic-Measurement**
- Analysis 64:179
- Boiler 64:179
- Direct-Measurement 47:B35
- Fermentation-Broth 47:B35
- Gas-Hold-Up 47:B35
- Practical-Approach 64:179
- Residual 47:B35
- Viscous 47:B35
- Dynamic-Optimization** 51:83
- Dynamic-Response** 43:B1
- Dynamic-Transport** 57:91
- Dynamics**
- Anaerobic 55:B55
- Anaerobic-Digestion 43:B81
- Analysis 43:B81
- Backmixing 48:71
- Bulk-Copolymerization 48:71
- Comparison 55:B55
- Control 55:B55, 67:103
- Digester 55:B55
- Filter 58:145
- Gel-Effect 48:71
- Hydrodynamics 58:145
- Influence 48:71
- Laminar-Flow 58:145
- Mesophilic 55:B55
- Multivariable-Control 43:B81
- Nonlinear-System 67:103
- Performance 55:B55
- Rate-Parameter 48:71
- Rotary 58:145
- Sludge 55:B55
- Steady-State 67:103
- Theoretical-Analysis 48:71
- Thermophilic 55:B55
- Tubular-Reactor 48:71
- Unstable 67:103
- Economical-Optimization** 64:307
- Eddy** 67:83
- Effect**
- Adsorption 49:B41
- Bioreactor 56:B15
- Cell 56:B15
- Dipeptide 49:B41
- Nonlinear-Kinetics 49:B41
- Oxygen-Transfer 56:B15
- Particle 56:B15
- Physical-Presence 56:B15
- Reverse-Phase-Column 49:B41
- Separation 49:B41
- Solid 56:B15
- Effective-Diffusivity** 57:285
- Effective-Interfacial-Area** 46:69
- Effectiveness** 55:81
- Effectiveness-Factor**
- Analytical-Solution 59:161
- Approximate 59:161
- Catalytic-Reaction 59:161
- Consumption 62:149
- Entrapped 49:B23
- Evaluation 49:B23
- Hollow-Fiber-Biofilm-Reactor 62:149
- Immobilized-Cell-Aggregate 59:309
- Immobilized-Enzyme 57:B23
- Inhibition-Kinetics 57:B23
- Linear-Product 57:B23
- Maximum 62:149
- Mixed-Type 57:B23
- Parallel 59:161
- Pattern 59:309
- Product-Inhibition 59:309
- Substrate 62:149
- Theoretical-Approach 49:B23
- Yeast-Cell-Column 49:B23
- Efficiency**
- Circulating 45:9
- Cyclone-Reactor 45:9, 48:83
- Downcomer 63:167
- Entrainment 57:237
- Gas 45:9
- Gas-Phase 48:83
- Heat-and-Mass-Transfer 45:9
- Heat-Transfer 48:83
- Layout 63:167
- Measurement 48:83
- Multicomponent 57:237
- Pattern 63:167
- Reactor-Wall 45:9
- Single 45:9
- Solid-Phase 48:83
- Tray 57:237, 63:167
- Wall 48:83
- Efficient**
- Algorithm 65:77
- Bessel-Function 44:B25
- Computation 44:B25
- Design 65:77
- Equation 65:77
- Hollow-Fiber-Bioreactor 65:77
- Integral 44:B25
- Effluent** 57:53
- Elaboration** 67:55
- Electrical-Tomography** 56:127
- Electrochemical-Reactor**
- Affecting 61:13
- Baffled 66:1
- Bromine 61:13
- Current 66:1
- Distribution 66:1
- Ethene 61:13
- Factor 61:13
- Kinetics 53:137
- Local 66:1
- Mass-Transfer 66:1
- Mathematical-Model 61:13
- Oxide 61:13
- Parallel-Plate 66:1
- Percolation 53:137
- Poly-(18-Dibenzo-6-Crown) 53:137
- Porous-Electrode 53:137
- Production 61:13
- Pulsed 53:137
- Relative-Concentration 61:13
- Sieve-Plate 61:13
- Synthesis 53:137
- Unbaffled 66:1
- Electrodialysis**
- Acetate-Ion 51:1
- Aqueous-Solution 51:1
- Maxwell-Stefan-Description 57:163
- Modeling 57:163
- Nitrate-Ion 51:1
- Permselectivity 51:1
- Prediction 51:1
- Electrolytic**
- Convective-Diffusion 68:69
- Externally-Imposed 68:69
- Force-Field 68:69
- Manganese-Metal 54:167
- Mechanism 54:167
- Nitriding 54:167
- Numerical-Solution 68:69
- Electroplating-Line** 49:161
- Electroporator** 56:B75
- Electrostatic-Interaction** 57:B15
- Electrothermal-Desorption** 53:157
- Element** 62:89
- Elevated** 54:63
- Elevated-Pressure** 47:33
- Elliptic-Integral** 66:231
- Elution**
- Continuous-Annular-Chromatography 55:B19
- Glucose-Fructose-Mixtures 65:209
- Profile 65:209
- Protein-Mixture 55:B19
- Separation 55:B19, 65:209
- Embedding** 64:169
- Emission-Tomography** 56:109
- Emulsion**
- Carrier 63:127, 66:11
- Coarse 67:37
- Creosote-Based 45:B13
- Facilitated 63:127, 66:11
- Fine 67:37
- Liquid 63:127, 66:11
- Membrane 63:127, 66:11
- Mixture 67:37
- Modeling 63:127, 66:11
- Rheology 45:B13
- Storage-Loss-Modulus 67:37

- Viscosity 67:37
- Wood-Preservative 45:B13
- End-Use** 63:19
- Endoglucanase** 59:315
- Energetical-Valorization** 60:49
- Energy** 45:123
- Energy-Balance-Approach** 63:105
- Energy-Density** 50:59
- Energy-Dissipation** 63:105
- Energy-Input** 45:99
- Engineering** 56:127
- Engulfment** 45:25
- Enhancement** 51:93
- Enrichment**
 - Aqueous-Phase 59:297
 - Back-Extraction 59:297
 - Chemo-Autotrophic-Biogas 58:71
 - Kinetics 58:71
 - Mechanism 58:71
 - Methane 58:71
 - Partitioning-Behavior 59:297
 - Protein 59:297
 - Purification 58:71
 - Reversed-Micelle 59:297
- Entrainment**
 - Aerated 59:187
 - Bioreactor 59:187
 - Bubble 59:187
 - Determination 59:187
 - Draft-Tube 66:105
 - Efficiency 57:237
 - Fluidized-Bed 66:105
 - Internal-Circulation 66:105
 - Mass-Transfer 59:187
 - Multicomponent 57:237
 - Parameter 59:187
 - Solid 66:105
 - Surface 59:187
 - Tray 57:237
- Entrapped**
 - Alginate-Bead 55:B29
 - Biotransformation 45:B5
 - Continuous-Fluidized-Bed 55:B29
 - D-Sorbitol 45:B5
 - Decacidification 55:B29
 - Effectiveness-Factor 49:B23
 - Ethanol-Production 47:B1
 - Evaluation 49:B23
 - Gluconobacter-Suboxydan 45:B5
 - Grape 55:B29
 - L-Sorbose 45:B5
 - Must 55:B29
 - Polyacrylamide-Gel 45:B5
 - Process 55:B29
 - Schizosaccharomyces 55:B29
 - Theoretical-Approach 49:B23
 - Yeast-Cell-Column 47:B1, 49:B23
- Enumeration** 45:149
- Environmental** 56:159
- Enzymatic-Hydrolysis**
 - Batch 65:187, 65:195
 - Comparison 65:195
 - Complex 52:B13
 - Enzymatic-Kinetics 65:187
 - Enzyme 52:B13
 - Hydrolysis 65:187
 - Mixture 52:B13
 - Modeling 52:B13
 - Performance 65:195
 - Potato-Pulp 52:B13
 - Protein 65:187, 65:195
 - Simulation 52:B13
 - Stirred-Reactor 65:187, 65:195
 - Torus-Reactor 65:195
 - Wheat 65:187, 65:195
- Enzymatic-Kinetics** 65:187
- Enzymatic-Transformation** 65:27
- Enzyme**
 - Aliquat-336 59:303
 - Application 52:B49
 - ARMAX 50:B45
 - Bacillus-Subtilis 59:303
 - Coefficient 55:B1
 - Column 55:B1
 - Complex 52:B13
 - Concentration 59:303
 - Cosolvent 59:303
 - Enzymatic-Hydrolysis 52:B13
 - Extraction 55:B1
 - Fermentation 50:B45
 - Mass-Transfer 55:B1
 - Mixture 52:B13
 - Modeling 50:B45, 52:B13
 - Obstacle 52:B49
 - Opportunity 52:B49
 - Potato-Pulp 52:B13
 - Purification 59:303
 - Reversed-Micellar-Extraction 46:B69
 - Reversed-Micelle 59:303
 - Separation 59:303
 - Sieve-Plate 55:B1
 - Simulation 52:B13
 - State-Estimation 50:B45
 - Temperature-Effect 46:B69
 - Waste-Treatment 52:B49
- Enzyme | Crude**→ 61:247
- Enzyme | Immobilized**→
 - Continuous-Transport 53:B1
 - Design 53:B1
 - Effectiveness-Factor 57:B23
 - Electrostatic-Interaction 57:B15
 - Inhibition-Kinetics 57:B23
 - Kinetics 57:B15
 - Linear-Product 57:B23
 - Mixed-Type 57:B23
 - Modeling 57:B15
 - pH-Change 57:B15
 - Process-Optimization 53:B1
 - Reaction-Generated 57:B15
 - Reactor 53:B1
 - Strategy 53:B1
- Enzyme-Activity**
 - Constant 45:B1
 - Continuous-Flow-Reactor 45:B1
 - Control 51:B11
 - Stirred-Bioreactor 51:B11
- Enzyme-Catalysis** 44:B47
- Enzyme-Kinetics** 56:B87
- Enzyme-Linked-Immuno-sorbent-Assay** 65:87
- Enzyme-Reaction** 56:B61
- Enzyme-Reactor | Immobilized**→ 43:B93
- Enzyme-Refolding** 65:151
- Enzyme-System | Immobilized**→
 - Bioreactor 61:241
 - Fluidized-Bed 61:241
 - Magnetically-Stabilized 61:241
 - Mass-Transfer 61:241
 - Nonisothermal 58:275
 - Packed 58:275
 - Tool 61:241
 - Tubular-Reactor 58:275
- Epitaxial-Growth** 62:43
- Equation**
 - Algorithm 65:77
 - Bioreactor 51:B63, 55:B73
 - Design 51:B63, 55:B73, 65:77
 - Distillation-Column 46:97
 - Efficient 65:77
 - Fluid 55:B73
 - Heuristics 46:97
 - Hollow-Fiber 51:B63, 55:B73
 - Hollow-Fiber-Bioreactor 65:77
 - Michaelis-Menten-Kinetics 51:B63
 - Optimum-Sequence 46:97
 - Power-Law 55:B73
 - Rule-of-Thumb 46:97
 - Zero-Order-Limit 51:B63
- Equation-of-State**
 - Application 67:27
 - Chain-of-Rotator 46:29
 - Equilibrium-Vaporization 46:29
 - Extension 67:27
 - Group-Contribution 46:29
 - Near-Critical-Region 67:27
 - Oil 46:29
 - Patel-Teja-Equation 67:27
 - Prediction 52:93
 - Pure-Component-Property 52:93
 - Subcritical-Range 52:93
 - Three-Parameter 67:27
 - Wong-Sandler-Mixing-Rule 67:27
- Equilibrium**
 - Activated 59:205
 - Adsorption 48:173, 59:205
 - Amberlite 62:231
 - Amine 65:47
 - Blowdown-Policy 48:173
 - Carbon 59:205
 - Distribution 62:231
 - Extractant 65:47
 - Extraction 65:47
 - Lactic-Acid 65:47
 - Nonlinear-Analysis 48:173
 - Organic-Solution 62:231
 - Penicillin-G 62:231
 - Pressure-Swing 48:173
 - Reactive 65:47
 - Separation 48:173
 - Stochastic-Model 59:205
 - Water 62:231
- Equilibrium-Isotherms** 46:B93
- Equilibrium-Vaporization** 46:29
- Equipped**
 - Agitated-Vessel 58:135
 - Baffle 58:135
 - Bioreactor 57:B1
 - Design 57:B1
 - Evaporator 56:51
 - Gas-Transfer 57:B1
 - Heat-Transfer 58:135
 - High-Rate 57:B1
 - Jacketed 58:135
 - Liquid 56:51
 - Nonstandard 58:135
 - Performance 57:B1
 - Residence-Time 56:51
 - Spiral-Element 56:51
 - Thin-Layer 56:51
 - Venturi-Injector 57:B1
- Equivalence**
 - Adsorption-Process 60:81
 - Analysis 60:81
 - Apparent 60:81
 - Corrected-Fick's-Law 61:123
 - Criterion 60:81
 - Diffusion 60:81
 - Diffusion-Convection 60:81
 - Driving-Force 60:81
 - Extended-Linear-Model 60:81
 - Fixed-Bed 61:123
 - Ion-Exchange-Process 61:123
 - Large-Pore 60:81
 - Material 60:81
 - Modeling 61:123
 - Nernst-Planck-Law 61:123
- Equivalent** 63:189
- Escherichia-Coli** 56:B75
- Estimation**
 - Absence 43:41
 - Acid 63:189
 - Activated-Carbon-Column 58:239
 - Apparent-Yield-Stress 45:B49
 - Application 51:77
 - Continuous-Stirred-Tank-Reactor 58:239

- Correlation 63:189
 - Critical-Pressure 59:127
 - Critical-Temperature 54:147
 - Crude-Oil 45:83, 51:151
 - Crystal-Growth 53:125
 - Crystallizer 53:125
 - Culture 61:35
 - Density 59:127
 - Equivalent 63:189
 - Experiment 53:193, 58:239
 - Extraction-Column 45:133
 - Fast-Fourier-Transform 51:77
 - Fed-Batch 61:35
 - Fermentation-Broth 45:B49
 - Film 43:41
 - Fixed-Bed 53:193
 - Fixed-Bed-Reactor 51:77
 - Flow 53:193
 - Fraction 45:83, 51:151
 - Heat 59:127
 - Humic-Acid 63:189
 - Inorganic-Substance 54:147
 - Intraparticle-Kinetic-Parameter 58:239
 - Kinematic-Viscosity 51:151
 - Kinetic-Parameter 51:77, 53:193
 - L-Lysine-Production 61:35
 - Liquid 59:127
 - Low-Cost 45:B49
 - Maldistribution 53:193
 - Mass-Transfer 43:41
 - Mass-Transfer-Coefficient 45:133
 - Modeling 61:35
 - Neural-Network 51:151, 61:35
 - Numerical-Technique 45:133
 - Online 61:35
 - Petroleum 45:83, 51:151
 - Pure-Compound 59:101
 - Pure-Liquid 48:211
 - Pure-Substance 59:127
 - Rate-Function 53:125
 - Regenerated 63:189
 - Residual-Function-Method 59:101
 - Resistance 43:41
 - Simple-Method 45:83
 - Simulation 58:239
 - Size-Dependent 53:125
 - Solid-Liquid-Adsorption 58:239
 - State 61:35
 - Surface-Diffusivity 43:41
 - Thermal-Conductivity 48:211
 - Tracer 53:193
 - Transport 53:193
 - Vaporization 59:127
 - Vaporization-Heat 59:101
 - Viscometer 45:B49
 - Viscosity 45:83
 - Xanthan-Gum-Solution 45:B49
- Ethanol**
- Alcohol 48:B15
 - Azeotropic-Distillation 43:59
 - Batch 48:B15
 - Batch-Culture 44:B69
 - Bioconversion 43:B1
 - Block 61:233
 - Carrier 61:233
 - Cellulose 45:B27
 - Characteristics 54:63
 - Controlled-Hydrolysis 44:133
 - Dehydration 43:59
 - Dried-Ground-Corn 43:B103
 - Dynamic-Response 43:B1
 - Elevated 54:63
 - Evaporative-Loss 48:B15
 - Experimental-Study 54:221
 - Fermentation 45:B27, 48:B15, 54:221
 - Formation 44:133
 - Fructose 61:233
 - Gas 54:63
 - High-Concentration 44:B69
 - Immobilized-Cell-Packed-Bed-Bioreactor 43:B1
 - Kinetics 54:221
 - Macroapproach 54:221
 - Mass-Transfer 54:63
 - Mathematical-Modeling 54:221
 - Methanol 54:63
 - Mixed-Solvent-Entrainer 43:59
 - Modeling 48:B15
 - Modified-Ghose-Model 44:B69
 - Monosized 44:133
 - Oil-Extraction 43:B103
 - Perturbation 43:B1
 - Pressure 54:63
 - Process-Parameter 43:B1
 - Production 61:233
 - Reaction-Kinetics 44:133
 - Saccharification 45:B27
 - Saccharomyces-Cerevisiae 44:B69, 54:221, 61:233
 - Silica-Sphere 44:133
 - Simulation 45:B27
 - Simultaneous 45:B27
 - Size-Control 44:133
 - Sugar 43:B1
 - Temperature 54:63
 - Tetraethyl-Orthosilicate 44:133
 - Wood 61:233
- Ethanol-Production** 47:B1
- Ethene**
- Affecting 61:13
 - Bromine 61:13
 - Electrochemical-Reactor 61:13
 - Factor 61:13
 - Fischer-Tropsch-Synthesis 47:83
 - Mathematical-Model 61:13
 - Oxide 61:13
 - Periodic-Dosing 47:83
 - Production 61:13
 - Relative-Concentration 61:13
 - Sieve-Plate 61:13
- Ether-Production** 57:219
- Europium** 57:253
- Evaluate** 65:63
- Evaluation**
- Adsorption 65:81
 - Adsorption-Data 65:81
 - Biodegradation 56:B91
 - Calcium-Alginate 65:81
 - Coal 59:133
 - Column 65:81
 - Control-Strategy 59:133
 - Copper 65:81
 - Diffusivity 61:7
 - Dynamic-Approach 65:81
 - Effectiveness-Factor 49:B23
 - Entrapped 49:B23
 - Gasifier 59:133
 - Immobilized 65:81
 - Implementation 59:133
 - Inversion 61:7
 - Ion-Exchange 61:7
 - Kinetic-Parameter 56:B91
 - Kinetics 56:B91
 - Metal-Cutting 56:B91
 - Moment-Analysis 65:81
 - Moving-Bed 59:133
 - Oil 56:B91
 - Packed-Bed 65:81
 - Reaction-Rate 61:7
 - Solution 61:7
 - Stimulus-Response 65:81
 - Sucrose 61:7
 - Technique 65:81
 - Theoretical-Approach 49:B23
 - Yeast-Cell-Column 49:B23
 - Zoogloea-Ramigera 65:81
- Evaporation** 48:1
- Evaporation-Loss** 55:61
- Evaporative-Loss** 48:B15
- Evaporator**
- Dispersion 62:89
 - Element 62:89
 - Equipped 56:51
 - Influence 62:89
 - Liquid 56:51, 62:89
 - Longitudinal 62:89
 - Residence-Time 56:51
 - Spiral 62:89
 - Spiral-Element 56:51
 - Thin-Layer 56:51, 62:89
- Exact-Solution** 55:135
- Exhaust-Gas** 53:47
- Exit** 47:105
- Expansion** 51:45
- Experiment**
- Activated-Carbon-Column 58:239
 - Continuous-Stirred-Tank-Reactor 58:239
 - Estimation 53:193, 58:239
 - Fixed-Bed 53:193
 - Flow 53:193
 - Intraparticle-Kinetic-Parameter 58:239
 - Kinetic-Parameter 53:193
 - Liquid-Solid-Mass-Transfer 63:1
 - Low-Reynolds-Number 63:1
 - Maldistribution 53:193
 - Model 63:1
 - Packed-Bed 63:1
 - Particle 63:1
 - Simulation 58:239
 - Solid-Liquid-Adsorption 58:239
 - Tracer 53:193
 - Transport 53:193
 - Variously-Shaped 63:1
- Experimental** 52:79
- Experimental-Assessment** 43:B13
- Experimental-Data**
- Catalytic-Cracking 44:53
 - Correlation 43:B43
 - Fluidized-Bed 44:53
 - Heated 65:99
 - Inactivation 65:99
 - Interpretation 44:53
 - Kinetic-Model 44:53, 65:99
 - Linear-Type 43:B43
 - Mathematical-Model 43:B43
 - Michaelis-Menten-Kinetics 43:B43
 - Multistage-Reactor 44:53
 - Oil-Fraction 44:53
 - Product-Inhibition 43:B43
 - Single-Stage-Reactor 44:53
 - Strain 65:99
 - Strawberry-Product 65:99
 - Thermal 65:99
 - Ultrafiltration-Membrane-Reactor 43:B43
 - Yeast 65:99
- Experimental-Determination** 44:B41
- Experimental-Investigation** 59:281
- Experimental-Result** 46:B1
- Experimental-Set-Up** 49:11
- Experimental-Study**
- Acid 67:55
 - Boiler 66:159
 - Bone-Powder 67:55
 - Bubbling-Bed-Reactor 66:193
 - Catalytic-Partial-Oxidation 66:193
 - Corn 59:221
 - Corrugated-Wall 54:23
 - Drying 59:221
 - Elaberation 67:55
 - Ethanol 54:221
 - Fermentation 54:221
 - Finned-Tube 66:159

- Flotation 59:221
- Flowing 54:23
- Fluidized-Bed 59:221
- Gas 66:193
- Gas-Solid-Separator 66:159
- Gelatin-Production 67:55
- Grid-Generated 47:155
- Hydrodynamics 54:23
- Impact 66:159
- Isothermal 54:23
- Kinetics 54:221, 59:221, 67:55
- Liquid-Film 54:23
- Macroapproach 54:221
- Mathematical-Modeling 54:221
- Methane 66:193
- Micromixing 47:155
- Modeling 67:55
- Overall-Scheme 67:55
- Process 67:55
- Saccharomyces-Cerevisiae 54:221
- Synthesis 66:193
- Theoretical-Analysis 47:155
- Tubular-Column 54:23
- Turbulence 47:155
- Experimental-Technique** 48:41
- Experimental-Verification** 58:123
- Experimentation** 45:B67
- Expert-System** 51:B35
- Exploitation** 49:167
- Exploring** 57:75
- Extension** 67:27
- External** 55:103
- External-Loop** 62:35
- External-Loop-Airlift-Contactor** 66:91
- External-Loop-Airlift-Reactor**
 - Hydrodynamics 67:205
 - Mass-Transfer 67:205
 - Mixing 66:97
- External-Wall** 46:47
- Externally-Imposed** 68:69
- Extracellular-Product** 56:B1
- Extractant**
 - Acidic 60:63
 - Amine 65:47
 - Backward-Extraction 60:63
 - Equilibrium 65:47
 - Extraction 65:47
 - Forward-Extraction 60:63
 - Kinetics 60:63
 - Lactic-Acid 65:47
 - Monoester 60:63
 - Neodymium 60:63
 - Phosphonic-Acid 60:63
 - Reactive 65:47
- Extraction**
 - Amberlite 58:285
 - Amine 65:47
 - Barium-Chloride 49:167
 - Carbon-Dioxide 61:227
 - Carrier 58:285
 - Cell 58:285
 - Chromatography 64:307
 - Coefficient 55:B1
 - Column 55:B1
 - Comparison 61:227
 - Constant-Interface-Area 58:285
 - Conventional 61:227
 - Economical-Optimization 64:307
 - Enzyme 55:B1
 - Equilibrium 65:47
 - Europium 57:253
 - Exploitation 49:167
 - Extractant 65:47
 - Fluidized 64:307
 - Grape 61:227
 - Ion-Exchange 64:307
 - Isotherm 49:167
 - Kinetics 58:285
 - Lactic-Acid 65:47
 - Liquid 57:253, 61:227
 - Mass-Transfer 55:B1
 - Membrane 57:253
 - Mobile 58:285
 - Mobile-Carrier 57:253
 - Modeling 64:307
 - Neutral 50:B39
 - Oil 61:227
 - Penicillin-G 50:B39, 58:285
 - Phosphorus-Ester 50:B39
 - Quinary-System 49:167
 - Reactive 65:47
 - Recovery 61:227
 - Seed 61:227
 - Sieve-Plate 55:B1
 - Simplified 64:307
 - Solvent-Extraction 61:227
 - Strontium-Chloride 49:167
 - Supercritical 61:227
 - Supported 57:253
 - Trivalent 57:253
 - Whey-Protein 64:307
- Extraction-Column**
 - Comparison 46:137
 - Estimation 45:133
 - Liquid-Test-System 46:137
 - Mass-Transfer-Coefficient 45:133
 - Mechanically-Agitated 46:137
 - Numerical-Technique 45:133
 - Single-Drop-Experiment 46:137
- Extractor** 57:229
- Facilitated**
 - Carrier 63:127, 66:11
 - Emulsion 63:127, 66:11
 - Liquid 63:127, 66:11
 - Membrane 63:127, 66:11
 - Modeling 63:127, 66:11
- Factor**
 - Affecting 61:13
 - Bromine 61:13
 - Catalyst 53:1
 - Design 53:1
 - Diffusion 53:1
 - Electrochemical-Reactor 61:13
 - Enhancement 51:93
 - Ethene 61:13
 - Instantaneous-Reaction 51:93
 - Intraparticle 53:1
 - Mass-Transfer 51:93
 - Mathematical-Model 61:13
 - Nonisothermal 51:93
 - Oxide 61:13
 - Particle 53:1
 - Production 61:13
 - Reaction-Kinetics 53:1
 - Relative-Concentration 61:13
 - Rigid-Drop-Model 51:93
 - Sieve-Plate 61:13
- Falling-Film** 49:119
- Falling-Film-Evaporator** 50:169
- Fast-Fourier-Transform** 51:77
- Fast-Parallel-Reactions** 58:15
- Fast-Reaction** 59:293
- Fed** 55:B47
- Fed-Batch**
 - Autoinductive 61:139
 - Choice 52:B59
 - Control 52:B59
 - Culture 61:35
 - Estimation 61:35
 - Fermentation 52:B59, 61:139
 - L-Lysine-Production 61:35
 - Modeling 61:35
 - Neural-Network 61:35
 - Nonlinear-Control 61:139
 - Observer-Based 61:139
 - Online 61:35
 - Optimization 52:B59
 - Process 61:139
 - State 61:35
 - Variable 52:B59
- Fed-Batch-Culture** 65:219
- Fed-Batch-Reactor** 47:149
- Feed** 54:17
- Feed-Concentration** 65:165
- Fermentation**
 - Aerated 46:B83
 - Alcohol 48:B15
 - α -Amylase 44:B51, 65:237
 - Amyloglucosidase 51:B17
 - ARMAX 50:B45
 - Autoinductive 61:139
 - Bacillus-Amyloliquefaciens 65:237
 - Batch 48:B15, 52:B35
 - Bed 51:B17
 - Cellulose 45:B27
 - Choice 52:B59
 - Complex-Selective-Medium 52:B35
 - Control 52:B59
 - Depth 51:B17
 - Different 51:B17
 - Enzyme 50:B45
 - Ethanol 45:B27, 48:B15, 54:221
 - Evaporative-Loss 48:B15
 - Experimental-Study 54:221
 - Fed-Batch 52:B59, 61:139
 - Glyceraldehyde-3-Phosphate-Dehydrogenase 52:B35
 - Heat-Transfer 46:B83, 60:199
 - High-Temperature 44:B51
 - Inert-Support 60:189
 - Kinetics 54:221
 - Level 51:B17
 - Macroapproach 54:221
 - Mathematical-Model 60:189
 - Mathematical-Modeling 54:221
 - Modeling 48:B15, 50:B45, 52:B35
 - Multidimensional 60:199
 - Mycelial-Fungi 60:189
 - Mycelial-System 46:B83
 - Nonaerated 46:B83
 - Nonlinear-Control 61:139
 - Observer-Based 61:139
 - Optimization 52:B59
 - Oxygen-Transfer 44:B51
 - Process 61:139
 - Production 52:B35
 - Recombinant-Escherichia-Coli 52:B35
 - Rheology 44:B51
 - Saccharification 45:B27
 - Saccharomyces-Cerevisiae 54:221
 - Simulation 45:B27
 - Simultaneous 45:B27
 - Solid-State 51:B17, 60:189, 60:199
 - Starch-Suspension 44:B51
 - State-Estimation 50:B45
 - Stirred-Tank-Reactor 46:B83
 - Temperature-Variation 51:B17
 - Transient 60:199
 - Variable 52:B59
- Fermentation-Broth**
 - Apparent-Yield-Stress 45:B49
 - Bubble-Column-Reactor 53:B35
 - Citric-Acid 53:B35
 - Direct-Measurement 47:B35
 - Dynamic-Measurement 47:B35
 - Estimation 45:B49
 - Gas-Hold-Up 47:B35
 - Low-Cost 45:B49
 - Morphological-Property 53:B35
 - Residual 47:B35
 - Rheological-Property 53:B35
 - Stirred-Tank-Reactor 53:B35
 - Submerged 53:B35

- Viscometer 45:B49
- Viscous 47:B35
- Xanthan-Gum-Solution 45:B49
- Fermenter**
 - Balancing 65:123
 - Batch 51:B57
 - Mammalian-Cell 65:123
 - Mixing 51:B57
 - Semicontinuous-Multi-Tank-Culture 65:123
 - Unstirred 51:B57
- Fermenter-Broth** 56:B1
- Ferrous-Sulfide** 56:B115
- Fiber** 58:245
- Fiber-Optic-Probe** 61:179
- Fibrous-Particle** 58:109
- Film**
 - Absence 43:41
 - Condensation 49:177
 - Estimation 43:41
 - Fluid 52:19, 64:361
 - Mass-Transfer 43:41, 52:19, 64:361
 - Model 49:177, 52:19, 64:361
 - Molecular-Evaporator 49:177
 - Multicomponent 52:19, 64:361
 - Nonideal-Mixture 52:19, 64:361
 - Resistance 43:41
 - Surface-Diffusivity 43:41
 - Temperature-Profile 49:177
- Filter** 58:145
- Filter-Cake** 50:69
- Filtration** 61:171
- Fine**
 - 1-Propanol 51:129
 - Alkoxide 55:93
 - Coarse 67:37
 - Controlled 51:129, 55:93
 - Emulsion 67:37
 - High-Temperature-Range 55:93
 - Hydrolysis 51:129, 55:93
 - Inversion 58:45
 - Liquid-Liquid-Dispersion 58:45
 - Method 58:45
 - Mixture 67:37
 - Particle 51:129, 55:93
 - Phase 58:45
 - Separation 58:45
 - Spherical 51:129, 55:93
 - Storage-Loss-Modulus 67:37
 - Synthesis 51:129, 55:93
 - Tetrabutoxide 51:129
 - Viscosity 67:37
 - Zirconia 51:129, 55:93
 - Zirconium 51:129, 55:93
- Fine-Chemical-Production**
 - Batch-Reactor 59:229
 - Biotransformation 61:53
 - Constrained-Optimization 59:229
 - γ -Butyrobetaine 61:53
 - L-Carnitine 61:53
 - Process-Integration 61:53
- Fine-Particle**
 - Axial-Mixing 47:47
 - Fluidized-Bed 47:47
 - Gas-Hold-Up 44:11
 - Three-Phase-Sparged-Reactor 44:11
- Fine-Wet-Grinding** 63:141
- Finned-Tube** 66:159
- First-Order-Reaction**
 - Catalyst 54:41
 - Catalytic-Process 60:111
 - Conversion 54:41, 60:111
 - Fixed-Bed-Reactor 54:41
 - Flow-Rate 60:111
 - Heterogeneous-Reactor 54:41
 - Intraparticle-Convection 54:41
 - Irreversible-Reaction 60:111
 - Isothermal 54:41
 - Large-Pore 54:41, 60:111
 - Material 60:111
 - Operating-Temperature 60:111
 - Plug-Flow-Reactor 60:111
- Fischer-Tropsch-Synthesis** 47:83
- Fixed-Bed**
 - Axial-Dispersion 52:63
 - Corrected-Fick's-Law 61:123
 - Different 52:63
 - Equivalence 61:123
 - Estimation 53:193
 - Experiment 53:193
 - Feed 54:17
 - Flow 53:193
 - Highly-Concentrated 54:17
 - Ion-Exchange-Process 61:123
 - K-Na-Exchange 54:17
 - Kinetic-Parameter 53:193
 - Liquid-Flow 52:63
 - Maldistribution 53:193
 - Metallic-Foam 52:63
 - Modeling 54:17, 61:123
 - Nernst-Planck-Law 61:123
 - Packed 52:63
 - Reticulated 52:63
 - Structure 52:63
 - Tracer 53:193
 - Transport 53:193
- Fixed-Bed-Catalytic-Reactor** 43:1
- Fixed-Bed-Reactor**
 - Analysis 47:105
 - Application 51:77
 - β -Galactosidase 65:93
 - Catalyst 47:105, 54:41
 - Catalytic-Method 58:33
 - Chitosan 65:93
 - Combined 47:105
 - Constant 47:105
 - Conversion 47:105, 54:41
 - Decay 47:105
 - Design 47:B11
 - Estimation 51:77
 - Exit 47:105
 - Fast-Fourier-Transform 51:77
 - First-Order-Reaction 54:41
 - Heterogeneous-Reactor 54:41
 - Hydrolysis 65:93
 - Immobilized 65:93
 - Intraparticle-Convection 54:41
 - Isothermal 54:41
 - Kinetic-Parameter 51:77
 - Lactose 65:93
 - Large-Pore 54:41
 - Limit 58:33
 - Pseudoadiabatic-Operation 58:33
 - Regime 58:33
 - Self-Inhibitory-Substrate 47:B11
 - Space-Time-Trajectory 47:105
 - Temperature 47:105
- Flat-Base** 55:27
- Flat-Fluidized-Photoreactor** 45:1
- Flexible**
 - Adaptive 63:65
 - Aerosol 58:109
 - Baffle 59:33
 - Batch-Process 63:65
 - Behavior 59:33
 - Control 63:65
 - Cylindrical-Collector 58:109
 - Deposition 58:109
 - Development 63:65
 - Fibrous-Particle 58:109
 - Flotation-Column 59:33
 - Neural-Network 63:65
 - Simulation 59:33
 - Stiff 58:109
 - Theoretical-Study 58:109
- Floc** 62:23
- Flotation**
 - Analysis 59:15
 - Cell 59:1
 - Circuit-Design-Principle 59:15
 - Column 59:1
 - Corn 59:221
 - Drying 59:221
 - Experimental-Study 59:221
 - Fluidized-Bed 59:221
 - Kinetics 59:221
 - Large-Scale 59:1
 - Performance 59:1
 - Pilot-Plant-Data 59:1
 - Prediction 59:1
- Flotation-Bed** 60:39
- Flotation-Column** 59:33
- Flow**
 - A-Priori-Information 56:167
 - Accelerated-Film-Technique 67:65
 - Application 62:193
 - Arbitrary 56:33
 - Batch 52:107
 - Bend 45:165
 - Biochemical 62:193
 - Characterization 64:107
 - Chemical-Reaction 52:107
 - Circulating 64:107
 - Cross Section 56:33
 - Cylindrical-Duct 56:33
 - Estimation 53:193
 - Experiment 53:193
 - Fixed-Bed 53:193
 - Fluid 56:33
 - Fluidized-Bed 64:107
 - Gas 56:B79
 - Generalized-Reynolds-Number 56:33
 - Highly-Viscous-Liquid 56:B79
 - Hold-Up 56:B79
 - Hydrodynamical 62:193
 - Imaging 56:167
 - Incline 60:141
 - Inclined 56:167
 - Interaction 62:193
 - Kinetic-Parameter 53:193
 - Liquid 62:193
 - Maldistribution 53:193
 - Modeling 56:167
 - Motor 67:65
 - Multifractal 64:107
 - Multiphase-Flow 56:167
 - Non-Newtonian-Liquid 45:165
 - Non-Viscous-Effect 59:111
 - Oil 67:65
 - Packed-Bed 59:111
 - Particle 62:193
 - Polymer-Thickened 67:65
 - Power-Law 56:33
 - Profile 56:167
 - Pulsatile 52:107
 - Slowly-Varying 60:141
 - Slug 56:B79
 - Sphere 59:111
 - Stalactite 56:B79
 - Stirred-Tank-Reactor 52:107
 - Stretching 67:65
 - Test 67:65
 - Tracer 53:193
 - Transport 53:193
 - Trickle 60:141
 - Velocity 56:167
 - Viscous 60:141
 - Xanthan-Gum-Solution 59:111
- Flow-Behavior** 63:195
- Flow-Characteristics**
 - High-Velocity 63:181
 - Highly-Concentrated 43:53
 - Liquid-Solid-Loop-Reactor 63:181
 - Mixing-Property 63:181
 - Oil-Water-Emulsion 43:53
 - Parallel Channel-Spacer 44:73

- Flow-Direction** 64:345
Flow-Induced 52:137
Flow-Measurement 63:59
Flow-Pattern
 · Air-Water-Pipe-Flow 48:197
 · Atmospheric-Condition 48:197
 · Bubble-Column-Reactor 48:141
 · Disk 45:87
 · Doughnut-Column 45:87
 · Hold-Up 48:197
 · Horizontal 48:197
 · Pressure-Drop 48:197
 · Simulation 45:87
 · Surface-Tension 48:197
 · Transport-Phenomena 48:141
Flow-Rate 60:111
Flow-Regime 64:169
Flow-Specification 50:133
Flowing
 · Colloidal-Dispersion 56:143
 · Corrugated-Wall 54:23
 · Dynamic-Interface 56:143
 · Experimental-Study 54:23
 · Hydrodynamics 54:23
 · Isothermal 54:23
 · Liquid-Film 54:23
 · Microelectrical-Tomography 56:143
 · Tubular-Column 54:23
Fluctuation 53:39
Fluid
 · Arbitrary 56:33
 · Bioreactor 55:B73
 · Catalytic-Wall-Reaction 62:51
 · Chemical-Vapor-Deposition-Reactor 54:137
 · Compressible 54:137
 · Computational 59:39
 · Convective-Diffusion 62:51
 · Cross-Section 56:33
 · Cylindrical-Duct 56:33
 · Design 55:B73
 · Duct 62:51
 · Equation 55:B73
 · Film 52:19, 64:361
 · Flow 56:33
 · Flow-Specification 50:133
 · Generalized-Reynolds-Number 56:33
 · Hollow-Fiber 55:B73
 · Homogeneous 62:51
 · Horizontal 54:137
 · Inside 62:51
 · Laminar-Flow 45:43
 · Large-Scale 50:133
 · Mass-Transfer 52:19, 64:361
 · Mixed-Pressure 50:133
 · Mixing 59:39
 · Model 52:19, 64:361
 · Multicomponent 52:19, 64:361
 · Network-Analysis 50:133
 · Nonideal-Mixture 52:19, 64:361
 · Pipe 45:43
 · Power-Law 55:B73, 56:33, 62:51
 · Progress 59:39
 · Residence-Time-Distribution 45:43
 · Single 62:51
 · Stability 54:137
 · Stirred-Vessel 59:39
 · Transport-Property 54:137
 · Variable 54:137
Fluid-Fluid-System 60:105
Fluid-System 57:189
Fluidization
 · Demarcate 57:261
 · Development 68:7
 · Fluidized-Bed 68:7
 · Measurement 57:261
 · Mini-Tapered 68:7
 · Onset 57:261
 · Particle 68:7
 · Stability 68:7
 · System 68:7
 · Tapered-Vessel 51:121
 · Thermogravimetric-Analyzer 68:7
 · Turbulence 57:261
 · Velocity 57:261
Fluidized
 · Application 66:227
 · Bioparticle 65:117
 · Chromatography 64:307
 · Continuous-Ethanol-Production 50:B17
 · Corn 60:39
 · Distribution 60:89
 · Drying 60:39
 · Economical-Optimization 64:307
 · Extraction 64:307
 · Flotation-Bed 60:39
 · Gas 60:89
 · Glucose 50:B17
 · High-Pressure 60:89
 · Hydrolysis 66:227
 · Immobilized 50:B17
 · Ion-Exchange 64:307
 · Kinetics 60:39, 65:117
 · Methyl-Acetate 66:227
 · Microcarrier 50:B17
 · Modeling 60:39, 64:307
 · Particle-Size 60:89
 · Reaction-Distillation-Column 66:227
 · Saccharomyces-Cerevisiae 50:B17
 · Segregation 60:89
 · Simplified 64:307
 · Solid 60:89
 · Substrate-Inhibition 65:117
 · Whey-Protein 64:307
 · Wide 60:89
Fluidized-Bed
 · Axial-Mixing 44:1, 47:47
 · Behavior 50:87
 · Bioreactor 61:241
 · Bubble 56:95
 · Capacitance 56:95
 · Catalytic-Cracking 44:53
 · Characteristics 43:67
 · Characterization 64:107
 · Circulating 64:107
 · Coalescing-Property 55:1
 · Comparative-Study 60:75
 · Computer-Aided-Analysis 46:47
 · Core-Annulus 68:51
 · Corn 59:221
 · Description 61:73
 · Design 53:75, 60:75
 · Determination 48:119
 · Deterministic-Chaos 53:75
 · Development 68:7
 · Dissolution 48:119
 · Distributor 56:95
 · Draft-Tube 66:105
 · Drying 59:221
 · Entrainment 66:105
 · Experimental-Data 44:53
 · Experimental-Study 59:221
 · External-Wall 46:47
 · Fine-Particle 47:47
 · Flotation 59:221
 · Flow 64:107
 · Fluidization 68:7
 · Formation 56:95
 · Gas-Liquid-Solid-Circulation 58:259
 · Global 61:73
 · Growth 48:119
 · Heat-Transfer 55:1
 · Hold-Up 43:67
 · Hydrodynamics 55:1
 · Imaging 56:95
 · Immobilized-Enzyme-System 61:241
 · Internal-Circulation 66:105
 · Interpretation 44:53
 · Kinetic-Model 44:53
 · Kinetics 48:119, 59:221
 · Liquid 50:87, 51:135, 55:1
 · Liquid-Solid-Circulating 68:51
 · Local 61:73
 · Local-Heat-Transfer 46:47
 · Magnetically-Stabilized 61:241
 · Mass-Transfer 55:1, 61:241
 · Mini-Tapered 68:7
 · Model 68:51
 · Modeling 61:73
 · Monosized-Crystal 50:87
 · Movement 51:135
 · Multifractal 64:107
 · Multistage-Reactor 44:53
 · Non-Newtonian-Liquid 52:131
 · Oil-Fraction 44:53
 · Operation 53:75
 · Particle 51:135, 68:7
 · Phase 43:67
 · Phase-Hold-Up 58:259
 · Radial-Flow 68:51
 · Real-Time 56:95
 · Single-Stage-Reactor 44:53
 · Sodium-Perborate 50:87
 · Sodium-Perborate-Tetrahydrate 48:119
 · Solid 44:1, 51:135, 66:105
 · Solid-Liquid-Mass-Transfer 52:131
 · Stability 68:7
 · Structure 61:73, 68:51
 · System 68:7
 · Thermogravimetric-Analyzer 68:7
 · Three-Phase 43:67, 55:1
 · Tool 61:241
 · Turbulent 44:1, 61:73
 · Tuyere 60:75
Fluidized-Bed-Bioreactor 45:B35
Fluidized-Bed-Reactor
 · Catalyst 60:131
 · Fiber-Optic-Probe 61:179
 · Mathematical-Modeling 60:131
 · Modeling 61:179
 · Tracer 61:179
 · Turbulent 61:179
 · Unsteady-State 60:131
Fluidized-Bed-System
 · Anaerobic 54:B25
 · Fruit 54:B25
 · Imaging 56:83
 · Kinetics 54:B25
 · Processing 54:B25
 · Purification 54:B25
 · Waste-Water 54:B25
Fluorinated-Hydrocarbon 44:173
Fluorite 64:283
Flux
 · Bubble-Size 67:71
 · Cross-Flow 61:171
 · Filtration 61:171
 · Frequency 67:71
 · Gas 67:71
 · Membrane 67:71
 · Particle 61:171
 · Permeation 61:171, 67:71
 · Sparged 67:71
 · Steady-State 61:171
 · Tubular 67:71
 · Ultrafiltration 67:71
Flux-Decay 48:B1
Fly-Ash 66:171
Force 60:55
Force-Field 68:69
Forced-Convection

- Catalyst 57:101
- Darcy 50:33
- Free-Convection 50:33
- Heat-Transfer 50:33
- Inelastic-Fluid 50:33
- Mixed-Convection 50:33
- Mole-Change 57:101
- Non-Darcy 50:33
- Non-Newtonian-Fluid 50:33
- Porous 57:101
- Porous-Medium 50:33
- Reaction 57:101
- Saturated 50:33
- Unified-Similarity-Transformation 50:33
- Forced-Flow** 45:123
- Formation**
 - Bubble 56:95
 - Capacitance 56:95
 - Catalytic-Bed-Reactor 44:97
 - Controlled-Hydrolysis 44:133
 - Distributor 56:95
 - Ethanol 44:133
 - Fluidized-Bed 56:95
 - Imaging 56:95
 - Kinetic-Model 44:97
 - Methyl-tert-Butyl-Ether 44:97
 - Monosized 44:133
 - Reaction-Kinetics 44:133
 - Real-Time 56:95
 - Silica-Sphere 44:133
 - Size-Control 44:133
 - Tetraethyl-Orthosilicate 44:133
- Forward-Extraction** 60:63
- Four-Parameter** 55:139
- Fractal**
 - Analysis 64:45
 - Artificial 64:63
 - Catalyst 64:69
 - Catalytic-Reaction 64:63
 - Chaos 64:v
 - Chemical-Engineering 64:v
 - Dense 64:99
 - Design 64:69
 - Devils-Comb 64:63
 - Heterogeneous-Medium 64:21
 - Linear 64:21
 - Linear-Transport-Phenomena 64:45
 - Morphology 64:69
 - Nonlinear 64:21
 - Percolation 64:21
 - Rheological-Modeling 64:99
 - Scalar 64:21
 - Scaling-Law 64:21
 - Simulation 64:63
 - Suspension 64:99
 - Transport-Process 64:21
 - Vector 64:21
- Fraction**
 - Crude-Oil 45:83, 51:151
 - Estimation 45:83, 51:151
 - Kinematic-Viscosity 51:151
 - Neural-Network 51:151
 - Petroleum 45:83, 51:151
 - Simple-Method 45:83
 - Viscosity 45:83
- Free-Convection**
 - Circular-Tube 55:103
 - Coupling 55:103
 - Darcy 50:33
 - External 55:103
 - Forced-Convection 50:33
 - Heat-Transfer 50:33, 55:103
 - Inelastic-Fluid 50:33
 - Laminar-Flow 55:103
 - Mixed-Convection 50:33
 - Non-Darcy 50:33
 - Non-Newtonian-Fluid 50:33
 - Porous-Medium 50:33
 - Saturated 50:33
 - Unified-Similarity-Transformation 50:33
 - Vertical-Tube 55:103
- Freezing** 57:53
- Frequency** 67:71
- Fresh-Water** 56:B109
- Fructose** 61:233
- Fruit** 54:B25
- Fuel** 57:219
- Fully-Developed-Flow** 55:15
- Functional-Transformation-Method** 51:63
- Fungal** 65:219
- Fuzzy-Calculus** 54:155
- Galactosidase** | β -» 65:93
- Galactosidase** | Free- β -» 52:B1
- Galactosidase** | Immobilized- β -» 52:B1
- Gas**
 - Accumulation-Effect 59:281
 - Active-Carbon 44:43
 - Agitated-Reactor 47:33
 - Air-Water-System 53:167
 - Aphron 65:1
 - Bubble-Size 67:71
 - Bubbling-Bed-Reactor 66:193
 - Calcined 47:1
 - Catalytic-Partial-Oxidation 66:193
 - Characteristics 54:63
 - Characterization 65:1
 - Circulating 45:9
 - Colloidal 65:1
 - Cyclone-Reactor 45:9
 - Determination 47:1
 - Distribution 60:89
 - Dynamic-Transport 57:91
 - Efficiency 45:9
 - Elevated 54:63
 - Elevated-Pressure 47:33
 - Ethanol 54:63
 - Experimental-Investigation 59:281
 - Experimental-Study 66:193
 - Flow 56:B79
 - Fluidized 60:89
 - Flux 67:71
 - Frequency 67:71
 - Gas-Hold-Up 53:167
 - Generalization 56:67
 - Heat-and-Mass-Transfer 45:9
 - High-Pressure 60:89
 - Highly-Viscous-Liquid 56:B79
 - Hold-Up 56:B79
 - Hydrogen-Chloride 47:1
 - Intermediate 53:167
 - Kinetic-Parameter 47:1
 - Limestone 47:1
 - Limitation 59:195
 - Liquid 59:281
 - Liquid-Mixing 53:167
 - Low-Pressure 56:67
 - Low-Velocity 53:167
 - Mass-Transfer 54:63, 59:195
 - Mass-Transfer-Characteristics 47:33
 - Membrane 67:71
 - Metering 59:281
 - Methane 66:193
 - Methanol 54:63
 - Microbial-System 59:195
 - Mixture 56:67, 57:91
 - Multicomponent 57:91
 - Normal-Decane 47:33
 - Orifice 59:281
 - Particle-Size 60:89
 - Permeation 67:71
 - Porous-Solid 57:91
 - Presence 44:43
 - Pressure 54:63
 - Protein 65:1
 - Reaction 47:1
 - Reactor-Wall 45:9
 - Recovery 65:1
 - Segregation 60:89
 - Simple 56:67
 - Single 45:9
 - Slug 56:B79
 - Solid 60:89
 - Sparged 67:71
 - Stalactite 56:B79
 - Subsequent 65:1
 - Substrate 59:195
 - Synthesis 66:193
 - Temperature 47:33, 54:63
 - Thermal-Conductivity-Measurement 44:43
 - Thermogravimetry 47:1
 - Tubular 67:71
 - Two-Phase-Flow 59:281
 - Ultrafiltration 67:71
 - Uncoupling 59:195
 - Viscosity 56:67
 - Wide 60:89
- Gas-Highly-Viscous-Liquid-Solid-System** 50:B29
- Gas-Liquid-Solid-Circulation** 58:259
- Gas-Liquid-Solid-Fluidization** 51:109
- Gas-Liquid-Solid-Fluidized-Bed**
 - Axial-Dispersion 44:51, 44:52
 - Liquid 44:51, 44:52
- Gas-Liquid-Bioreactor** 49:B13
- Gas-Liquid-Circulation** 56:B101
- Gas-Liquid-Cocurrent-Downflow**
 - Hydrodynamics 58:83
 - Mass-Transfer 58:83
 - Model 51:19
 - Packed-Bed 51:19
 - Pressure-Drop 51:19
 - Three-Phase-Fixed-Bed-Reactor 58:83
- Gas-Liquid-Contactor** 64:157
- Gas-Liquid-Controlling** 62:61
- Gas-Liquid-Dispersion** 61:83
- Gas-Liquid-Ejector** 53:67
- Gas-Liquid-Flow**
 - Boundary-Layer-Separation 49:55
 - Cylindrical 49:55
 - Diffuser 49:55
 - Hold-Up 45:55
 - Inclined 45:55
 - Prediction 45:55
 - Section 49:55
 - Two-Phase 45:55
 - Venturi-Scrubber 49:55
- Gas-Liquid-Mass-Transfer**
 - Airlift-Column 62:35
 - Airlift-Slurry-Reactor 62:223
 - Bubble-Column-Reactor 62:223
 - Characteristics 62:223
 - Comparative-Evaluation 62:223
 - External-Loop 62:35
 - Hydrodynamic 62:223
 - Newtonian-Fluid 62:35
 - Non-Newtonian-Fluid 62:35
- Gas-Liquid-Parameter** 52:121
- Gas-Liquid-Processing** 56:183
- Gas-Liquid-Property** 59:91
- Gas-Liquid-Separator**
 - Downcomer 57:B7
 - External-Loop-Airlift-Contactor 66:91
 - Gas-Hold-Up 57:B7
 - Global 66:91
 - Height 66:91
 - Hydrodynamic-Parameter 66:91
 - Internal-Loop-Airlift-Reactor 57:B7
 - Liquid 66:91
 - Relationship 57:B7
 - Riser 57:B7
- Gas-Liquid-Transfer** 66:21

- Gas–Solid–Cocurrent–Downflow-System** 64:345
- Gas–Solid–Cocurrent–Upflow-System** 64:345
- Gas–Solid–Fluidized–Bed** 53:89
- Gas–Solid–Fluidized–Bed–Reactor** 58:223
- Gas–Solid–Reaction**
 - Application 63:79
 - Grain-Size-Distribution-Model 53:25
 - Half-Order 63:79
 - Model 63:79, 68:1
 - Moving-Boundary-Problem 63:79
 - Noncatalytic 53:25
 - Nucleation 68:1
 - Quantized-Solution 68:1
 - Reaction 63:79
 - Volume 63:79
- Gas–Solid–Separator** 66:159
- Gas–Solids–Injector** 45:137
- Gas–Absorption**
 - Boundary-Value-Problem 57:27
 - Determination 57:67
 - Mass-Transfer-Coefficient 57:67
 - Packed-Column 57:67
 - Physical-System 57:67
 - Reactive 57:27
 - Technique 57:67
- Gas–Bubble**
 - Agitated-Vessel 48:41
 - Application 48:41
 - Capacitance-Probe 52:1
 - Characterization 52:1
 - Experimental-Technique 48:41
 - Highly-Viscous-Liquid 48:41
 - Liquid 48:41
 - Mass-Transfer 48:41
 - Measurement 48:41
 - Stirred-Tank-Reactor 52:1
- Gas–Bubble–Entrainment** 44:157
- Gas–Disengagement** 65:263
- Gas–Flow**
 - Chemical-Reaction 58:223
 - Conical 56:19
 - Corrugated-Sheet 53:55
 - Distribution 53:55
 - Gas–Solid-Fluidized-Bed-Reactor 58:223
 - Liquid 61:95
 - Measurement 53:55
 - Modeling 53:55, 58:223
 - Packing 53:55, 61:95
 - Pattern 61:95
 - Random 61:95
 - Reconsideration 58:223
 - Simplified-Model 56:19
 - Spouted-Bed 56:19
 - Structured 53:55
 - Variation 58:223
- Gas–Hold-Up**
 - Air–Water-System 53:167
 - Alcohol 50:47
 - Bidimensional 47:135, 50:143
 - Bubble-Column 50:47
 - Bubble-Column-Reactor 50:1
 - Bubble-Rise-Velocity 50:47
 - Bubble-Size 50:47
 - Bubble-Size-Distribution 50:B29
 - Concentration 50:47
 - Direct-Measurement 47:B35
 - Downcomer 57:B7
 - Downjet-Loop-Reactor 49:49
 - Dynamic-Measurement 47:B35
 - Fermentation-Broth 47:B35
 - Fine-Particle 44:11
 - Gas 53:167
 - Gas–Highly-Viscous-Liquid–Solid-System 50:B29
 - Gas–Liquid-Separator 57:B7
 - Intermediate 53:167
 - Internal-Loop-Airlift-Reactor 57:B7
 - Liquid-Mixing 53:167
 - Liquid-Phase 49:49
 - Low-Velocity 53:167
 - Mass-Transfer-Coefficient 49:49
 - Newtonian-Fluid 50:1
 - Non-Newtonian-Fluid 50:1
 - Organic-Acid 50:47
 - Potassium-Chloride 50:47
 - Prediction 50:1
 - Relationship 57:B7
 - Residual 47:B35
 - Riser 57:B7
 - Slurry-Bubble-Column 49:151
 - Spouted-Bed 47:135, 50:143
 - Three-Phase 50:143
 - Three-Phase-Sparged-Reactor 44:11
 - Three-Phase-System 49:151
 - Time-Dependent 50:B29
 - Two-Phase 47:135
 - Two-Phase-System 49:151
 - Viscous 47:B35
 - Volumetric 49:49
- Gas–Phase** 48:83
- Gas–Phase–Dispersion** 59:91
- Gas–Sparging** 47:187
- Gas–Transfer** 57:B1
- Gasification** 64:77
- Gasifier** 59:133
- Gel** 55:B35
- Gel–Effect** 48:71
- Gelatin–Production** 67:55
- General** 61:161
- Generalization** 56:67
- Generalized–Analysis** 56:B61
- Generalized–Approach** 65:133
- Geometrical** 62:1
- Geometry**
 - Analogy 61:113
 - Catalyst 61:113
 - Conical 62:113
 - Convection 61:113
 - Cylinder 61:113
 - Diffusion 61:113
 - Hydrodynamics 62:113
 - Influence 62:113
 - Particle 61:113
 - Reaction 61:113
 - Section 62:113
 - Shallow 62:113
 - Slab 61:113
 - Spouted-Bed 62:113
- Ghose–Model | Modified–>** 44:B69
- Gibberellic–Acid** 46:B53
- Gibbs'–Free–Energy** 54:187
- Glaserite** 67:1
- Global**
 - Continuous-Stirred-Tank-Bioreactor 56:B69
 - Control 56:B69
 - Description 61:73
 - External-Loop-Airlift-Contactor 66:91
 - Fluidized-Bed 61:73
 - Gas–Liquid-Separator 66:91
 - Height 66:91
 - Hydrodynamic-Parameter 66:91
 - Liquid 66:91
 - Local 61:73
 - Modeling 61:73
 - Structure 61:73
 - Turbulent 61:73
- Gluconobacter–Suboxydan** 45:B5
- Glucose**
 - Alginate 56:B9
 - Calcium 56:B9
 - Continuous-Ethanol-Production 50:B17
 - Determination 56:B9
 - Diffusion-Coefficient 56:B9
 - Fluidized 50:B17
 - Identification 56:B9
 - Immobilized 50:B17
 - Malic-Acid 56:B9
 - Membrane 56:B9
 - Microcarrier 50:B17
 - Model 56:B9
 - Saccharomyces-Cerevisiae 50:B17
- Glucose–Fructose–Mixtures** 65:209
- Glucose–Oxidase** 65:71
- Glucosyltransferase** 61:247
- Glyceraldehyde-3-Phosphate–Dehydrogenase** 52:B35
- Goethite** 59:287
- Granulometric–Distribution** 49:141
- Grape**
 - Alginate-Bead 55:B29
 - Carbon-Dioxide 61:227
 - Comparison 61:227
 - Continuous-Fluidized-Bed 55:B29
 - Conventional 61:227
 - Deacidification 55:B29
 - Entrapped 55:B29
 - Extraction 61:227
 - Liquid 61:227
 - Must 55:B29
 - Oil 61:227
 - Process 55:B29
 - Recovery 61:227
 - Schizosaccharomyces 55:B29
 - Seed 61:227
 - Solvent-Extraction 61:227
 - Supercritical 61:227
- Graphical–Representation** 59:23
- Gravimetric–Determination** 53:147
- Green** 62:81
- Green–Microalgae** 65:13
- Grid–Generated** 47:155
- Group–Contribution** 46:29
- Group–Contribution–Method** 50:9
- Growth**
 - Acetobacter-Aceti 54:B15
 - Aerobic-Mixed-Culture 53:B47
 - Bioprocess 65:109
 - Continuous-Flow-Stirred-Tank-Reactor 62:143
 - Continuous-Stirred-Reactor 53:B47
 - Culture 54:B15
 - Determination 48:119
 - Dissolution 48:119
 - Fluidized-Bed 48:119
 - Kinetic-Model 54:B15
 - Kinetics 48:119
 - L-Alanine-Production 65:109
 - Optimum-Design 62:143
 - Oxygen-Transfer 65:109
 - Parameter 65:109
 - Phenol 53:B47
 - Production 62:143
 - Pseudomonas-Dacunhae 65:109
 - Recombinant-Escherichia-Coli 62:143
 - Sodium-Perborate-Tetrahydrate 48:119
 - Stage 62:143
 - Steady-State-Behavior 53:B47
 - Submerged 54:B15
 - Tryptophan-Synthetase-Subunit 62:143
 - Two-Stage 62:143

- Growth-Kinetics** 53:B13
- Gypsum** 67:1
- H₂O** 46:79
- H₂S** 46:79
- Half-Order** 63:79
- HCl-Gas** 47:11
- Heat**
- Critical-Pressure 59:127
 - Density 59:127
 - Development 58:123
 - Estimation 59:127
 - Experimental-Verification 58:123
 - Heterogeneous-System 50:79
 - Liquid 59:127
 - Mass-Transfer 50:79, 58:123
 - Model 58:123
 - Momentum 58:123
 - Pure-Substance 59:127
 - Solution-Method 50:79
 - Spray-Drying 58:123
 - Vaporization 59:127
- Heat-and-Mass-Transfer** 45:9
- Heat-Capacity** 52:31
- Heat-Transfer**
- Aerated 46:B83
 - Agitated-Vessel 58:135
 - Baffle 58:135
 - Bubble-Column 47:91
 - Circular-Tube 55:103
 - Coalescing-Property 55:1
 - Configuration-Factor 45:75
 - Correlation 55:39
 - Coupling 55:103
 - Cyclone-Reactor 48:83
 - Cylindrical-Probe 44:141
 - Darcy 50:33
 - Determination 45:75
 - Efficiency 48:83
 - Equipped 58:135
 - External 55:103
 - Falling-Film 49:119
 - Fermentation 46:B83, 60:199
 - Fluidized-Bed 55:1
 - Forced-Convection 50:33
 - Free-Convection 50:33, 55:103
 - Gas-Phase 48:83
 - Horizontal-Pipe 55:39
 - Hydrodynamic-Investigation 47:91
 - Hydrodynamics 55:1
 - Immersed 44:141
 - Inelastic-Fluid 50:33
 - Influence 50:149
 - Jacketed 58:135
 - Laminar 49:119
 - Laminar-Flow 55:103
 - Liquid 49:119, 55:1
 - Liquid-Solid-Flow 55:39
 - Liquid-Vessel 61:107
 - Mass-Transfer 49:119, 55:1
 - Measurement 48:83, 61:107
 - Mixed 61:107
 - Mixed-Convection 50:33
 - Monte-Carlo-Method 45:75
 - Multicomponent 49:119
 - Multidimensional 60:199
 - Mycelial-System 46:B83
 - Non-Darcy 50:33
 - Non-Newtonian-Fluid 50:33
 - Nonaerated 46:B83
 - Nonstandard 58:135
 - Porous-Medium 50:33
 - Powder 47:91
 - Radiative 45:75
 - Reaction 49:119
 - Saturated 50:33
 - Simultaneous 49:119
 - Slurry-Bubble-Column 44:141, 52:49, 52:51
 - Small-Particle 47:91
 - Solid-Phase 48:83
 - Solid-State 60:199
 - Stirred-Tank-Reactor 46:B83
 - Thermal 45:75
 - Thin-Layer-Evaporator 50:149
 - Three-Phase 44:141, 55:1
 - Transient 60:199
 - Unified-Similarity-Transformation 50:33
 - Vertical-Tube 55:103
 - Vibrating-Element 50:149
 - Vibratory-Agitator 61:107
 - Viscous-Liquid 47:91
 - Wall 48:83
- Heat-Transfer-Rate** 51:7
- Heated** 65:99
- Heavy-Metal** 60:181
- Heavy-Oil-Processing** 46:61
- Height** 66:91
- Helical** 52:9
- Helical-Coil-Reactor** 64:129
- Helical-Ribbon-Impeller-Mixer** 67:215
- Heterogeneity** 51:159
- Heterogeneous-Medium** 64:21
- Heterogeneous-Reaction** 50:27
- Heterogeneous-Reactor** 54:41
- Heterogeneous-System** 50:79
- Heterogeneously-Catalyzed** 66:181
- Heteropolyacid** 64:247
- Heuristics** 46:97
- Hexane** 54:115
- Hierarchy** 64:273
- High** 59:153
- High-Concentration** 44:B69
- High-Conversion** 55:87
- High-Efficiency** 56:B75
- High-Frequency** 66:21
- High-Performance-Affinity-Chromatography** 65:175
- High-Performance-Compact-Reactor** 49:B1
- High-Pressure**
- Application 61:27
 - Calculation 61:27
 - Computation 60:1
 - Distribution 60:89
 - Fluidized 60:89
 - Gas 60:89
 - Model 61:27
 - Particle-Size 60:89
 - Segregation 60:89
 - Solid 60:89
 - Thermodynamic-Interpretation 60:1
 - Vapor-Liquid-Equilibrium 60:1, 61:27
 - Wide 60:89
- High-Rate** 57:B1
- High-Strength** 52:B21
- High-Temperature**
- Aerosol 64:239
 - α -Amylase 44:B51
 - Autoclave-Reactor 67:175
 - Characterization 64:239
 - Concentration 67:175
 - Copper-Modified 64:239
 - Decomposition 64:239
 - Fermentation 44:B51
 - Higher-Alcohol 64:239
 - Oxygen-Transfer 44:B51
 - Process 64:239
 - Rheology 44:B51
 - Solid 67:175
 - Starch-Suspension 44:B51
 - Synthesis 64:239
 - Ultrasonic-Measurement 67:175
 - Zinc-Chromite 64:239
- High-Temperature-Range** 55:93
- High-Throughput** 53:115
- High-Velocity** 63:181
- High-Yield** 56:B49
- Higher-Alcohol** 64:239
- Higher-Molecular-Weight** 67:191
- Highly-Compact** 46:B43
- Highly-Concentrated**
- Feed 54:17
 - Fixed-Bed 54:17
 - Flow-Characteristics 43:53
 - K-Na-Exchange 54:17
 - Modeling 54:17
 - Oil-Water-Emulsion 43:53
- Highly-Viscous-Fluid** 52:9
- Highly-Viscous-Liquid**
- Agitated-Vessel 48:41
 - Application 48:41
 - Experimental-Technique 48:41
 - Flow 56:B79
 - Gas 56:B79
 - Gas-Bubble 48:41
 - Hold-Up 56:B79
 - Liquid 48:41
 - Mass-Transfer 48:41
 - Measurement 48:41
 - Slug 56:B79
 - Stalactite 56:B79
- Hold-Up**
- Air-Water-Pipe-Flow 48:197
 - Atmospheric-Condition 48:197
 - Characteristics 43:67
 - Flow 56:B79
 - Flow-Pattern 48:197
 - Fluidized-Bed 43:67
 - Gas 56:B79
 - Gas-Liquid-Flow 45:55
 - Highly-Viscous-Liquid 56:B79
 - Horizontal 48:197
 - Inclined 45:55
 - Phase 43:67
 - Prediction 43:49, 45:55
 - Pressure-Drop 48:197
 - Slug 56:B79
 - Solid-Fluid-Flow 43:49
 - Stalactite 56:B79
 - Surface-Tension 48:197
 - Three-Phase 43:67
 - Two-Phase 45:55
- Hollow-Fiber**
- Bioreactor 51:B63, 55:B73
 - Design 51:B63, 55:B73
 - Equation 51:B63, 55:B73
 - Fluid 55:B73
 - Michaelis-Menten-Kinetics 51:B63
 - Power-Law 55:B73
 - Zero-Order-Limit 51:B63
- Hollow-Fiber-Biofilm-Reactor**
- Consumption 62:149
 - Effectiveness-Factor 62:149
 - Mathematical-Model 56:B53
 - Maximum 62:149
 - Substrate 62:149
- Hollow-Fiber-Bioreactor** 65:77
- Homogeneous**
- Antigen-Coupled 54:B33
 - Catalytic-Wall-Reaction 62:51
 - Characterization 54:B33
 - Convective-Diffusion 62:51
 - Duct 62:51
 - Fluid 62:51
 - Immunoassay 54:B33, 62:169
 - Inside 62:51
 - Liposome 54:B33, 62:169
 - Multicomponent 64:215
 - NMR 64:215
 - Peptide-Coupled 62:169
 - Polyclonal-Antibody 54:B33, 62:169
 - Power-Law 62:51
 - Protein 62:169
 - Single 62:51
 - Solution 64:215
 - Ternary-Mixture 59:51
 - Vanadium-Oxide 64:215
 - Vapor-Liquid-Separation 59:51

- Homogeneous-Catalytic Reaction** 49:35
- Homoionic-Zeolite** 66:65
- Horizontal**
- Air-Water-Pipe-Flow 48:197
 - Atmospheric-Condition 48:197
 - Chemical-Vapor-Deposition-Reactor 54:137, 57:39
 - Compressible 54:137
 - Flow-Pattern 48:197
 - Fluid 54:137
 - Hold-Up 48:197
 - Hot-Wall 57:39
 - Low-Pressure 57:39
 - Modeling 57:39
 - Pressure-Drop 48:197
 - Stability 54:137
 - Surface-Tension 48:197
 - Thermal 57:39
 - Transport-Property 54:137
 - Tubular 57:39
 - Variable 54:137
- Horizontal-Pipe**
- Chaos 64:149
 - Correlation 55:39
 - Deterministic-Analysis 64:149
 - Heat-Transfer 55:39
 - Intermittent-Flow-Regime 64:149
 - Liquid-Solid-Flow 55:39
 - Pressure-Fluctuation 64:149
- Horizontal-Stretching** 48:129
- Hot-Wall** 57:39
- Humic-Acid** 63:189
- Hyacinth** 56:B109
- Hydrated** 61:133
- Hydration** 50:115
- Hydrocarbon**
- Activity 52:115
 - Alternative 45:33
 - Carbon-Dioxide 66:217
 - Catalyst 52:115
 - Characterization 52:115
 - Cobalt 52:115
 - Conversion 45:33
 - Correlation 66:217
 - Corresponding-States 66:217
 - Kinetic-Model 45:33
 - Methanol 45:33
 - Modeling 45:33
 - Oxidation 52:115
 - Oxide 52:115
 - System 66:217
 - Total 52:115
 - Vapor-Liquid-Equilibrium 66:217
- Hydrodenitrogenation** 46:79
- Hydrodynamic**
- Agitator 61:83
 - Airlift-Slurry-Reactor 62:223
 - Bubble-Column-Reactor 62:223
 - Characteristics 62:223
 - Comparative-Evaluation 62:223
 - Gas-Liquid-Dispersion 61:83
 - Gas-Liquid-Mass-Transfer 62:223
 - Mixing-Vessel 61:83
 - Modified-Rushton-Turbine 61:83
 - Transfer-Process 61:83
- Hydrodynamic-Characteristics** 65:263
- Hydrodynamic-Investigation** 47:91
- Hydrodynamic-Parameter** 66:91
- Hydrodynamic-Shear** 62:121
- Hydrodynamical** 62:193
- Hydrodynamics**
- Analogous 53:89
 - Bioreactor 62:175
 - Bubble-Column 53:89
 - Capillary-Gap-Cell 43:107
 - Characteristics 43:95, 53:67
 - Coalescing-Property 55:1
 - Cocurrent 63:93
 - Conical 62:113
 - Corrugated-Wall 54:23
 - Description 53:89
 - Draft-Tube 60:155
 - Dynamics 58:145
 - Experimental-Study 54:23
 - External-Loop-Airlift-Reactor 67:205
 - Filter 58:145
 - Flat-Base 55:27
 - Flowing 54:23
 - Fluidized-Bed 55:1
 - Gas-Liquid-Solid-Fluidization 51:109
 - Gas-Liquid-Cocurrent-Downflow 58:83
 - Gas-Liquid-Ejector 53:67
 - Gas-Solid-Fluidized-Bed 53:89
 - Geometry 62:113
 - Heat-Transfer 55:1
 - Influence 62:113
 - Inverse 51:109
 - Isothermal 54:23
 - Laminar-Flow 58:145
 - Liquid 55:1
 - Liquid-Film 54:23
 - Local 53:67
 - Mass-Transfer 43:95, 43:107, 53:67, 55:1, 58:83, 62:175, 63:93, 67:205
 - Membrane 62:175
 - Packed-Bubble-Column 43:95
 - Packed-Column 63:93
 - Position 60:155
 - Promoter 43:107
 - Rotary 58:145
 - Section 62:113
 - Shallow 62:113
 - Slurry-Bubble-Column 60:155
 - Spouted-Bed 55:27, 62:113
 - Theoretical-Study 63:93
 - Three-Phase 55:1
 - Three-Phase-Fixed-Bed-Reactor 58:83
 - Tubular-Column 54:23
 - Turbulence 43:107
 - Vortex 62:175
 - Wave 62:175
- Hydrogen-Chloride** 47:1
- Hydrogen-Incorporation** 48:191
- Hydrogen-Peroxide** 60:101
- Hydrogen-Production** 62:103
- Hydrogenation**
- Borate 63:27
 - Catalyst 63:27
 - Catalytic-Transfer 51:B51
 - Coal 58:53
 - Influence 58:53
 - Kinetics 51:B51, 58:53
 - Mo-Catalyzed 58:53
 - Naphthalene 63:27
 - Nature 58:53
 - Platinum-Aluminum 63:27
 - Porous 58:53
 - Soybean-Oil 51:B51
- Hydrogenation-Reaction** 48:191
- Hydrolysis**
- 1-Propanol 51:129
 - Alkoxide 55:93
 - Application 66:227
 - Aspergillus-Niger 52:B1
 - Batch 65:187
 - β -Galactosidase 65:93
 - Chitosan 65:93
 - Controlled 51:129, 55:93
 - Conventional 59:253
 - Enzymatic-Hydrolysis 65:187
 - Enzymatic-Kinetics 65:187
 - Fine 51:129, 55:93
 - Fixed-Bed-Reactor 65:93
 - Fluidized 66:227
 - Free- β -Galactosidase 52:B1
 - High-Temperature-Range 55:93
 - Immobilized 65:93
 - Immobilized- β -Galactosidase 52:B1
 - Lactose 52:B1, 65:93
 - Methyl-Acetate 66:227
 - Microwave-Heating 59:253
 - Modeling 52:B1
 - Particle 51:129, 55:93
 - Protein 65:187
 - Reaction-Distillation-Column 66:227
 - Simulation 52:B1
 - Spherical 51:129, 55:93
 - Stirred-Reactor 65:187
 - Stirred-Tank-Reactor 59:253
 - Sucrose 59:253
 - Synthesis 51:129, 55:93
 - Tetrabutoxide 51:129
 - Wheat 65:187
 - Zirconia 51:129, 55:93
 - Zirconium 51:129, 55:93
- Hydrous-Tin-Dioxide** 66:85
- Hydroxide** 66:171
- Identification** 56:B9
- Imaging**
- A-Priori-Information 56:167
 - Air-Core 56:135
 - Bubble 56:95
 - Capacitance 56:95
 - Cyclonic-Separator 56:135
 - Design 56:135
 - Distributor 56:95
 - Flow 56:167
 - Fluidized-Bed 56:95
 - Fluidized-Bed-System 56:83
 - Formation 56:95
 - Implication 56:135
 - Inclined 56:167
 - Modeling 56:135, 56:167
 - Multiphase-Flow 56:167
 - Profile 56:167
 - Real-Time 56:95
 - Separator 56:135
 - Velocity 56:167
- Immersed** 44:141
- Immobilization**
- Acrylic 65:249
 - Adsorption 54:B1
 - Copolymer 65:249
 - Glucose-Oxidase 65:71
 - Ion-Exchange-Resin 61:149
 - Lipase 61:149, 65:249
 - Mass-Transfer 54:B1
 - Matrix 54:B1
 - Microbead 65:71
 - Modified 65:71
 - Monosize 65:71
 - Mucor-Miehei 61:149
- Immobilized**
- Adsorption 65:81
 - Adsorption-Data 65:81
 - Anaerobic-Digestion 54:B9
 - β -Galactosidase 65:93
 - Biomass 54:B9
 - Butanol 46:B11, 65:159
 - Calcium-Alginate 65:81
 - Cell 46:B11
 - Chitosan 65:93
 - Column 65:81
 - Continuous-Ethanol-Production 50:B17
 - Continuous-Fermentation 46:B11
 - Copper 65:81
 - Cow-Manure 54:B9
 - Deactivation 65:159
 - Diffusion 56:B61
 - Dynamic-Approach 65:81
 - Enzyme-Reaction 56:B61

- Evaluation 65:81
- Fixed-Bed-Reactor 65:93
- Fluidized 50:B17
- Generalized-Analysis 56:B61
- Glucose 50:B17
- Hydrolysis 65:93
- Integration 46:B11
- Internal 56:B61
- Kinetics 54:B9
- Lactose 65:93
- Lipozyme 65:159
- Mathematical-Modeling 46:B11
- Microcarrier 50:B17
- Moment-Analysis 65:81
- Multienzyme-Reaction 56:B61
- Packed-Bed 65:81
- Pervaporation 46:B11
- Saccharomyces-Cerevisiae 50:B17
- Simulation 46:B11
- Stimulus-Response 65:81
- Technique 65:81
- Temperature 65:159
- Water-Content 65:159
- Zeolite 54:B9
- Zoogloea-Ramigera 65:81
- Immobilized-Cell** 46:B1
- Immobilized-Cell-Aggregate** 59:309
- Immobilized-Cell-Packed-Bed-Bioreactor** 43:B1
- Immunoassay**
 - Antigen-Coupled 54:B33
 - Characterization 54:B33
 - Homogeneous 54:B33, 62:169
 - Liposome 54:B33, 62:169
 - Peptide-Coupled 62:169
 - Polyclonal-Antibody 54:B33, 62:169
 - Protein 62:169
- Immunogenicity** 65:257
- Impact**
 - Activity 56:B23
 - Anaerobic-Granule 56:B23
 - Boiler 66:159
 - Experimental-Study 66:159
 - Finned-Tube 66:159
 - Gas-Solid-Separator 66:159
 - Organic-Loading 56:B23
 - Reactor-Hydrodynamics 56:B23
 - Size 56:B23
- Impeller**
 - Aeration 58:59
 - Biological-Batch-Reactor 56:B43
 - Bioreactor 58:59
 - Cod 56:B43
 - Kinetics 56:B43
 - Reduction 56:B43
 - Self-Aspirating 58:59
 - Speed 56:B43
 - Submergence 56:B43
- Implantable** 44:B81
- Implementation** 59:133
- Implication** 56:135
- Importance** 61:203
- Inactivation**
 - Carbon-Dioxide 52:B29
 - Experimental-Data 65:99
 - Heated 65:99
 - Kinetic-Model 65:99
 - Leuconostoc-Dextranicum 52:B29
 - Pressure 52:B29
 - Strain 65:99
 - Strawberry-Product 65:99
 - Thermal 65:99
 - Yeast 65:99
- Incline** 60:141
- Inclined**
 - A-Priori-Information 56:167
 - Flow 56:167
 - Gas-Liquid-Flow 45:55
 - Hold-Up 45:55
 - Imaging 56:167
 - Modeling 56:167
 - Multiphase-Flow 56:167
 - Prediction 45:55
 - Profile 56:167
 - Two-Phase 45:55
 - Velocity 56:167
- Inconsistent-Data** 54:125
- Induced-Aeration** 54:199
- Industrial**
 - Acetifier 62:183, 65:201
 - Batch 62:183
 - Catalyst 57:273
 - Closed-System 62:183, 65:201
 - Computer-Simulation 62:183, 65:201
 - Copper(II) 57:273
 - γ -Alumina 57:273
 - Intrinsic-Kinetics 57:273
 - Methane 57:273
 - Operating-Condition 62:183, 65:201
 - Operation 62:183
 - Optimum 62:183, 65:201
 - Oxidation 57:273
 - Oxide 57:273
 - Semi-Continuous-Operation 65:201
 - Support 57:273
- Industrial-Application** 56:149
- Industrial-Scale** 51:B35
- Inelastic-Fluid** 50:33
- Inert-Membrane** 64:319
- Inert-Support** 60:189
- Infinite-Dilution** 46:35
- Influence**
 - Absorption 67:131
 - Adsorbent 53:147
 - Adsorption-Kinetics 53:147
 - Alga 47:B23
 - Anaerobic-Treatment 52:B21
 - Aqueous 67:97
 - Backmixing 48:71
 - Biological-Fluidized-Bed 52:B21
 - Bubbling 67:131
 - Bulk-Copolymerization 48:71
 - Cadmium 47:B23
 - Carbon-Dioxide 67:131
 - Cell-Size-Distribution 47:B23
 - Chlorella-Vulgaris 47:B23
 - Coal 58:53
 - Competing-Reaction 61:41
 - Conical 62:113
 - Cost 61:41
 - Dispersion 62:89, 67:97
 - Distribution 67:83
 - Dynamics 48:71
 - Eddy 67:83
 - Element 62:89
 - Evaporator 62:89
 - Fast-Parallel-Reactions 58:15
 - Gel-Effect 48:71
 - Geometry 62:113
 - Gravimetric-Determination 53:147
 - Heat-Transfer 50:149
 - High-Strength 52:B21
 - Hydrodynamics 62:113
 - Hydrogenation 58:53
 - Kinetics 58:53
 - Liquid 62:89, 67:83
 - Liquid-Solid-Flow 67:83
 - Liquid-Phase 47:51
 - Longitudinal 62:89
 - Mass-Transfer-Resistance 47:51
 - Mo-Catalyzed 58:53
 - Nature 58:53
 - Non-Maintained 67:83
 - Organic-Loading-Rate 52:B21
 - Packed-Column 47:51
 - Particle 53:147
 - pH 67:97
 - Porous 58:53
 - Presence 67:83
 - Product-Distribution 58:15
 - Protein 61:41
 - Rate-Parameter 48:71
 - Refolding 61:41
 - Rheology 67:97
 - Section 62:113
 - Semisynthetic-Waste-Water 52:B21
 - Shallow 62:113
 - Solid 67:83
 - Spiral 62:89
 - Spouted-Bed 62:113
 - Stability 67:97
 - Staying-Time 67:83
 - Stirred-Tank 67:131
 - Strategy 61:41
 - Surfactant 67:131
 - Temperature 67:97
 - Theoretical-Analysis 48:71
 - Thin-Layer 62:89
 - Thin-Layer-Evaporator 50:149
 - Titanium-Dioxide 67:97
 - Transfer 53:147
 - Tubular-Reactor 48:71
 - Vibrating-Element 50:149
 - Viscosity 47:51, 58:15
 - Zinc 47:B23
- Inhibition-Kinetics** 57:B23
- Inhibitory-Effect** 53:B13
- Inhibitory-Substrate**
 - Characteristics 55:B47
 - Continuous-Stirred-Tank-Bioreactor 50:B1, 55:B47
 - Degrading 50:B1
 - Fed 55:B47
 - Operational-Range 50:B1
 - Stability 55:B47
 - Upper-Limit 55:B47
- Inlet** 52:137
- Inorganic-Membrane** 48:11
- Inorganic-Substance** 54:147
- Input** 51:29
- Inside** 62:51
- Instantaneous-Reaction** 51:93
- Insulant-Production** 44:B81
- Intact-Insulin** 65:257
- Integral** 44:B25
- Integral-Flow-Reactor** 46:79
- Integral-Reactor** 63:45
- Integral-Spectral-Approach** 68:11
- Integration**
 - Butanol 46:B1, 46:B11
 - Cell 46:B11
 - Continuous-Fermentation 46:B1, 46:B11
 - Experimental-Result 46:B1
 - Immobilized 46:B11
 - Immobilized-Cell 46:B1
 - Mathematical-Modeling 46:B11
 - Pervaporation 46:B1, 46:B11
 - Simulation 46:B11
- Interaction**
 - Application 62:193
 - Biochemical 62:193
 - Boundary-Layer 66:201
 - Cross-Flow 66:201
 - Flow 62:193
 - Hydrodynamical 62:193
 - Liquid 62:193
 - Particle 62:193
 - Particle-Turbulence 66:201
 - Tube 66:201
 - Turbulent 66:201
- Interaction-by-Exchange-with-the-Mean** 45:25
- Interfacial** 57:205
- Interfacial-Stretching** 64:129
- Intermediate** 53:167

- Intermittent-Flow-Regime** 64:149
- Intermittent-Operation** 52:73
- Internal** 56:B61
- Internal-Circulation** 66:105
- Internal-Diffusion** 43:B13
- Internal-Fouling** 60:31
- Internal-Loop-Airlift-Reactor** 57:B7
- Interpretation**
 - Carbon 57:137
 - Catalytic-Cracking 44:53
 - Experimental-Data 44:53
 - Fluidized-Bed 44:53
 - Kinetic-Model 44:53
 - Langmuir-Kinetics 57:137
 - Mass-Transfer 57:137
 - Molecular-Sieve 57:137
 - Multistage-Reactor 44:53
 - Oil-Fraction 44:53
 - Single-Stage-Reactor 44:53
- Intraparticle** 53:1
- Intraparticle-Convection** 54:41
- Intraparticle-Kinetic-Parameter** 58:239
- Intrinsic-Kinetics** 57:273
- Inverse** 51:109
- Inversion**
 - Diffusivity 61:7
 - Evaluation 61:7
 - Fine 58:45
 - Ion-Exchange 61:7
 - Liquid-Liquid-Dispersion 58:45
 - Method 58:45
 - Phase 58:45
 - Reaction-Rate 61:7
 - Separation 58:45
 - Solution 61:7
 - Sucrose 61:7
- Ion** 62:73
- Ion-Exchange**
 - Amberlite-252 66:137
 - Ammonia-Removal 66:65
 - Anaerobically-Treated 66:65
 - Chromatography 64:307
 - Column 66:65
 - Diffusivity 61:7
 - Economical-Optimization 64:307
 - Evaluation 61:7
 - Exploring 57:75
 - Extraction 64:307
 - Fluidized 64:307
 - Homoionic-Zeolite 66:65
 - Inversion 61:7
 - Maxwell-Stefan-Description 57:75
 - Mixture 66:137
 - Modeling 64:307
 - Packed 66:65
 - Piggery-Manure 66:65
 - Potassium 66:137
 - Reaction-Rate 61:7
 - Removal 66:137
 - Simplified 64:307
 - Solution 61:7
 - Sucrose 61:7
 - Water-Methanol-Polyol 66:137
 - Whey-Protein 64:307
- Ion-Exchange-Equilibrium** 44:113
- Ion-Exchange-Membrane** 47:75
- Ion-Exchange-Process**
 - Corrected-Fick's-Law 61:123
 - Cyclic-Regime 43:B53
 - Equivalence 61:123
 - Fixed-Bed 61:123
 - Kinetic-Mechanism 57:17
 - Modeling 43:B53, 61:123
 - Nernst-Planck-Law 61:123
 - Optimization 43:B53
 - Sugar-Juice-Softening 43:B53
- Ion-Exchange-Resin** 61:149
- Ionic-Bubble** 57:1
- Ionic-Transport** 47:75
- Irreversible-Reaction** 60:111
- Isobutanol** 50:115
- Isocyanuric-Acid** 62:13
- Isomerization**
 - 1-Butene 60:147, 64:265
 - Acid 64:265
 - Adsorption-Enthalpy 60:147
 - Al₂O₃ 64:265
 - Bronsted-Type 64:265
 - Catalyst 60:147, 64:265
 - Direct-Test 60:147
 - Mixed-Oxide 64:265
 - Relationship 64:265
 - Silica-Alumina 60:147
 - Silicon-Dioxide 64:265
 - Site 64:265
 - Solid 64:265
 - Surface-Active 64:265
 - Titanium-Dioxide 64:265
 - Zirconium-Dioxide 64:265
- Isopropylation** 54:79
- Isopropylbenzene** 58:7
- Isotherm** 49:167
- Isothermal**
 - Catalyst 54:41
 - Concentration-Dependent 43:1
 - Conversion 54:41
 - Corrugated-Wall 54:23
 - Deactivation 43:1
 - Experimental-Study 54:23
 - First-Order-Reaction 54:41
 - Fixed-Bed-Catalytic-Reactor 43:1
 - Fixed-Bed-Reactor 54:41
 - Flowing 54:23
 - Heterogeneous-Reactor 54:41
 - Hydrodynamics 54:23
 - Intraparticle-Convection 54:41
 - Large-Pore 54:41
 - Liquid-Film 54:23
 - Parametric-Study 43:1
 - Tubular-Column 54:23
- Isothermal-Oxidative-Stabilization** 49:133
- Isotropic-Turbulence** 43:B19
- Isozyme** 65:105
- Jacketed** 58:135
- Jet** 63:11
- Jet-Flame** 53:39
- K-Na-Exchange** 54:17
- Kenics-Static-Mixer**
 - Chaotic-Flow 67:153
 - Data-Correlation 59:265
 - Three-Dimensional 67:153
- Kinematic-Viscosity**
 - 1,2-Ethanediol 52:41
 - 2-Methoxyethanol 52:41
 - Binary-Mixture 52:41
 - Crude-Oil 51:151
 - Different 52:41
 - Estimation 51:151
 - Fraction 51:151
 - Neural-Network 51:151
 - Petroleum 51:151
 - Temperature 52:41
- Kinetic-Behavior** 53:183
- Kinetic-Mechanism** 57:17
- Kinetic-Parameter**
 - Antibiotic-Separation 65:63
 - Application 51:77, 65:63
 - Biodegradation 56:B91
 - Calcined 47:1
 - Coefficient 65:63
 - Continuous-Stirred-Tank-Reactor 65:63
 - Determination 47:1
 - Estimation 51:77, 53:193
 - Evaluate 65:63
 - Evaluation 56:B91
 - Experiment 53:193
 - Fast-Fourier-Transform 51:77
 - Fixed-Bed 53:193
 - Fixed-Bed-Reactor 51:77
 - Flow 53:193
 - Gas 47:1
 - Hydrogen-Chloride 47:1
 - Kinetics 56:B91
 - Limestone 47:1
 - Maldistribution 53:193
 - Mass-Transfer 65:63
 - Metal-Cutting 56:B91
 - Oil 56:B91
 - Reaction 47:1
 - Thermogravimetry 47:1
 - Tracer 53:193
 - Transport 53:193
- Kinetic-Process** 43:B93
- Kinetics**
 - Acid 67:55
 - Acidic 60:63
 - Adsorption 49:11
 - Alkaline 49:B17
 - Amberlite 58:285
 - Anaerobic 54:B25
 - Anaerobic-Digestion 54:B9
 - Autocatalytic-Reaction 66:231
 - Backward-Extraction 60:63
 - Bacterial-Adaptation 56:B115
 - Benzyl-Chloride 53:107
 - Biodegradation 56:B91
 - Biofilm-Reactor 65:227
 - Bioremediation 56:B115
 - Biological-Batch-Reactor 56:B43
 - Biomass 54:B9
 - Bioparticle 65:117
 - Bone-Powder 67:55
 - Burning-Coke 54:35
 - Calcium-Oxide 46:119
 - Calculation 54:35, 55:125
 - Carbon-Dioxide 44:107
 - Carbon-Formation 46:129
 - Carrier 58:285
 - Catalyst 54:35
 - Catalytic-Transfer 51:B51
 - Cell 58:285
 - Chemo-Autotrophic-Biogas 58:71
 - Coal 58:53
 - Cod 56:B43
 - Coke 55:125
 - Comparison 55:125
 - Constant-Interface-Area 58:285
 - Corn 59:221, 60:39
 - Cow-Manure 54:B9
 - Deactivation 55:125
 - Denitrification 65:227
 - Desulfurization 46:119
 - Determination 48:119
 - Digestion 56:B109
 - Diglycolamine 44:107
 - Dissolution 48:119
 - Dry 46:119
 - Drying 59:221, 60:39
 - Elaboration 67:55
 - Electrochemical-Reactor 53:137
 - Electrostatic-Interaction 57:B15
 - Elliptic-Integral 66:231
 - Enrichment 58:71
 - Ethanol 54:221
 - Evaluation 56:B91
 - Experimental-Set-Up 49:11
 - Experimental-Study 54:221, 59:221, 67:55
 - Extractant 60:63
 - Extraction 58:285
 - Fermentation 54:221
 - Ferrous-Sulfide 56:B115
 - Flotation 59:221
 - Flotation-Bed 60:39
 - Fluidized 60:39, 65:117
 - Fluidized-Bed 48:119, 59:221
 - Fluidized-Bed-System 54:B25

- Forward-Extraction 60:63
- Fresh-Water 56:B109
- Fruit 54:B25
- Gelatin-Production 67:55
- Growth 48:119
- H₂O 46:79
- H₂S 46:79
- High-Conversion 55:87
- Hyacinth 56:B109
- Hydrodenitrogenation 46:79
- Hydrogenation 51:B51, 58:53
- Immobilized 54:B9
- Immobilized-Enzyme 57:B15
- Impeller 56:B43
- Influence 58:53
- Integral-Flow-Reactor 46:79
- Isopropylation 54:79
- Kinetic-Parameter 56:B91
- Lignin 49:B17
- Low-Pressure 58:101
- Macroapproach 54:221
- Mathematical-Modeling 54:221
- Mathematical-Treatment 57:61
- Mechanism 56:B115, 58:71
- Metal-Cutting 56:B91
- Methane 58:71
- Methane-Hydrogen-Mixture 46:129
- Methanol 58:101
- Method 55:125
- Methylcyclohexane 67:123
- Mo-Catalyzed 58:53
- Mobile 58:285
- Modeling 57:B15, 60:39, 67:55, 67:123
- Monoester 60:63
- Morpholine 44:107
- N,N-Dialkylhydrazine 57:61
- Nature 58:53
- Neodymium 60:63
- NH₃ 46:79
- Nickel-Alumina-Catalyst 46:129
- Nitrobenzene 49:B17
- Oil 56:B91
- Overall-Scheme 67:55
- Oxidation 49:B17, 67:115
- Penicillin-G 58:285
- Percolation 53:137
- pH-Change 57:B15
- Phenol 67:115
- Phosphonic-Acid 60:63
- Poly-(18-Dibenzo-6-Crown) 53:137
- Porous 58:53
- Porous-Electrode 53:137
- Presence 46:79
- Process 67:55
- Processing 54:B25
- Pulsed 53:137
- Purification 54:B25, 58:71
- PVC 55:87
- Pyrolysis 55:87, 67:123
- Quaternization 53:107
- Quinoline 46:79
- Raschig-Process 57:61
- Reaction 44:107
- Reaction-Generated 57:B15
- Reactive-Intermediate-Species 66:231
- Reduction 56:B43
- Regeneration 54:35
- Rice-Straw 49:B17
- Rotating-Disk 65:227
- Saccharomyces-Cerevisiae 54:221
- Semicontinuous-Operation 56:B109
- Sodium-Perborate-Tetrahydrate 48:119
- Soybean-Oil 51:B51
- Speed 56:B43
- Submergence 56:B43
- Substrate-Inhibition 65:117
- Synthesis 53:137, 57:61, 58:101
- Temperature-Ramp 54:35
- Termolecular-Reaction 66:231
- Tertiary-Amine 53:107
- Thermal-Measurement 49:11
- Thermodynamics 58:101
- Toluene 54:79
- Waste 55:87
- Waste-Water 54:B25
- Wet-Air 67:115
- Zeolite 54:B9
- Zeolite-Catalyzed 54:79
- Knowledge** 54:155
- Kolmogorov-Theory** 43:B19
- Krone-Doolittle-Equation** 60:117
- Kurihara-Mixing-Rule** Modified-> 61:213
- Kühni-Column** 44:27
- L-Alanine-Production** 65:109
- L-Carnitine** 61:53
- L-Lysine-Production** 61:35
- L-Sorbose** 45:B5
- Lactic-Acid** 65:47
- Lactose**
 - Aspergillus-Niger 52:B1
 - β -Galactosidase 65:93
 - Chitosan 65:93
 - Dissolution 53:B25
 - Fixed-Bed-Reactor 65:93
 - Free- β -Galactosidase 52:B1
 - Hydrolysis 52:B1, 65:93
 - Immobilized 65:93
 - Immobilized- β -Galactosidase 52:B1
 - Mathematical-Model 53:B25
 - Modeling 52:B1
 - Simulation 52:B1
- Laminar**
 - Arrangement 55:15
 - Condition 55:15
 - Falling-Film 49:119
 - Fully-Developed-Flow 55:15
 - Heat-Transfer 49:119
 - Liquid 49:119
 - Mass-Transfer 49:119
 - Multicomponent 49:119
 - Numerical-Study 55:15
 - Reaction 49:119
 - Simultaneous 49:119
 - Wavy-Walled-Pipe 55:15
- Laminar-Flow**
 - Circular-Tube 55:103
 - Coupling 55:103
 - Dynamics 58:145
 - External 55:103
 - Filter 58:145
 - Fluid 45:43
 - Free-Convection 55:103
 - Heat-Transfer 55:103
 - Hydrodynamics 58:145
 - Pipe 45:43
 - Residence-Time-Distribution 45:43
 - Rotary 58:145
 - Vertical-Tube 55:103
- Langmuir-Freundlich-Isotherm-Equation** | Generalized-> 64:85
- Langmuir-Kinetics** 57:137
- Large-Polydisperse-Particle** 61:161
- Large-Pore**
 - Adsorption-Process 60:81
 - Analysis 60:81
 - Apparent 60:81
 - Catalyst 54:41
 - Catalytic-Process 60:111
 - Conversion 54:41, 60:111
 - Criterion 60:81
 - Diffusion 60:81
 - Diffusion-Convection 60:81
 - Driving-Force 60:81
 - Equivalence 60:81
 - Extended-Linear-Model 60:81
 - First-Order-Reaction 54:41, 60:111
 - Fixed-Bed-Reactor 54:41
 - Flow-Rate 60:111
 - Heterogeneous-Reactor 54:41
 - Intraparticle-Convection 54:41
 - Irreversible-Reaction 60:111
 - Isothermal 54:41
 - Material 60:81, 60:111
 - Operating-Temperature 60:111
 - Plug-Flow-Reactor 60:111
- Large-Scale**
 - Batch 51:B43
 - Biosynthesis 51:B43
 - Cell 59:1
 - Column 59:1
 - Continuous-Chromatography 51:B43
 - Dextran 51:B43
 - Dextransucrase 51:B43
 - Flotation 59:1
 - Flow-Specification 50:133
 - Fluid 50:133
 - Leuconostoc-Mesenteriodes 51:B43
 - Mixed-Pressure 50:133
 - Network-Analysis 50:133
 - Performance 59:1
 - Pilot-Plant-Data 59:1
 - Prediction 59:1
 - Purification 51:B43
- Latex** 60:31
- Layout** 63:167
- Leaching** 54:207
- Lemna-Gibba**
 - Dynamic-Modeling 57:B37
 - Plant 57:B37
 - Pollutant 54:B41
 - Removal 54:B41
 - Waste-Water-Treatment 57:B37
 - Water 54:B41
- Leuconostoc-Dextranicum** 52:B29
- Leuconostoc-Mesenteriodes** 51:B43
- Level**
 - Amyloglucosidase 51:B17
 - Bed 51:B17
 - Depth 51:B17
 - Different 51:B17
 - Fermentation 51:B17
 - Mixer 56:119
 - Performance 56:119
 - Positron-Camera 56:119
 - Powder 56:119
 - Solid-State 51:B17
 - Temperature-Variation 51:B17
- Light-Energy** 45:1
- Light-Hydrocarbon** 57:145
- Lignin** 49:B17
- Limestone**
 - Absorption 51:99
 - Calcined 47:1
 - Determination 47:1
 - Gas 47:1
 - Hydrogen-Chloride 47:1
 - Kinetic-Parameter 47:1
 - Reaction 47:1
 - Slurry 47:99
 - Sulfur-Dioxide 51:99
 - Thermogravimetry 47:1
- Limit** 58:33
- Limitation**
 - Experimental-Assessment 43:B13
 - Gas 59:195
 - Internal-Diffusion 43:B13
 - Mass-Transfer 59:195
 - Microbial-System 59:195
 - Substrate 59:195

- Uncoupling 59:195
- Yeast-Floes 43:B13
- Linear** 64:21
- Linear-Controller** 64:141
- Linear-Diffusion-Reaction-Problem** 47:169
- Linear-Product** 57:B23
- Linear-Transport-Phenomena** 64:45
- Linear-Type** 43:B43
- Lipase**
 - Acrylic 65:249
 - Copolymer 65:249
 - Immobilization 61:149, 65:249
 - Ion-Exchange-Resin 61:149
 - Mucor-Miehei 61:149
- Liposome**
 - Antigen-Coupled 54:B33
 - Characterization 54:B33
 - Homogeneous 54:B33, 62:169
 - Immunoassay 54:B33, 62:169
 - Peptide-Coupled 62:169
 - Polyclonal-Antibody 54:B33, 62:169
 - Protein 62:169
- Lipozyme** 65:159
- Liquid**
 - Accumulation-Effect 59:281
 - Agitated 62:23
 - Agitated-Vessel 48:41
 - Application 48:41, 62:193
 - Axial-Dispersion 44:51, 44:52
 - Behavior 50:87
 - Biochemical 62:193
 - Breakage 62:23
 - Carbon-Dioxide 61:227
 - Carrier 63:127, 66:11
 - Coalescing-Property 55:1
 - Comparison 61:227
 - Conventional 61:227
 - Critical-Pressure 59:127
 - Density 59:127
 - Dependence 52:31
 - Dispersion 62:89
 - Distribution 67:83
 - Eddy 67:83
 - Element 62:89
 - Emulsion 63:127, 66:11
 - Equipped 56:51
 - Estimation 59:127
 - Europium 57:253
 - Evaporator 56:51, 62:89
 - Experimental-Investigation 59:281
 - Experimental-Technique 48:41
 - Extended-Thomas-Method 44:173
 - External-Loop-Airlift-Contactor 66:91
 - Extraction 57:253, 61:227
 - Facilitated 63:127, 66:11
 - Falling-Film 49:119
 - Floe 62:23
 - Flow 62:193
 - Fluidized-Bed 50:87, 51:135, 55:1
 - Fluorinated-Hydrocarbon 44:173
 - Gas 59:281
 - Gas-Liquid-Solid-Fluidized-Bed 44:51, 44:52
 - Gas-Liquid-Separator 66:91
 - Gas-Bubble 48:41
 - Gas-Flow 61:95
 - Global 66:91
 - Grape 61:227
 - Heat 59:127
 - Heat-Capacity 52:31
 - Heat-Transfer 49:119, 55:1
 - Height 66:91
 - Highly-Viscous-Liquid 48:41
 - Hydrodynamic-Parameter 66:91
 - Hydrodynamical 62:193
 - Hydrodynamics 55:1
 - Influence 62:89, 67:83
 - Interaction 62:193
 - Laminar 49:119
 - Liquid-Solid-Flow 67:83
 - Longitudinal 62:89
 - Mass-Transfer 48:41, 49:119, 55:1
 - Measurement 48:41
 - Membrane 57:253, 63:127, 66:11
 - Metering 59:281
 - Mobile-Carrier 57:253
 - Modeling 63:127, 66:11
 - Molecular-Structure 52:31
 - Monosized-Crystal 50:87
 - Movement 51:135
 - Multicomponent 49:119
 - Non-Maintained 67:83
 - Oil 61:227
 - Orifice 59:281
 - Packed-Bed 48:61
 - Packing 61:95
 - Particle 51:135, 62:193
 - Pattern 61:95
 - Phosphorus-Containing-Compound 51:41
 - Prediction 44:173, 51:41
 - Presence 67:83
 - Pure-Substance 59:127
 - Radial-Spreading 48:61
 - Random 61:95
 - Rational-Description 48:61
 - Reaction 49:119
 - Recovery 61:227
 - Residence-Time 56:51
 - Rotating-Mixer 62:23
 - Seed 61:227
 - Simultaneous 49:119
 - Sodium-Perborate 50:87
 - Solid 51:135, 67:83
 - Solvent-Extraction 61:227
 - Souder-Method 51:41
 - Spiral 62:89
 - Spiral-Element 56:51
 - Staying-Time 67:83
 - Supercritical 61:227
 - Supported 57:253
 - Suspension 62:23
 - Temperature 52:31
 - Thin-Layer 56:51, 62:89
 - Three-Phase 55:1
 - Trickle-Flow 48:61
 - Trivalent 57:253
 - Two-Phase-Flow 59:281
 - Vaporization 59:127
 - Vibrating-Mixer 62:23
 - Viscosity 44:173, 51:41
- Liquid-Liquid-Dispersion**
 - Computer-Assisted-Image-Analysis 49:141
 - Determination 49:141
 - Development 49:141
 - Fine 58:45
 - Granulometric-Distribution 49:141
 - Inversion 58:45
 - Method 58:45
 - Phase 58:45
 - Separation 58:45
 - Solid-Liquid-Dispersion 49:141
 - Solid-Solid-Dispersion 49:141
- Liquid-Liquid-Extraction** 56:B1
- Liquid-Liquid-Extraction-Column** 45:111
- Liquid-Liquid-Mass-Transfer** 54:7
- Liquid-Solid-Circulating** 68:51
- Liquid-Solid-Flow**
 - Correlation 55:39
 - Distribution 67:83
 - Eddy 67:83
 - Heat-Transfer 55:39
 - Horizontal-Pipe 55:39
 - Influence 67:83
 - Liquid 67:83
 - Non-Maintained 67:83
 - Presence 67:83
 - Solid 67:83
 - Staying-Time 67:83
- Liquid-Solid-Loop-Reactor** 63:181
- Liquid-Solid-Mass-Transfer**
 - Batch-Packed 54:51
 - Bubble-Column 54:51
 - Experiment 63:1
 - Gas-Liquid-Controlling 62:61
 - Low-Reynolds-Number 63:1
 - Model 63:1
 - Packed-Bed 62:61, 63:1
 - Particle 63:1
 - Raschig-Ring 62:61
 - Two-Phase-Flow 62:61
 - Variously-Shaped 63:1
- Liquid-Chromatography** 61:191
- Liquid-Dispersion** 53:151
- Liquid-Distribution** 48:49
- Liquid-Film**
 - Corrugated-Wall 54:23
 - Distribution 59:259
 - Experimental-Study 54:23
 - Flowing 54:23
 - Hydrodynamics 54:23
 - Isothermal 54:23
 - Residence-Time 59:259
 - Tubular-Column 54:23
 - Wiped 59:259
- Liquid-Flow** 52:63
- Liquid-Fluidization** 46:15
- Liquid-Fluidized-Bed** 49:17
- Liquid-Foam** 56:187
- Liquid-Fuel** 60:49
- Liquid-Jet** 44:157
- Liquid-Mixing**
 - Air-Water-System 53:167
 - Gas 53:167
 - Gas-Hold-Up 53:167
 - Intermediate 53:167
 - Low-Velocity 53:167
 - Mixer 48:135
 - Mixing-Time 48:135
 - Power-Consumption 48:135
 - Ribbon 48:135
- Liquid-Mixture** 48:183
- Liquid-Phase**
 - Airlift-Bioreactor 57:B31
 - Animal-Cell 57:B31
 - Catalysis 43:33
 - Cobalt-Salt 43:33
 - Convective-Mass-Transfer 62:43
 - Downjet-Loop-Reactor 49:49
 - Epitaxial-Growth 62:43
 - Gas-Hold-Up 49:49
 - Influence 47:51
 - Local-Flow-Behavior 57:B31
 - Mass-Transfer-Coefficient 49:49
 - Mass-Transfer-Resistance 47:51
 - Normal-Octane 43:33
 - Overall-Kinetics 43:33
 - Oxidation 43:33
 - Packed-Column 47:51
 - Potential 57:B31
 - Product-Distribution 43:33
 - Short-Time 62:43
 - Suspension-Culture 57:B31
 - Viscosity 47:51
 - Volumetric 49:49
- Liquid-Side** 58:251
- Liquid-Test-System** 46:137
- Liquor** 59:287
- Local**
 - Baffled 66:1
 - Characteristics 53:67

- Current 66:1
- Description 61:73
- Distribution 66:1
- Electrochemical-Reactor 66:1
- Fluidized-Bed 61:73
- Gas-Liquid-Ejector 53:67
- Global 61:73
- Hydrodynamics 53:67
- Mass-Transfer 53:67, 66:1
- Modeling 61:73
- Parallel-Plate 66:1
- Structure 61:73
- Turbulent 61:73
- Unbaffled 66:1
- Local-Flow-Behavior** 57:B31
- Local-Heat-Transfer** 46:47
- Long-Chain** 66:35
- Long-Cylindrical-Particle** 45:123
- Longitudinal** 62:89
- Loop-Reactor** 44:B57
- Low-Concentration** 53:B41
- Low-Cost**
 - Apparent-Yield-Stress 45:B49
 - Construction 56:B75
 - Electroporator 56:B75
 - Escherichia-Coli 56:B75
 - Estimation 45:B49
 - Fermentation-Broth 45:B49
 - High-Efficiency 56:B75
 - Simple 56:B75
 - Strain 56:B75
 - Transformation 56:B75
 - Viscometer 45:B49
 - Xanthan-Gum-Solution 45:B49
- Low-Frequency** 65:145
- Low-Pressure**
 - Chemical-Vapor-Deposition-Reactor 57:39
 - Gas 56:67
 - Generalization 56:67
 - Horizontal 57:39
 - Hot-Wall 57:39
 - Kinetics 58:101
 - Methanol 58:101
 - Mixture 56:67
 - Modeling 57:39
 - Simple 56:67
 - Synthesis 58:101
 - Thermal 57:39
 - Thermodynamics 58:101
 - Tubular 57:39
 - Viscosity 56:67
- Low-Pressure-Drop** 45:79
- Low-Reynolds-Number**
 - Cocurrent-Upflow-Bioreactor 62:237
 - Dynamic-Liquid-Hold-Up 62:237
 - Experiment 63:1
 - High 59:153
 - Liquid-Solid-Mass-Transfer 63:1
 - Mass-Transfer 59:153, 62:237
 - Model 59:153, 63:1
 - Oxygen 62:237
 - Packed-Bed 63:1
 - Particle 63:1
 - Prediction 59:153
 - Schmidt-Number 59:153
 - Small-Packing 62:237
 - Turbulence 59:153
 - Turbulent 59:153
 - Variously-Shaped 63:1
- Low-Velocity** 53:167
- Lysine-Production** 62:207
- Macedo-Litovitz-Equation** 60:117
- Macro-Instability** 67:139
- Macroapproach** 54:221
- Macropore** 55:81
- Magnesium-Chloride-Rich** 52:89
- Magnesium-Sulfate** 52:89
- Magnetically-Stabilized** 61:241
- Magnetized-Fluidized-Bed** 50:59
- Main-Fractionator** 44:119
- Maintenance-Coefficient** 62:215
- Maldistribution** 53:193
- Malic-Acid** 56:B9
- Mammalian-Cell** 65:123
- Manganese-Metal** 54:167
- Marangoni-Instability** 58:151
- Mass-Input** 45:99
- Mass-Transfer**
 - Absence 43:41
 - Adsorption 54:B1
 - Aerated 59:187
 - Agitated-Vessel 48:41
 - Airlift-Bioreactor 56:B101
 - Airlift-Fluidized-Bed 49:89, 55:143, 55:145
 - Airlift-Reactors 65:263
 - Annular-Swirling-Decay 52:137
 - Antibiotic-Separation 65:63
 - Application 48:41, 65:63
 - Baffled 66:1
 - Biocatalyst 44:B41
 - Bioreactor 59:187, 61:241, 62:175
 - Boundary-Layer 44:B41
 - Bubble 59:187
 - Cadmium 53:183
 - Capillary-Gap-Cell 43:107
 - Carbon 57:137
 - Characteristics 43:95, 53:67, 54:63, 58:251
 - Chelated 53:183
 - Chemical-Reaction 57:205
 - Coalescing-Property 55:1
 - Cocurrent 63:93
 - Cocurrent-Upflow-Bioreactor 62:237
 - Coefficient 55:B1, 65:63
 - Column 55:B1
 - Continuous-Stirred-Tank-Reactor 65:63
 - Current 66:1
 - Design 49:89, 55:143, 55:145
 - Determination 59:187
 - Development 58:123
 - Dispersion 67:45
 - Dissolution 66:57
 - Distillation 57:177
 - Distribution 66:1
 - Dynamic-Liquid-Hold-Up 62:237
 - Electrochemical-Reactor 66:1
 - Elevated 54:63
 - Energy 45:123
 - Enhancement 51:93
 - Entrainment 59:187
 - Enzyme 55:B1
 - Estimation 43:41
 - Ethanol 54:63
 - Evaluate 65:63
 - Experimental-Determination 44:B41
 - Experimental-Technique 48:41
 - Experimental-Verification 58:123
 - External-Loop-Airlift-Reactor 67:205
 - Extraction 55:B1
 - Factor 51:93
 - Falling-Film 49:119
 - Film 43:41, 52:19, 64:361
 - Flow-Induced 52:137
 - Fluid 52:19, 64:361
 - Fluidized-Bed 55:1, 61:241
 - Forced-Flow 45:123
 - Gas 54:63, 59:195
 - Gas-Liquid-Circulation 56:B101
 - Gas-Liquid-Cocurrent-Downflow 58:83
 - Gas-Liquid-Ejector 53:67
 - Gas-Bubble 48:41
 - Gas-Disengagement 65:263
 - Gas-Sparging 47:187
 - Heat 50:79, 58:123
 - Heat-Transfer 49:119, 55:1
 - Heterogeneous-System 50:79
 - High 59:153
 - Highly-Viscous-Liquid 48:41
 - Hydrodynamic-Characteristics 65:263
 - Hydrodynamics 43:95, 43:107, 53:67, 55:1, 58:83, 62:175, 63:93, 67:205
 - Immobilization 54:B1
 - Immobilized-Enzyme-System 61:241
 - Inlet 52:137
 - Instantaneous-Reaction 51:93
 - Interfacial 57:205
 - Interpretation 57:137
 - Kinetic-Behavior 53:183
 - Kinetic-Parameter 65:63
 - Laminar 49:119
 - Langmuir-Kinetics 57:137
 - Limitation 59:195
 - Liquid 48:41, 49:119, 55:1
 - Liquid-Side 58:251
 - Local 53:67, 66:1
 - Long-Cylindrical-Particle 45:123
 - Low-Reynolds-Number 59:153, 62:237
 - Magnetically-Stabilized 61:241
 - Matrix 54:B1
 - Measurement 48:41
 - Membrane 62:175
 - Methanol 54:63
 - Microbial-System 59:195
 - Model 52:19, 58:123, 59:153, 64:361
 - Modeling 49:89, 55:143, 55:145, 57:177, 67:45
 - Molecular-Sieve 57:137
 - Momentum 58:123
 - Multicomponent 49:119, 52:19, 57:177, 64:361
 - Non-Newtonian-Fluid 56:B101
 - Nonideal-Mixture 52:19, 64:361
 - Nonideal-Phenomena 57:205
 - Nonisothermal 51:93
 - Operational 55:143
 - Operational-Parameter 49:89, 55:145
 - Optimization 49:89, 55:143, 55:145
 - Organic-Compound 67:45
 - Oxygen 62:237
 - Packed-Bed 45:123
 - Packed-Bubble-Column 43:95
 - Packed-Column 63:93
 - Packing 58:251
 - Parallel-Plate 66:1
 - Parameter 55:143, 59:187
 - Polymer 67:45
 - Prediction 59:153
 - Pressure 54:63
 - Promoter 43:107
 - Rate 47:187
 - Reaction 49:119
 - Resistance 43:41
 - Respect 55:143
 - Rigid-Drop-Model 51:93
 - Role 57:205
 - Schmidt-Number 59:153
 - Sieve-Plate 55:B1
 - Simultaneous 49:119
 - Single-Sphere 47:187
 - Small-Packing 62:237
 - Solid 66:57
 - Solution 53:183
 - Solution-Method 50:79
 - Spherical-Particle 44:B41

- Spray-Drying 58:123
- Structured 58:251
- Substrate 59:195
- Surface 59:187
- Surface-Active-Agent 65:263
- Surface-Diffusivity 43:41
- Tangential 52:137
- Temperature 54:63
- Theoretical-Study 63:93
- Three-Phase 55:1
- Three-Phase-Fixed-Bed-Reactor 58:83
- Tool 61:241
- Turbulence 43:107, 59:153
- Turbulent 59:153
- Unbaffled 66:1
- Uncoupling 59:195
- Viscous 56:B101
- Volatile 67:45
- Vortex 62:175
- Wave 62:175
- Mass-Transfer-Reaction-Coupling** 57:189
- Mass-Transfer-Characteristics** 47:33
- Mass-Transfer-Coefficient**
 - Correlation 63:157
 - Determination 57:67
 - Downjet-Loop-Reactor 49:49
 - Estimation 45:133
 - Extraction-Column 45:133
 - Gas-Absorption 57:67
 - Gas-Hold-Up 49:49
 - Liquid-Phase 49:49
 - Numerical-Technique 45:133
 - Packed-Column 57:67
 - Physical-System 57:67
 - Pulsed-Baffled-Reactor 63:157
 - Scale-Up 63:157
 - Technique 57:67
 - Volumetric 49:49
- Mass-Transfer-Resistance** 47:51
- Mass-Transport**
 - Chemical-Reaction 57:115
 - Description 57:115
 - Dusty-Gas 57:115
 - Maxwell-Stefan-Description 57:155
 - Membrane 57:155
 - Model 57:115
 - Porous-Medium 57:115
 - Zeolite 57:155
- Material**
 - Adsorption-Process 60:81
 - Analysis 60:81
 - Apparent 60:81
 - Catalytic-Process 60:111
 - Conversion 60:111
 - Criterion 60:81
 - Diffusion 60:81
 - Diffusion-Convection 60:81
 - Driving-Force 60:81
 - Equivalence 60:81
 - Extended-Linear-Model 60:81
 - First-Order-Reaction 60:111
 - Flow-Rate 60:111
 - Geometrical 62:1
 - Irreversible-Reaction 60:111
 - Large-Pore 60:81, 60:111
 - Model 62:1
 - Operating-Temperature 60:111
 - Plug-Flow-Reactor 60:111
 - Porous-Medium 62:1
 - Random 62:1
 - Two-Phase 62:1
- Mathematical-Description**
 - Correct 66:149, 66:151
 - Model 66:149, 66:151
 - Packed-Column 66:149, 66:151
- Mathematical-Formulation** 68:11
- Mathematical-Treatment** 57:61
- Matrix** 54:B1
- Maximum**
 - Bubble-Size 49:B13
 - Calcium 66:171
 - Consumption 62:149
 - Effectiveness-Factor 62:149
 - Fly-Ash 66:171
 - Gas-Liquid-Bioreactor 49:B13
 - Hollow-Fiber-Biofilm-Reactor 62:149
 - Hydroxide 66:171
 - Mixture 66:171
 - Removal 66:171
 - Stable 49:B13
 - Structural-Property 66:171
 - Substrate 62:149
 - Sulphur-Dioxide 66:171
 - Yield 66:171
- Maxwell-Stefan-Approach** 57:229
- Maxwell-Stefan-Description**
 - Electrodialysis 57:163
 - Exploring 57:75
 - Ion-Exchange 57:75
 - Mass-Transport 57:155
 - Membrane 57:155
 - Modeling 57:163
 - Zeolite 57:155
- Maxwell-Stefan-Equation|Generalized**→ 57:145
- Maxwell-Stefan-Model|Modified**→ 64:319
- Mean-Free-Path** 56:39
- Measurement**
 - Agitated-Vessel 48:41
 - Air-Water-Flow 66:131
 - Application 48:41
 - Chemical-Method 67:167
 - Comparison 67:167
 - Concentration 60:161
 - Contactor 52:121
 - Corrugated-Sheet 53:55
 - Cyclone-Reactor 48:83
 - Delineate 57:261
 - Distribution 53:55
 - Efficiency 48:83
 - Energy-Balance-Approach 63:105
 - Energy-Dissipation 63:105
 - Experimental-Technique 48:41
 - Fluidization 57:261
 - Gas-Liquid-Parameter 52:121
 - Gas-Bubble 48:41
 - Gas-Flow 53:55
 - Gas-Phase 48:83
 - Heat-Transfer 48:83, 61:107
 - Highly-Viscous-Liquid 48:41
 - Liquid 48:41
 - Liquid-Vessel 61:107
 - Mass-Transfer 48:41
 - Mechanically-Agitated 52:121
 - Mixed 61:107
 - Mixing-Time 67:167
 - Modeling 53:55
 - Onset 57:261
 - Oscillating-Grid 63:105
 - Packing 53:55
 - Physical-Method 67:167
 - Rate 63:105
 - Solid 60:161
 - Solid-Phase 48:83
 - Sound 66:131
 - Speed 66:131
 - Structured 53:55
 - Three-Phase-Reactor 60:161
 - Turbulence 57:261
 - Ultrasonic-Technique 60:161
 - Velocity 57:261
 - Vibratory-Agitator 61:107
 - Wall 48:83
- Mechanical** 46:69
- Mechanical-Mixing** 62:155
- Mechanically-Agitated**
 - Comparison 46:137
 - Contactor 52:121
 - Extraction-Column 46:137
 - Gas-Liquid-Parameter 52:121
 - Liquid-Test-System 46:137
 - Measurement 52:121
 - Single-Drop-Experiment 46:137
- Mechanically-Agitated-Three-Phase-Reactor** 49:107
- Mechanically-Stirred** 63:85
- Mechanism**
 - Bacterial-Adaptation 56:B115
 - Bioleaching 56:B115
 - Chemo-Autotrophic-Biogas 58:71
 - Electrolytic 54:167
 - Enrichment 58:71
 - Ferrous-Sulfide 56:B115
 - Kinetics 56:B115, 58:71
 - Manganese-Metal 54:167
 - Methane 58:71
 - Nitriding 54:167
 - Purification 58:71
- Mechanochemical-Processing** 66:79
- Mediator** 56:1
- Medium** 51:B1
- Membrane**
 - Adsorption 62:73
 - Alginate 56:B9
 - Application 57:145
 - Bioreactor 62:175
 - Bubble-Size 67:71
 - Calcium 56:B9
 - Carrier 63:127, 66:11
 - Change 62:73
 - Charge 62:73
 - Cross-Flow 60:31
 - Determination 56:B9
 - Dialysis 62:73
 - Diffusion-Coefficient 56:B9
 - Dilute 60:31
 - Emulsion 63:127, 66:11
 - Europium 57:253
 - Extraction 57:253
 - Facilitated 63:127, 66:11
 - Flux 67:71
 - Frequency 67:71
 - Gas 67:71
 - Generalized-Maxwell-Stefan-Equation 57:145
 - Glucose 56:B9
 - Hydrodynamics 62:175
 - Identification 56:B9
 - Internal-Fouling 60:31
 - Ion 62:73
 - Latex 60:31
 - Light-Hydrocarbon 57:145
 - Liquid 57:253, 63:127, 66:11
 - Malic-Acid 56:B9
 - Mass-Transfer 62:175
 - Mass-Transport 57:155
 - Maxwell-Stefan-Description 57:155
 - Microporous-Filtration 60:31
 - Mobile-Carrier 57:253
 - Model 56:B9
 - Modeling 63:127, 66:11
 - Permeability 62:73
 - Permeation 57:145, 67:71
 - Protein 62:73
 - Separation 57:145
 - Silicalite-1 57:145
 - Sparged 67:71
 - Supported 57:253
 - Suspension 60:31
 - Trivalent 57:253
 - Tubular 67:71
 - Ultrafiltration 67:71
 - Vortex 62:175
 - Wave 62:175
 - Zeolite 57:155
- Membrane-Distillation** 54:87

- Membrane-Partitioned-Electrode-Reactor** 47:25
- Membrane-Process** 58:175
- Membrane-Reactor** 49:35
- Mesophase-Pitch-Fiber** 49:133
- Mesophilic** 55:B55
- Mesoporous** 64:255
- Metal-Cutting** 56:B91
- Metal-Oxide** 64:295
- Metallic-Foam** 52:63
- Metering** 59:281
- Methanation** 68:63
- Methane**
- Bubbling-Bed-Reactor 66:193
 - Catalyst 57:273
 - Catalytic-Partial-Oxidation 66:193
 - Catalytically-Stabilized-Thermal-Burner 50:123
 - Chemo-Autotrophic-Biogas 58:71
 - Combustion 50:123
 - Copper(II) 57:273
 - Enrichment 58:71
 - Experimental-Study 66:193
 - γ -Alumina 57:273
 - Gas 66:193
 - Industrial 57:273
 - Intrinsic-Kinetics 57:273
 - Kinetics 58:71
 - Mechanism 58:71
 - Oxidation 57:273
 - Oxide 57:273
 - Purification 58:71
 - Support 57:273
 - Synthesis 66:193
- Methane-Hydrogen-Mixture** 46:129
- Methane-Production** 65:37
- Methanol**
- Alternative 45:33
 - Characteristics 54:63
 - Conversion 45:33
 - Elevated 54:63
 - Ethanol 54:63
 - Gas 54:63
 - Hydrocarbon 45:33
 - Kinetic-Model 45:33
 - Kinetics 58:101
 - Low-Pressure 58:101
 - Mass-Transfer 54:63
 - Modeling 45:33
 - Pressure 54:63
 - Synthesis 58:101
 - Temperature 54:63
 - Thermodynamics 58:101
- Methanol-Steam** 62:103
- Methanol-to-Gasoline-Process** 63:45
- Method**
- Calculation 55:125
 - Coke 55:125
 - Comparison 55:125
 - Deactivation 55:125
 - Fine 58:45
 - Inversion 58:45
 - Kinetics 55:125
 - Liquid-Liquid-Dispersion 58:45
 - Phase 58:45
 - Separation 58:45
- Methyl-Acetate** 66:227
- Methyl-tert-Butyl-Ether**
- Catafractionation 56:11
 - Catalytic-Bed-Reactor 44:97
 - Formation 44:97
 - Kinetic-Model 44:97
 - Sulfur-Promoted 67:199
 - Synthesis 67:199
 - Technology 56:11
 - Zirconium-Dioxide 67:199
- Methylcyclohexane**
- Catalyst 46:109
 - Deactivation 46:109
 - Dehydrogenation 46:109
 - Kinetics 67:123
 - Modeling 67:123
 - Pt-Sn/Al₂O₃ 46:109
 - Pyrolysis 67:123
- Methyldiethanolamine** 60:123
- Micellar-Catalyzed** 67:19
- Michaelis-Menten-Kinetics**
- Bioreactor 51:B63
 - Correlation 43:B43
 - Design 51:B63
 - Equation 51:B63
 - Experimental-Data 43:B43
 - Hollow-Fiber 51:B63
 - Linear-Type 43:B43
 - Mathematical-Model 43:B43
 - Product-Inhibition 43:B43
 - Ultrafiltration-Membrane-Reactor 43:B43
 - Zero-Order-Limit 51:B63
- Microalgae** 62:81
- Microbead** 65:71
- Microbial-Cell**
- Animal 62:121
 - Cavitation 55:B67
 - Cultivation 62:121
 - Disruption 55:B67
 - Hydrodynamic-Shear 62:121
 - Plant 62:121
 - Role 55:B67, 62:121
- Microbial-Film** 44:B87
- Microbial-Growth** 48:B9
- Microbial-System** 59:195
- Microcarrier**
- BHK 58:65
 - Cell-Culture 58:65
 - Continuous-Ethanol-Production 50:B17
 - Fluidized 50:B17
 - Glucose 50:B17
 - Immobilized 50:B17
 - Preparation 58:65
 - Saccharomyces-Cerevisiae 50:B17
 - Silicone-Based 58:65
- Microelectrical-Tomography** 56:143
- Microfiltration**
- Inorganic-Membrane 48:11
 - Intermittent-Operation 52:73
 - Model 48:11
 - Optimization 52:73
 - Process 52:73
 - Steady-State-Flux 48:11
- Micromixing**
- Biological-Growth-Process 51:B25
 - Chemical-Reactor 58:183
 - Comparison 45:25
 - Engulfment 45:25
 - Experimental-Study 47:155
 - Grid-Generated 47:155
 - Interaction-by-Exchange-with-the-Mean 45:25
 - Model 45:25
 - Order 51:B25
 - Segregation 51:B25
 - Stirred-Tank-Reactor 51:B25
 - Theoretical-Analysis 47:155
 - Turbulence 47:155
 - Turbulent 58:183
- Microporous-Filtration** 60:31
- Microporous-Membrane** 48:B1
- Microwave-Heating** 59:253
- Microwave-Radiation** 49:79
- Milled-Coal** 59:23
- Mineral-Process** 59:71
- Mini-Hydrocyclone** 65:21
- Mini-Tapered** 68:7
- Miscibility-to-Extraction-Temperature-Ratio** 60:169
- Mixed** 61:107
- Mixed-Convection** 50:33
- Mixed-Gas** 64:85
- Mixed-Oxide** 64:265
- Mixed-Pressure** 50:133
- Mixed-Solvent** 48:31
- Mixed-Solvent-Entrainer** 43:59
- Mixed-Specification** 44:89
- Mixed-Type** 57:B23
- Mixer**
- Calculation 47:141
 - Level 56:119
 - Liquid-Mixing 48:135
 - Mixing 52:13
 - Mixing-Time 48:135, 52:13
 - Motionless 47:141
 - Newtonian-Liquid 52:13
 - Non-Newtonian-Liquid 52:13
 - Performance 56:119
 - Positron-Camera 56:119
 - Powder 56:119
 - Power-Consumption 48:135, 52:13
 - Residence-Time 47:141
 - Ribbon 48:135, 52:13
 - Trajectory 47:141
- Mixer-Settler** 49:127
- Mixing**
- Attainable-Region 54:175
 - Batch 51:B57
 - Computational 59:39
 - Draft-Tube 59:273
 - External-Loop-Airlift-Reactor 66:97
 - Fermenter 51:B57
 - Fluid 59:39
 - Mixer 52:13
 - Mixing-Time 52:13
 - Multiple-Rate-Process 54:175
 - Newtonian-Liquid 52:13
 - Non-Newtonian-Liquid 52:13
 - Numerical-Simulation 63:117
 - Optimal-Structure 54:175
 - Power-Consumption 52:13
 - Progress 59:39
 - Reactor 54:175
 - Ribbon 52:13
 - Static-Mixer 63:117
 - Stirred-Vessel 59:39
 - Suspension 59:273
 - System 54:175
 - Tall-Vessel 59:273
 - Unstirred 51:B57
- Mixing-Property** 63:181
- Mixing-Rules** 61:213
- Mixing-Time**
- Chemical-Method 67:167
 - Comparison 67:167
 - Liquid-Mixing 48:135
 - Measurement 67:167
 - Mixer 48:135, 52:13
 - Mixing 52:13
 - Newtonian-Liquid 52:13
 - Non-Newtonian-Liquid 52:13
 - Physical-Method 67:167
 - Power-Consumption 48:135, 52:13
 - Ribbon 48:135, 52:13
- Mixture**
- Amberlite-252 66:137
 - Behavior 43:11
 - Calcium 66:171
 - Catalyst 43:11
 - Change 43:11
 - Coarse 67:37
 - Complex 52:B13
 - Deactivation 43:11
 - Dynamic-Transport 57:91
 - Emulsion 67:37
 - Enzymatic-Hydrolysis 52:B13
 - Enzyme 52:B13
 - Fine 67:37
 - Fly-Ash 66:171
 - Gas 56:67, 57:91
 - Generalization 56:67
 - Hydroxide 66:171
 - Ion-Exchange 66:137

- Low-Pressure 56:67
- Maximum 66:171
- Model 43:11
- Modeling 52:B13
- Multicomponent 57:91
- Pore-Size 43:11
- Porous-Solid 57:91
- Potassium 66:137
- Potato-Pulp 52:B13
- Reaction 43:11
- Removal 66:137, 66:171
- Simple 56:67
- Simulation 52:B13
- Single-Pellet 43:11
- Storage-Loss-Modulus 67:37
- Structural-Property 66:171
- Sulphur-Dioxide 66:171
- Support 43:11
- Supported-Catalyst 43:11
- Viscosity 56:67, 67:37
- Water-Methanol-Polyol 66:137
- Yield 66:171
- Mo-Catalyzed** 58:53
- Mobile** 58:285
- Mobile-Carrier** 57:253
- Model**
 - Absorption 66:123
 - Alginate 56:B9
 - Analysis 47:25, 65:55
 - Application 61:27, 63:79
 - Assessment 55:69
 - Behavior 43:11
 - Biofilter 65:55
 - Branching 64:77
 - Calcium 56:B9
 - Calcium-Sulfite 66:123
 - Calculating 56:27
 - Calculation 61:21, 61:27
 - Carbon 64:77
 - Catalyst 43:11
 - Change 43:11
 - Chemical-Reaction 57:115
 - Coal 57:295
 - Comparison 45:25, 61:21, 65:55
 - Comprehensive 57:295
 - Computation 57:295
 - Condensation 49:177
 - Control 50:159
 - Core-Annulus 68:51
 - Correct 66:149, 66:151
 - Correlated 64:7
 - Crystal-Growth-Rate-Function 55:69
 - Crystallization-Kinetics-Data 55:69
 - Cutting 56:27
 - Deactivation 43:11
 - Description 57:115
 - Determination 56:B9
 - Development 48:17, 56:101, 58:123, 65:27
 - Diffusion-Coefficient 56:B9
 - Diffusion-Limited 64:77
 - Dusty-Gas 57:115
 - Engulfment 45:25
 - Enzymatic-Transformation 65:27
 - Experiment 63:1
 - Experimental-Verification 58:123
 - Film 49:177, 52:19, 64:361
 - Fluid 52:19, 64:361
 - Fluidized-Bed 68:51
 - Gas-Liquid-Cocurrent-Downflow 51:19
 - Gas-Solid-Reaction 63:79, 68:1
 - Gasification 64:77
 - Geometrical 62:1
 - Glucose 56:B9
 - Half-Order 63:79
 - Heat 58:123
 - High 59:153
 - High-Pressure 61:27
 - Identification 56:B9
 - Inorganic-Membrane 48:11
 - Interaction-by-Exchange-with-the-Mean 45:25
 - Liquid-Solid-Circulating 68:51
 - Liquid-Solid-Mass-Transfer 63:1
 - Low-Reynolds-Number 59:153, 63:1
 - Malic-Acid 56:B9
 - Mass-Transfer 52:19, 58:123, 59:153, 64:361
 - Mass-Transport 57:115
 - Material 62:1
 - Mathematical-Description 66:149, 66:151
 - Membrane 56:B9
 - Membrane-Partitioned-Electrode-Reactor 47:25
 - Microfiltration 48:11
 - Micromixing 45:25
 - Mixture 43:11
 - Modeling 64:77
 - Molecular-Evaporator 49:177
 - Momentum 58:123
 - Moving-Boundary-Problem 63:79
 - Multicomponent 52:19, 64:361
 - Nonideal-Mixture 52:19, 64:361
 - Nonisothermal-Water-Gas-Shift-Reactor 48:17
 - Nucleation 68:1
 - Oil-Emulsion 56:27
 - Organic-Ultrafiltration-Membrane 56:27
 - Oxidase 65:27
 - Oxygen 66:123
 - Packed-Bed 51:19, 63:1
 - Packed-Column 66:149, 66:151
 - Particle 63:1
 - Permeability 64:7
 - pH 65:27
 - Polyphenol 65:27
 - Pore 64:77
 - Pore-Size 43:11
 - Porous-Medium 57:115, 62:1, 64:7
 - Prediction 50:159, 59:153, 61:21, 64:7
 - Pressure-Drop 51:19
 - Quantized-Solution 68:1
 - Radial-Flow 68:51
 - Random 62:1
 - Reaction 43:11, 63:79
 - Schmidt-Number 59:153
 - Set-Point-Weighting 50:159
 - Simplified 50:159
 - Simulation 48:17
 - Sinapine 65:27
 - Single-Pellet 43:11
 - Size-Dependent 55:69
 - Solid-Liquid-Mixing 56:101
 - Solution 66:123
 - Specific-Energy 57:295
 - Spray-Drying 58:123
 - Steady-State-Flux 48:11, 56:27
 - Structure 68:51
 - Support 43:11
 - Supported-Catalyst 43:11
 - System 55:69
 - Temperature 65:27
 - Temperature-Profile 49:177
 - Tomographic-Technique 56:101
 - Trametes-Versicolor 65:27
 - Turbulence 59:153
 - Turbulent 59:153
 - Two-Phase 62:1
 - Vapor-Liquid-Equilibrium 61:21, 61:27
 - Variously-Shaped 63:1
 - Verification 48:17
 - Volume 63:79
- Model| Binary-Friction→** 64:319
- Model| Circulation-Time→** 47:149
- Model| Extended-Linear→** 60:81
- Model| Flow-Reactor→** 60:105
- Model| Grain-Size-Distribution→** 53:25
- Model| Group-Unary-Wilson→** 48:183
- Model| Kinetic→**
 - Acetobacter-Aceti 54:B15
 - Alternative 45:33
 - Analysis 63:45
 - Catalytic-Bed-Reactor 44:97
 - Catalytic-Cracking 44:53
 - Conversion 45:33
 - Culture 54:B15
 - Experimental-Data 44:53, 65:99
 - Fluidized-Bed 44:53
 - Formation 44:97
 - Growth 54:B15
 - Heated 65:99
 - Hydrocarbon 45:33
 - Inactivation 65:99
 - Integral-Reactor 63:45
 - Interpretation 44:53
 - Methanol 45:33
 - Methanol-to-Gasoline-Process 63:45
 - Methyl-tert-Butyl-Ether 44:97
 - Modeling 45:33
 - Multistage-Reactor 44:53
 - Oil-Fraction 44:53
 - Single-Stage-Reactor 44:53
 - Strain 65:99
 - Strawberry-Product 65:99
 - Submerged 54:B15
 - Thermal 65:99
 - Yeast 65:99
- Model| Kinetic-Invariant→** 61:161
- Model| Mathematical→**
 - Affecting 61:13
 - Application 43:B19
 - Bioreactor 43:B19
 - Bromine 61:13
 - Correlation 43:B43
 - Design 43:B19
 - Dissolution 53:B25
 - Electrochemical-Reactor 61:13
 - Ethene 61:13
 - Experimental-Data 43:B43
 - Factor 61:13
 - Fermentation 60:189
 - Goethite 59:287
 - Hollow-Fiber-Biofilm-Reactor 56:B53
 - Inert-Support 60:189
 - Isotropic-Turbulence 43:B19
 - Kolmogorov-Theory 43:B19
 - Lactose 53:B25
 - Linear-Type 43:B43
 - Liqueur 59:287
 - Michaelis-Menten-Kinetics 43:B43
 - Mycelial-Fungi 60:189
 - Oxide 61:13
 - Oxyprecipitation 59:287
 - Pickling 59:287
 - Product-Inhibition 43:B43
 - Production 61:13
 - Relative-Concentration 61:13
 - Sieve-Plate 61:13
 - Solid-State 60:189
 - Steel 59:287
 - Synthesis 59:287

- Ultrafiltration-Membrane-Reactor 43:B43
- Model| Partial-Wetting->** 46:B59
- Model| Rigid-Drop->** 51:93
- Model| Semitheoretical->** 47:163
- Model| Simplified->** 56:19
- Model| Steady-State->** 43:121
- Model| Stochastic->** 59:205
- Model| Structured->** 44:B1
- Model| Two-Phase-Flow->** 50:69
- Modeling**
 - 1,2-Epoxyoctane 53:B13
 - A-Priori-Information 56:167
 - Acid 67:55
 - Active 53:13
 - Adsorbent 51:159
 - Adsorption 52:B71
 - Adsorption-Process 56:59
 - Air-Core 56:135
 - Airlift-Fluidized-Bed 49:89, 55:143, 55:145
 - Alcohol 48:B15
 - Alternative 45:33
 - Anaerobic-Stratified-Biofilm 65:37
 - ARMAX 50:B45
 - Aspergillus-Niger 52:B1
 - Automobile 53:47
 - Axial 44:B57
 - Backmixing-Effect 44:B57
 - Batch 48:B15, 52:B35, 61:157
 - Biological 44:B57
 - Bone-Powder 67:55
 - Branching 64:77
 - Calf-Rennet 56:B87
 - Carbon 64:77
 - Carbon-Monoxide 53:47
 - Carrier 63:127, 66:11
 - Catalyst 53:13
 - Catalytic-Afterburner 52:79
 - Catalytic-Converter 53:47
 - Cephalosporin-C 52:B71
 - Chemical-Reaction 58:223
 - Chemical-Vapor-Deposition 53:13
 - Chemical-Vapor-Deposition-Reactor 57:39
 - Chromatography 64:307
 - Comparison 56:59
 - Complex 52:B13
 - Complex-Selective-Medium 52:B35
 - Control 50:95, 59:71
 - Conversion 45:33
 - Corn 60:39
 - Corrected-Fick's-Law 61:123
 - Corrugated-Sheet 53:55
 - Countercurrent 56:59
 - Culture 61:35
 - Cyclic-Regime 43:B53
 - Cyclonic-Separator 56:135
 - Description 61:73
 - Design 49:89, 55:143, 55:145, 56:135
 - Diffusion-Limited 64:77
 - Dispersion 67:45
 - Distillation 57:177
 - Distribution 53:55
 - Drying 60:39
 - Dual-Limitation 48:B9
 - Economical-Optimization 64:307
 - Elaboration 67:55
 - Electrodialysis 57:163
 - Electroplating-Line 49:161
 - Electrostatic-Interaction 57:B15
 - Emulsion 63:127, 66:11
 - Enzymatic-Hydrolysis 52:B13
 - Enzyme 50:B45, 52:B13
 - Enzyme-Kinetics 56:B87
 - Equivalence 61:123
 - Estimation 61:35
 - Ethanol 48:B15
 - Evaporative-Loss 48:B15
 - Exhaust-Gas 53:47
 - Experimental 52:79
 - Experimental-Study 67:55
 - Experimentation 45:B67
 - Extraction 64:307
 - Facilitated 63:127, 66:11
 - Fed-Batch 61:35
 - Feed 54:17
 - Fermentation 48:B15, 50:B45, 52:B35
 - Fiber-Optic-Probe 61:179
 - Fixed-Bed 54:17, 61:123
 - Flotation-Bed 60:39
 - Flow 56:167
 - Fluidized 60:39, 64:307
 - Fluidized-Bed 61:73
 - Fluidized-Bed-Reactor 61:179
 - Free- β -Galactosidase 52:B1
 - Gas-Solid-Fluidized-Bed-Reactor 58:223
 - Gas-Flow 53:55, 58:223
 - Gasification 64:77
 - Gelatin-Production 67:55
 - Global 61:73
 - Glyceraldehyde-3-Phosphate-Dehydrogenase 52:B35
 - Growth-Kinetics 53:B13
 - Heterogeneity 51:159
 - Highly-Concentrated 54:17
 - Horizontal 57:39
 - Hot-Wall 57:39
 - Hydrocarbon 45:33
 - Hydrolysis 52:B1
 - Imaging 56:135, 56:167
 - Immobilized- β -Galactosidase 52:B1
 - Immobilized-Enzyme 57:B15
 - Implication 56:135
 - Inclined 56:167
 - Inhibitory-Effect 53:B13
 - Ion-Exchange 64:307
 - Ion-Exchange-Process 43:B53, 61:123
 - Isothermal-Oxidative-Stabilization 49:133
 - K-Na-Exchange 54:17
 - Kinetic-Model 45:33
 - Kinetics 57:B15, 60:39, 67:55, 67:123
 - L-Lysine-Production 61:35
 - Lactose 52:B1
 - Liquid 63:127, 66:11
 - Local 61:73
 - Loop-Reactor 44:B57
 - Low-Pressure 57:39
 - Mass-Transfer 49:89, 55:143, 55:145, 57:177, 67:45
 - Maxwell-Stefan-Description 57:163
 - Measurement 53:55
 - Membrane 63:127, 66:11
 - Mesophase-Pitch-Fiber 49:133
 - Methane-Production 65:37
 - Methanol 45:33
 - Methylcyclohexane 67:123
 - Microbial-Growth 48:B9
 - Mineral-Process 59:71
 - Mixture 52:B13
 - Model 64:77
 - Modified 52:B71
 - Monolithic 53:47
 - Multicomponent 57:177
 - Multiphase-Flow 56:167
 - Multiple-Steady-State 65:37
 - Multistage-Crystallizer 46:9
 - Nernst-Planck-Law 61:123
 - Neural-Network 61:35
 - Not-Fully-Developed-Flow 52:79
 - Online 61:35
 - Onopordum-Turcicum 56:B87
 - Operational 55:143
 - Operational-Parameter 49:89, 55:145
 - Optimization 43:B53, 49:89, 55:143, 55:145
 - Organic-Compound 67:45
 - Oscillatory-Feeding 53:47
 - Overall-Scheme 67:55
 - Oxygen 53:47
 - Packed-Bed 44:B57
 - Packing 53:55
 - Parameter 55:143
 - Performance 52:79, 53:47, 67:9
 - pH-Change 57:B15
 - Pharmaceutical-Lyophilization 45:B67
 - Phase 53:13
 - Pilot-Plant 45:B67
 - Polymer 50:95, 67:45
 - Pore 64:77
 - Potato-Pulp 52:B13
 - Powdered 56:B87
 - Prediction 65:37
 - Preparation 53:13
 - Process 67:55
 - Production 52:B35
 - Profile 53:13, 56:167
 - Pseudomonas-Oleovorans 53:B13
 - Pyrolysis 67:123
 - Reaction-Engineering 50:95
 - Reaction-Generated 57:B15
 - Recombinant-Escherichia-Coli 52:B35
 - Reconsideration 58:223
 - Recycle 44:B57
 - Resin 52:B71
 - Respect 55:143
 - Rinsing-Process 49:161
 - Separator 56:135
 - Simplified 64:307
 - Simulation 46:9, 52:B1, 52:B13, 56:59, 65:37
 - Solid-Liquid-Adsorption 51:159
 - State 61:35
 - State-Estimation 50:B45
 - Stirred-Tank 52:B71
 - Strategy 56:59
 - Structure 61:73
 - Structured 53:55
 - Sugar-Juice-Softening 43:B53
 - Technique 53:13
 - Thermal 57:39
 - Tomographic-Imaging 59:71
 - Tracer 61:179
 - Tubular 57:39
 - Turbulent 61:73, 61:179
 - Ultrafiltration 61:157
 - Variation 58:223
 - Velocity 56:167
 - Venturi-Scrubber 67:9
 - Volatile 67:45
 - Whey-Protein 64:307
- Modeling| Dynamic->**
 - Application 65:133
 - Biofilter 65:133
 - Denitrification 65:133
 - Generalized-Approach 65:133
 - Lemna-Gibba 57:B37
 - Plant 57:B37
 - Simulation 65:133
 - Waste-Water 65:133
 - Waste-Water-Treatment 57:B37
- Modeling| Kinetic->**
 - α -Pinene 50:115
 - Catalyst 58:7
 - Commercial 58:7
 - Cracking 58:7
 - Deactivation 58:7
 - Hydration 50:115

- Isobutanol 50:115
- Isopropylbenzene 58:7
- Phase-Equilibrium 50:115
- Silica-Alumina 58:7
- Terpene 50:115
- Water 50:115
- Modeling | Mathematical-**
- Bacterial 54:207
- Batch 54:207
- Butanol 46:B11
- Catalyst 60:131
- Cell 46:B11
- Continuous 54:207
- Continuous-Fermentation 46:B11
- Ethanol 54:221
- Experimental-Study 54:221
- Fermentation 54:221
- Fluidized-Bed-Reactor 60:131
- Immobilized 46:B11
- Integration 46:B11
- Kinetics 54:221
- Leaching 54:207
- Macroapproach 54:221
- Pervaporation 46:B11
- Saccharomyces-Cerevisiae 54:221
- Simulation 46:B11
- Unsteady-State 60:131
- Modeling | Microscopic-** 53:157
- Modeling | Rheological-** 64:99
- Modeling | Stochastic-** 66:207
- Modified**
- Adsorption 52:B71
- Cephalosporin-C 52:B71
- Glucose-Oxidase 65:71
- Immobilization 65:71
- Microbead 65:71
- Modeling 52:B71
- Monosize 65:71
- Resin 52:B71
- Stirred-Tank 52:B71
- Molar-Volume** 48:167
- Mole-Change** 57:101
- Molecular-Distillation** 56:39
- Molecular-Evaporator** 49:177
- Molecular-Sieve**
- Acidity 64:255
- Adsorption-Model 58:21
- Carbon 57:137
- Interpretation 57:137
- Langmuir-Kinetics 57:137
- Mass-Transfer 57:137
- Mesoporous 64:255
- Pore-Size 64:255
- Stability 64:255
- Two-Step 58:21
- Molecular-Structure** 52:31
- Molecule** 56:39
- Moment-Analysis** 65:81
- Momentum** 58:123
- Monoester** 60:63
- Monolithic** 53:47
- Monosize** 65:71
- Monosized** 44:133
- Monosized-Crystal** 50:87
- Monte-Carlo-Method** 45:75
- Monte-Carlo-Simulation** 46:B35
- Mordenite** 54:115
- Morpholine** 44:107
- Morphological-Property** 53:B35
- Morphology**
- Catalyst 64:69
- Design 64:69
- Fractal 64:69
- Immobilized-Catalase 55:B41
- Motionless** 47:141
- Motor** 67:65
- Movement** 51:135
- Moving-Bed** 59:133
- Moving-Boundary-Problem** 63:79
- Mucor-Miehei** 61:149
- Multi-Substrate** 65:165
- Multicomponent**
- Chemical-Vapor-Deposition-Reactor 57:127
- Diffusion 57:127
- Distillation 57:177
- Dynamic-Transport 57:91
- Efficiency 57:237
- Entrainment 57:237
- Falling-Film 49:119
- Film 52:19, 64:361
- Fluid 52:19, 64:361
- Fluid-System 57:189
- Gas 57:91
- Heat-Transfer 49:119
- Homogeneous 64:215
- Laminar 49:119
- Liquid 49:119
- Mass-Transfer 49:119, 52:19, 57:177, 64:361
- Mass-Transfer-Reaction-Coupling 57:189
- Mixture 57:91
- Model 52:19, 64:361
- Modeling 57:177
- Multiple-Wafer 57:127
- NMR 64:215
- Nonideal-Mixture 52:19, 64:361
- Phenomena 57:127
- Porous-Solid 57:91
- Reaction 49:119
- Simultaneous 49:119
- Solution 64:215
- Tray 57:237
- Two-Phase 57:189
- Vanadium-Oxide 64:215
- Multicomponent-Batch-Process** 51:83
- Multidimensional** 60:199
- Multienzyme-Reaction** 56:B61
- Multifractal** 64:107
- Multiphase-Flow** 56:167
- Multiphase-Reactor** 64:169
- Multiphase-Reactor** 46:B43
- Multiple-Rate-Process** 54:175
- Multiple-Steady-State** 65:37
- Multiple-Turbine** 63:53
- Multiple-Wafer** 57:127
- Multipurpose** 44:167
- Multistage-Crystallizer** 46:9
- Multistage-Reactor** 44:53
- Multivariable-Control**
- Anaerobic-Digestion 43:B81
- Analysis 43:B81
- Case-Study 44:119
- Dynamics 43:B81
- Main-Fractionator 44:119
- Slurry-Pumparound 44:119
- Must** 55:B29
- Mycelial-Fungi** 60:189
- Mycelial-System** 46:B83
- N,N-Dialkylhydrazine** 57:61
- Nanocrystalline** 64:225
- Naphthalene**
- Alkylation 53:173
- $\text{BF}_3\text{H}_3\text{PO}_4$ 53:173
- Borate 63:27
- Catalyst 53:173, 63:27
- Hydrogenation 63:27
- Platinum-Aluminum 63:27
- Propene 53:173
- Three-Phase-System 53:173
- Natural** 59:169
- Natural-Gas** 53:39
- Natural-Object** 64:1
- Nature** 58:53
- Near-Critical-Region** 67:27
- Necessary** 51:29
- Neodymium** 60:63
- Nernst-Planck-Law** 61:123
- Netherlands** 53:v
- Network-Analysis**
- Flow-Specification 50:133
- Fluid 50:133
- Large-Scale 50:133
- Mixed-Pressure 50:133
- Mixed-Specification 44:89
- Partitioning-Method 44:89
- Pipeline 44:89
- Neural-Network**
- Adaptive 63:65
- Analysis 68:41
- Application 62:207
- Batch-Process 63:65
- Control 63:65
- Crude-Oil 51:151
- Culture 61:35
- Development 63:65
- Dynamic-Control 68:41
- Estimation 51:151, 61:35
- Fed-Batch 61:35
- Flexible 63:65
- Fraction 51:151
- Kinematic-Viscosity 51:151
- L-Lysine-Production 61:35
- Lysine-Production 62:207
- Modeling 61:35
- Nonlinear-System 68:41
- Online 61:35
- Optimal-Structure 68:41
- Petroleum 51:151
- Stability 68:41
- State 61:35
- Neutral** 50:B39
- Newtonian-Fluid**
- Airlift-Column 62:35
- Bubble-Column-Reactor 50:1
- External-Loop 62:35
- Gas-Liquid-Mass-Transfer 62:35
- Gas-Hold-Up 50:1
- Non-Newtonian-Fluid 50:1, 62:35
- Prediction 50:1
- Newtonian-Liquid**
- Bubble-Growth 63:149
- Mixer 52:13
- Mixing 52:13
- Mixing-Time 52:13
- Non-Newtonian-Liquid 52:13, 63:149
- Power-Consumption 52:13
- Ribbon 52:13
- Viscous 63:149
- NH₃** 46:79
- Ni/Al₂O₃-Catalyst** 49:45
- Nickel**
- Adsorption 58:265
- Batch-Stirred-Reactor 58:265
- Copper(II) 58:265
- Cyclohexane 50:165
- Cyclohexene 50:165
- Dehydrogenation 50:165
- Platinum 50:165
- Rhizopus-Arrhizus 58:265
- Series-Analysis 58:265
- Supported-Catalyst 50:165
- Nickel-Alumina-Catalyst** 46:129
- Nitrate-Ion** 51:1
- Nitriding** 54:167
- Nitrification** 65:165
- Nitrobenzene** 49:B17
- Nitrogen-Oxide** 43:75
- Nitrous-Acid-Formation** 43:75
- Nitrous-Oxide** 43:25
- NMR** 64:215
- Non-Darcy** 50:33
- Non-Maintained** 67:83
- Non-Newtonian-Fluid**
- Airlift-Bioreactor 56:B101
- Airlift-Column 62:35
- Bubble-Column-Reactor 50:1
- Darcy 50:33
- External-Loop 62:35
- Forced-Convection 50:33
- Free-Convection 50:33

- Gas-Liquid-Circulation 56:B101
- Gas-Liquid-Mass-Transfer 62:35
- Gas-Hold-Up 50:1
- Heat-Transfer 50:33
- Inelastic-Fluid 50:33
- Mass-Transfer 56:B101
- Mixed-Convection 50:33
- Newtonian-Fluid 50:1, 62:35
- Non-Darcy 50:33
- Porous-Medium 50:33
- Prediction 50:1
- Saturated 50:33
- Unified-Similarity-Transformation 50:33
- Viscous 56:B101
- Non-Newtonian-Liquid**
 - Bend 45:165
 - Bubble-Growth 63:149
 - Flow 45:165
 - Fluidized-Bed 52:131
 - Mixer 52:13
 - Mixing 52:13
 - Mixing-Time 52:13
 - Newtonian-Liquid 52:13, 63:149
 - Power-Consumption 52:13
 - Ribbon 52:13
 - Solid-Liquid-Mass-Transfer 52:131
 - Viscous 63:149
- Non-Porous-Adsorbent** 65:175
- Non-Viscous-Effect** 59:111
- Nonaerated** 46:B83
- Noncatalytic** 53:25
- Nonferrous-Sulfide** 44:B31
- Nonideal-Mixture**
 - Film 52:19, 64:361
 - Fluid 52:19, 64:361
 - Mass-Transfer 52:19, 64:361
 - Model 52:19, 64:361
 - Multicomponent 52:19, 64:361
- Nonideal-Phenomena** 57:205
- Nonisothermal**
 - Enhancement 51:93
 - Factor 51:93
 - Immobilized-Enzyme-System 58:275
 - Instantaneous-Reaction 51:93
 - Mass-Transfer 51:93
 - Packed 58:275
 - Rigid-Drop-Model 51:93
 - Tubular-Reactor 58:275
- Nonisothermal-Reactor** 47:17
- Nonisothermal-Water-Gas-Shift-Reactor** 48:17
- Nonlinear** 64:21
- Nonlinear-Analysis** 48:173
- Nonlinear-Control** 61:139
- Nonlinear-Controller** 64:141
- Nonlinear-Kinetics** 49:B41
- Nonlinear-Oscillation** 59:169
- Nonlinear-Statistical-Technique** 67:181
- Nonlinear-System**
 - Analysis 68:41
 - Control 67:103
 - Dynamic-Control 68:41
 - Dynamics 67:103
 - Neural-Network 68:41
 - Optimal-Structure 68:41
 - Stability 68:41
 - Steady-State 67:103
 - Unstable 67:103
- Nonlinearity** 66:27
- Nonparametric-Method** 54:1
- Nonpolar-Liquid** 47:163
- Nonstandard** 58:135
- Nonstoichiometric** 64:225
- Nonuniform-Catalyst** 46:91
- Normal-Boiling-Point** 48:167
- Normal-Butyl-Acetate** 67:19
- Normal-Decane** 47:33
- Normal-Octane** 43:33
- Normal-Paraffin** 52:55
- Normalization** 59:177
- Not-Fully-Developed-Flow** 52:79
- Nuclear-Magnetic-Resonance** 56:149
- Nucleation** 68:1
- Nucleation-Kinetics** 58:209
- Numerical-Illustration** 68:11
- Numerical-Simulation** 63:117
- Numerical-Solution** 68:69
- Numerical-Study** 55:15
- Numerical-Technique** 45:133
- Observer-Based** 61:139
- Obstacle** 52:B49
- OH-Concentration** 53:39
- Oil**
 - Accelerated-Film-Technique 67:65
 - Biodegradation 56:B91
 - Carbon-Dioxide 61:227
 - Chain-of-Rotator 46:29
 - Comparison 61:227
 - Conventional 61:227
 - Equation-of-State 46:29
 - Equilibrium-Vaporization 46:29
 - Evaluation 56:B91
 - Extraction 61:227
 - Flow 67:65
 - Grape 61:227
 - Group-Contribution 46:29
 - Kinetic-Parameter 56:B91
 - Kinetics 56:B91
 - Liquid 61:227
 - Metal-Cutting 56:B91
 - Motor 67:65
 - Polymer-Thickened 67:65
 - Recovery 61:227
 - Seed 61:227
 - Solvent-Extraction 61:227
 - Stretching 67:65
 - Supercritical 61:227
 - Test 67:65
- Oil-Water-Emulsion**
 - Anomalous-Effect 63:195
 - Flow-Behavior 63:195
 - Flow-Characteristics 43:53
 - Flow-Measurement 63:59
 - Highly-Concentrated 43:53
 - Segmental-Orifice-Meter 63:59
 - Two-Phase 63:59
 - Wedge-Meter 63:59
- Oil-Agglomeration-Process** 57:9
- Oil-Emulsion** 56:27
- Oil-Extraction** 43:B103
- Oil-Fraction** 44:53
- Oligomerization** 54:115
- Online** 61:35
- Onopordum-Turcicum** 56:B87
- Onset** 57:261
- Operability** 44:81
- Operating-Condition**
 - Acetifier 62:183, 65:201
 - Batch 62:183
 - Closed-System 62:183, 65:201
 - Computer-Simulation 62:183, 65:201
 - Determination 63:19
 - End-Use 63:19
 - Industrial 62:183, 65:201
 - Operation 62:183
 - Optimization 63:19
 - Optimum 62:183, 65:201
 - Property 63:19
 - Semi-Continuous-Operation 65:201
 - Sequential-Method 63:19
 - Terpolymer 63:19
- Operating-Parameter** 57:9
- Operating-Temperature** 60:111
- Operation**
 - Acetifier 62:183
 - Batch 62:183
 - Characteristics 51:7
 - Closed-System 62:183
 - Computer-Simulation 62:183
 - Design 53:75
 - Deterministic-Chaos 53:75
 - Fluidized-Bed 53:75
 - Heat-Transfer-Rate 51:7
 - Industrial 62:183
 - Operating-Condition 62:183
 - Optimum 62:183
 - Tubular-Reactor 51:7
- Operation-Condition** 65:151
- Operational** 55:143
- Operational-Parameter**
 - Airlift-Fluidized-Bed 49:89, 55:145
 - Design 49:89, 55:145
 - Mass-Transfer 49:89, 55:145
 - Modeling 49:89, 55:145
 - Optimization 49:89, 55:145
- Operational-Range** 50:B1
- Opportunity** 52:B49
- Optimal-Control-Problem** 68:35
- Optimal-Geometry** 68:29
- Optimal-Structure**
 - Analysis 68:41
 - Attainable-Region 54:175
 - Dynamic-Control 68:41
 - Mixing 54:175
 - Multiple-Rate-Process 54:175
 - Neural-Network 68:41
 - Nonlinear-System 68:41
 - Reactor 54:175
 - Stability 68:41
 - System 54:175
- Optimization**
 - Airlift-Fluidized-Bed 49:89, 55:143, 55:145
 - Cascade 50:109
 - Choice 52:B59
 - Control 52:B59
 - Countercurrent-Flotation-Circuit 59:7
 - Cyclic-Regime 43:B53
 - Design 49:89, 55:143, 55:145
 - Determination 63:19
 - Discontinuous-Microfiltration-Backwash 57:247
 - End-Use 63:19
 - Fed-Batch 52:B59
 - Fed-Batch-Culture 65:219
 - Fermentation 52:B59
 - Fungal 65:219
 - Intermittent-Operation 52:73
 - Ion-Exchange-Process 43:B53
 - Mass-Transfer 49:89, 55:143, 55:145
 - Microfiltration 52:73
 - Modeling 43:B53, 49:89, 55:143, 55:145
 - Operating-Condition 63:19
 - Operational 55:143
 - Operational-Parameter 49:89, 55:145
 - Parameter 55:143
 - Performance 50:109
 - Polygalacturonase 65:219
 - Process 52:73, 57:247
 - Property 63:19
 - Respect 55:143
 - Saccharomyces Cerevisiae 65:219
 - Sequential-Method 63:19
 - Sugar-Juice-Softening 43:B53
 - Synthesis 65:219
 - Tank-Electrolyzer 50:109
 - Terpolymer 63:19
 - Variable 52:B59
- Optimum**
 - Acetifier 62:183, 65:201
 - Batch 62:183

- Closed-System 62:183, 65:201
- Computer-Simulation 62:183, 65:201
- Industrial 62:183, 65:201
- Operating-Condition 62:183
- Operating-Conditions 65:201
- Operation 62:183
- Semi-Continuous-Operation 65:201
- Optimum-Design** 62:143
- Optimum-Sequence** 46:97
- Option** 45:99
- Order** 51:B25
- Organic-Acid** 50:47
- Organic-Compound**
 - Dispersion 67:45
 - Higher-Molecular-Weight 67:191
 - Mass-Transfer 67:45
 - Modeling 67:45
 - Pervaporation 67:191
 - Polymer 67:45
 - Separation 67:191
 - Volatile 67:45
- Organic-Electrolyte** 66:111
- Organic-Liquid**
 - Group-Contribution-Method 50:9
 - Prediction 50:9, 59:181
 - Simple-Method 59:181
 - Surface-Tension 59:181
 - Viscosity 50:9
- Organic-Loading** 56:B23
- Organic-Loading-Rate** 52:B21
- Organic-Solution** 62:231
- Organic-Ultrafiltration-Membrane** 56:27
- Orifice**
 - Accumulation-Effect 59:281
 - Aqueous-Solution 49:65
 - Bubble-Formation 49:65
 - Closely-Spaced 49:65
 - Experimental-Investigation 59:281
 - Gas 59:281
 - Liquid 59:281
 - Metering 59:281
 - Two-Phase-Flow 59:281
- Oscillating-Grid** 63:105
- Oscillatory** 57:219
- Oscillatory-Feeding** 53:47
- Oscillatory-Reaction** 66:27
- Oscillatory-Reaction-System** 44:129
- Outlet**
 - Boundary-Condition 57:299, 57:303
 - Slurry-Bubble-Column 57:299, 57:303
 - Solid 57:299, 57:303
- Overall-Kinetics** 43:33
- Overall-Processing** 60:169
- Overall-Scheme** 67:55
- Overall-Volumetric-Transfer-Coefficient** 68:29
- Oxidase** 65:27
- Oxidation**
 - Activity 52:115
 - Alkaline 49:B17
 - Carbon-Monoxide 64:283
 - Catalysis 43:33, 64:283
 - Catalyst 52:115, 57:273, 64:295
 - Characterization 52:115
 - Cobalt 52:115
 - Cobalt-Salt 43:33
 - Copper(II) 57:273
 - Copper-Cerium-Dioxide 64:283
 - Fluorite 64:283
 - γ -Alumina 57:273
 - Hydrocarbon 52:115
 - Industrial 57:273
 - Intrinsic-Kinetics 57:273
 - Kinetics 49:B17, 67:115
 - Lignin 49:B17
 - Liquid-Phase 43:33
 - Metal-Oxide 64:295
 - Methane 57:273
 - Nitrobenzene 49:B17
 - Normal-Octane 43:33
 - Overall-Kinetics 43:33
 - Oxide 52:115, 57:273, 64:283
 - Phenol 67:115
 - Product-Distribution 43:33
 - Rice-Straw 49:B17
 - Soot 64:295
 - Steady-State-Model 43:121
 - Sulphur-Dioxide 43:121
 - Support 57:273
 - Total 52:115
 - Transition-Metal-Promoted 64:283
 - Trickle-Bed-Reactor 43:121
 - Wet-Air 67:115
- Oxide**
 - Activity 52:115
 - Affecting 61:13
 - Bromine 61:13
 - Carbon-Monoxide 64:283
 - Catalysis 64:283
 - Catalyst 52:115, 57:273, 64:203
 - Characterization 52:115
 - Cobalt 52:115
 - Copper(II) 57:273
 - Copper-Cerium-Dioxide 64:283
 - Electrochemical-Reactor 61:13
 - Ethene 61:13
 - Factor 61:13
 - Fluorite 64:283
 - γ -Alumina 57:273
 - Hydrocarbon 52:115
 - Industrial 57:273
 - Intrinsic-Kinetics 57:273
 - Mathematical-Model 61:13
 - Methane 57:273
 - Oxidation 52:115, 57:273, 64:283
 - Preparation 64:203
 - Production 61:13
 - Recent-Advances 64:203
 - Relative-Concentration 61:13
 - Sieve-Plate 61:13
 - Support 57:273, 64:203
 - Total 52:115
 - Transition-Metal-Promoted 64:283
- Oxygen**
 - Absorption 66:123
 - Automobile 53:47
 - Calcium-Sulfite 66:123
 - Carbon-Monoxide 53:47
 - Catalytic-Converter 53:47
 - Cocurrent-Upflow-Bioreactor 62:237
 - Dynamic-Liquid-Hold-Up 62:237
 - Exhaust-Gas 53:47
 - Low-Reynolds-Number 62:237
 - Mass-Transfer 62:237
 - Model 66:123
 - Modeling 53:47
 - Monolithic 53:47
 - Oscillatory-Feeding 53:47
 - Performance 53:47
 - Small-Packing 62:237
 - Solution 66:123
- Oxygen-Transfer**
 - Airlift-Tube-Reactor 68:29
 - α -Amylase 44:B51
 - Bioprocess 65:109
 - Bioreactor 56:B15
 - Cell 56:B15
 - Effect 56:B15
 - Fermentation 44:B51
 - Growth 65:109
 - High-Temperature 44:B51
 - L-Alanine-Production 65:109
 - Optimal-Geometry 68:29
 - Overall-Volumetric-Transfer-Coefficient 68:29
 - Parameter 65:109
 - Particle 56:B15
 - Physical-Presence 56:B15
 - Pseudomonas-Dacunhae 65:109
 - Rheology 44:B51
 - Solid 56:B15
 - Starch-Suspension 44:B51
- Oxyprecipitation** 59:287
- Packed**
 - Ammonia-Removal 66:65
 - Anaerobically-Treated 66:65
 - Axial-Dispersion 52:63
 - Column 66:65
 - Different 52:63
 - Distillation-Column 57:219
 - Ether-Production 57:219
 - Fixed-Bed 52:63
 - Fuel 57:219
 - Homoionic-Zeolite 66:65
 - Immobilized-Enzyme-System 58:275
 - Ion-Exchange 66:65
 - Liquid-Flow 52:63
 - Metallic-Foam 52:63
 - Nonisothermal 58:275
 - Oscillatory 57:219
 - Piggery-Manure 66:65
 - Reactive 57:219
 - Reticulated 52:63
 - Structure 52:63
 - Transport-Phenomena 57:219
 - Tubular-Reactor 58:275
 - Vapor-Liquid 57:219
- Packed-Bed**
 - Adsorption 65:81
 - Axial-Data 65:81
 - Axial 44:B57
 - Axial-Dispersion 58:245
 - Backmixing-Effect 44:B57
 - Biofilm-Reactor 65:165
 - Biological 44:B57
 - Calcium-Alginate 65:81
 - Carbon-Oxidation 65:165
 - Column 65:81
 - Copper 65:81
 - Distributor 48:49
 - Dynamic-Approach 65:81
 - Energy 45:123
 - Evaluation 65:81
 - Experiment 63:1
 - Feed-Concentration 65:165
 - Fiber 58:245
 - Flow 59:111
 - Forced-Flow 45:123
 - Gas-Liquid-Cocurrent-Downflow 51:19
 - Gas-Liquid-Controlling 62:61
 - Immobilized 65:81
 - Liquid 48:61
 - Liquid-Solid-Mass-Transfer 62:61, 63:1
 - Liquid-Distribution 48:49
 - Long-Cylindrical-Particle 45:123
 - Loop-Reactor 44:B57
 - Low-Reynolds-Number 63:1
 - Mass-Transfer 45:123
 - Model 51:19, 63:1
 - Modeling 44:B57
 - Moment-Analysis 65:81
 - Multi-Substrate 65:165
 - Nitrification 65:165
 - Non-Viscous-Effect 59:111
 - Particle 63:1
 - Pressure-Drop 51:19
 - Radial-Spreading 48:61
 - Raschig-Ring 62:61

- Rational-Description 48:49, 48:61
- Recycle 44:B57
- Sinusoidal-Perturbations 65:165
- Sphere 59:111
- Stimulus-Response 65:81
- Technique 65:81
- Trickle-Flow 48:49, 48:61
- Two-Phase-Flow 62:61
- Upflow 65:165
- Variously-Shaped 63:1
- Xanthan-Gum-Solution 59:111
- Zoogloea-Ramigera 65:81
- Packed-Bubble-Column** 43:95
- Packed-Column**
 - Cocurrent 63:93
 - Correct 66:149, 66:151
 - Determination 57:67
 - Gas-Absorption 57:67
 - Hydrodynamics 63:93
 - Influence 47:51
 - Liquid-Phase 47:51
 - Mass-Transfer 63:93
 - Mass-Transfer-Coefficient 57:67
 - Mass-Transfer-Resistance 47:51
 - Mathematical-Description 66:149, 66:151
 - Model 66:149, 66:151
 - Physical-System 57:67
 - Technique 57:67
 - Theoretical-Study 63:93
 - Viscosity 47:51
- Packing**
 - Characteristics 58:251
 - Corrugated-Sheet 53:55
 - Distribution 53:55
 - Gas-Flow 53:55, 61:95
 - Liquid 61:95
 - Liquid-Side 58:251
 - Low-Pressure-Drop 45:79
 - Mass-Transfer 58:251
 - Measurement 53:55
 - Modeling 53:55
 - Pattern 61:95
 - Performance 45:79
 - Random 61:95
 - Structured 53:55, 58:251
- Palliate** 51:167
- Palm-Fruit** 66:223
- Pancreas** 44:B81
- Parallel** 59:161
- Parallel-Channel-Spacer** 44:73
- Parallel-Chemical-Reactions** 58:161
- Parallel-Plate** 66:1
- Parallel-Reaction** 51:167
- Parameter**
 - Aerated 59:187
 - Airlift-Fluidized-Bed 55:143
 - Bioprocess 65:109
 - Bioreactor 59:187
 - Bubble 59:187
 - Correlation-Constant 60:97
 - Design 55:143
 - Determination 59:187
 - Entrainment 59:187
 - Growth 65:109
 - L-Alanine-Production 65:109
 - Mass-Transfer 55:143, 59:187
 - Modeling 55:143
 - Operational 55:143
 - Optimization 55:143
 - Oxygen-Transfer 65:109
 - Pseudomonas-Dacunhae 65:109
 - Respect 55:143
 - Salt-Effect 60:97
 - Surface 59:187
 - Tie-Line 60:97
- Parametric-Sensitivity** 46:23
- Parametric-Study**
 - Concentration-Dependent 43:1
 - Deactivation 43:1, 51:167
 - Fixed-Bed-Catalytic-Reactor 43:1
 - Isothermal 43:1
 - Palliate 51:167
 - Parallel-Reaction 51:167
 - Series-Parallel-Reaction 51:167
 - Temperature 51:167
 - Time-Sequence 51:167
- Partially-Scaled-Fractal** 64:1
- Particle**
 - 1-Propanol 51:129
 - Adsorbent 53:147
 - Adsorption 66:223
 - Adsorption-Kinetics 53:147
 - Alkoxide 55:93
 - Analogy 61:113
 - Application 62:193
 - Aqueous-Solution 66:223
 - Basic-Dye 66:223
 - Biochemical 62:193
 - Bioreactor 56:B15
 - Bunch 66:223
 - Catalyst 53:1, 61:113
 - Cell 56:B15
 - Controlled 51:129, 55:93
 - Convection 61:113
 - Cross-Flow 61:171
 - Cylinder 61:113
 - Design 53:1
 - Determination 54:1
 - Development 68:7
 - Different 66:223
 - Diffusion 53:1, 61:113
 - Effect 56:B15
 - Experiment 63:1
 - Factor 53:1
 - Filtration 61:171
 - Fine 51:129, 55:93
 - Flow 62:193
 - Fluidization 68:7
 - Fluidized-Bed 51:135, 68:7
 - Flux 61:171
 - Geometry 61:113
 - Gravimetric-Determination 53:147
 - High-Temperature-Range 55:93
 - Hydrodynamical 62:193
 - Hydrolysis 51:129, 55:93
 - Influence 53:147
 - Interaction 62:193
 - Intraparticle 53:1
 - Liquid 51:135, 62:193
 - Liquid-Solid-Mass-Transfer 63:1
 - Liquid-Chromatography 61:191
 - Low-Reynolds-Number 63:1
 - Mini-Tapered 68:7
 - Model 63:1
 - Movement 51:135
 - Nonparametric-Method 54:1
 - Oxygen-Transfer 56:B15
 - Packed-Bed 63:1
 - Palm-Fruit 66:223
 - Permeability 61:191
 - Permeation 61:171
 - Physical-Presence 56:B15
 - Porous 61:191
 - Protein 61:191
 - Reaction 61:113
 - Reaction-Kinetics 53:1
 - Removal 66:223
 - Separation 61:191
 - Settling 54:1
 - Slab 61:113
 - Slurry-Bubble-Column 54:1
 - Solid 51:135, 56:B15
 - Spherical 51:129, 55:93
 - Stability 68:7
 - Steady-State 61:171
 - Synthesis 51:129, 55:93
 - System 68:7
 - Tetrabutoxide 51:129
 - Thermogravimetric-Analyzer 68:7
 - Transfer 53:147
 - Variously-Shaped 63:1
 - Velocity 54:1
 - Zirconia 51:129, 55:93
 - Zirconium 51:129, 55:93
- Particle-Dispersion** 66:207
- Particle-Laden**
 - Coaxial 63:11
 - Jet 63:11
 - Particle-Dispersion 66:207
 - Round-Jet 66:207
 - Stochastic-Modeling 66:207
 - Turbulent 66:207
 - Two-Phase 63:11
 - Velocity-Measurement 63:11
- Particle-Size**
 - Calcined-Limestone 47:11
 - Distribution 60:89
 - Fluidized 60:89
 - Gas 60:89
 - HCl-Gas 47:11
 - High-Pressure 60:89
 - Reaction 47:11
 - Segregation 60:89
 - Solid 60:89
 - Wide 60:89
- Particle-Turbulence** 66:201
- Partitioning-Behavior** 59:297
- Partitioning-Method** 44:89
- Patel-Teja-Equation** 67:27
- Pattern**
 - Downcomer 63:167
 - Effectiveness-Factor 59:309
 - Efficiency 63:167
 - Gas-Flow 61:95
 - Immobilized-Cell-Aggregate 59:309
 - Layout 63:167
 - Liquid 61:95
 - Packing 61:95
 - Product-Inhibition 59:309
 - Random 61:95
 - Tray 63:167
- Pattern-Recognition-Approach** 68:35
- Pellet** 59:177
- Penicillin-G**
 - Amberlite 58:285, 62:231
 - Carrier 58:285
 - Cell 58:285
 - Constant-Interface-Area 58:285
 - Distribution 62:231
 - Equilibrium 62:231
 - Extraction 50:B39, 58:285
 - Kinetics 58:285
 - Mobile 58:285
 - Neutral 50:B39
 - Organic-Solution 62:231
 - Phosphorus-Ester 50:B39
 - Water 62:231
- Pentaerythritol**
 - Crystal-Growth-Kinetics 58:215
 - Nucleation-Kinetics 58:209
- Peptide** 65:257
- Peptide-Coupled** 62:169
- Percolation**
 - Electrochemical-Reactor 53:137
 - Fractal 64:21
 - Heterogeneous-Medium 64:21
 - Kinetics 53:137
 - Linear 64:21
 - Nonlinear 64:21
 - Poly-(18-Dibenzo-6-Crown) 53:137
 - Porous-Electrode 53:137
 - Pulsed 53:137

- Scalar 64:21
- Scaling-Law 64:21
- Synthesis 53:137
- Transport-Process 64:21
- Vector 64:21
- Performance**
- Anaerobic 55:B55
- Automobile 53:47
- Batch 65:195
- Bioreactor 55:B35, 57:B1
- Carbon-Monoxide 53:47
- Cascade 50:109
- Catalytic-Afterburner 52:79
- Catalytic-Converter 53:47
- Cell 59:1
- Chemical-Reactor 59:169
- Column 59:1
- Comparison 55:B55, 65:195
- Control 55:B55
- Design 57:B1
- Diffusional-Characteristics 55:B35
- Digester 55:B55
- Dynamics 55:B55
- Enzymatic-Hydrolysis 65:195
- Equipped 57:B1
- Exhaust-Gas 53:47
- Experimental 52:79
- Flotation 59:1
- Gas-Transfer 57:B1
- Gel 55:B35
- High-Rate 57:B1
- Large-Scale 59:1
- Level 56:119
- Low-Pressure-Drop 45:79
- Mesophilic 55:B55
- Mixer 56:119
- Modeling 52:79, 53:47, 67:9
- Monolithic 53:47
- Natural 59:169
- Nonlinear-Oscillation 59:169
- Not-Fully-Developed-Flow 52:79
- Optimization 50:109
- Oscillatory-Feeding 53:47
- Oxygen 53:47
- Packing 45:79
- Pilot-Plant-Data 59:1
- Positron-Camera 56:119
- Powder 56:119
- Prediction 59:1
- Protein 65:195
- Sludge 55:B55
- Stirred-Reactor 65:195
- Swelling 55:B35
- Tank-Electrolyzer 50:109
- Thermophilic 55:B55
- Torus-Reactor 65:195
- Venturi-Injector 57:B1
- Venturi-Scrubber 67:9
- Wheat 65:195
- Periodic-Dosing** 47:83
- Permeability**
- Adsorption 62:73
- Change 62:73
- Charge 62:73
- Correlated 64:7
- Dialysis 62:73
- Ion 62:73
- Liquid-Chromatography 61:191
- Membrane 62:73
- Model 64:7
- Particle 61:191
- Porous 61:191
- Porous-Medium 64:7
- Prediction 64:7
- Protein 61:191, 62:73
- Separation 61:191
- Permeation**
- Application 57:145
- Bubble-Size 67:71
- Cross-Flow 61:171
- Filtration 61:171
- Flux 61:171, 67:71
- Frequency 67:71
- Gas 67:71
- Generalized-Maxwell-Stefan-Equation 57:145
- Light-Hydrocarbon 57:145
- Membrane 57:145, 67:71
- Particle 61:171
- Separation 57:145
- Silicalite-1 57:145
- Sparged 67:71
- Steady-State 61:171
- Tubular 67:71
- Ultrafiltration 67:71
- Permselectivity** 51:1
- Perturbation** 43:B1
- Pervaporation**
- Butanol 46:B1, 46:B11
- Cell 46:B11
- Continuous-Fermentation 46:B1, 46:B11
- Experimental-Result 46:B1
- Higher-Molecular-Weight 67:191
- Immobilized 46:B11
- Immobilized-Cell 46:B1
- Integration 46:B1, 46:B11
- Mathematical-Modeling 46:B11
- Organic-Compound 67:191
- Separation 67:191
- Simulation 46:B11
- Petroleum**
- Crude-Oil 45:83, 51:151
- Estimation 45:83, 51:151
- Fraction 45:83, 51:151
- Kinematic-Viscosity 51:151
- Neural-Network 51:151
- Simple-Method 45:83
- Viscosity 45:83
- pH**
- Aqueous 67:97
- Development 65:27
- Dispersion 67:97
- Enzymatic-Transformation 65:27
- Influence 67:97
- Model 65:27
- Oxidase 65:27
- Polyphenol 65:27
- Rheology 67:97
- Sinapine 65:27
- Stability 67:97
- Temperature 65:27, 67:97
- Titanium-Dioxide 67:97
- Trametes-Versicolor 65:27
- pH-Change** 57:B15
- pH-Elution** 65:175
- Pharmaceutical-Lyophilization** 45:B67
- Phase**
- Active 53:13
- Catalyst 53:13
- Characteristics 43:67
- Chemical-Equilibrium 54:187
- Chemical-Vapor-Deposition 53:13
- Convex-Hull 54:187
- Fine 58:45
- Fluidized-Bed 43:67
- Gibbs'-Free-Energy 54:187
- Hold-Up 43:67
- Inversion 58:45
- Liquid-Liquid-Dispersion 58:45
- Method 58:45
- Modeling 53:13
- Prediction 54:187
- Preparation 53:13
- Profile 53:13
- Separation 58:45
- Technique 53:13
- Three-Phase 43:67
- Phase-Equilibrium** 50:115
- Phase-Hold-Up** 58:259
- Phase-Transfer** 62:97
- Phenol**
- Aerobic-Mixed-Culture 53:B47
- Constant-Biomass-Hold-Up 45:B35
- Continuous-Stirred-Reactor 53:B47
- Continuous-Stirred-Tank-Bioreactor 62:67
- Degrading 45:B35, 62:67
- Development 45:B35
- Fluidized-Bed-Bioreactor 45:B35
- Growth 53:B47
- Kinetics 67:115
- Oxidation 67:115
- Range 62:67
- Stability 62:67
- Steady-State-Behavior 53:B47
- Wet-Air 67:115
- Phenomena** 57:127
- Phosphonic-Acid** 60:63
- Phosphorus-Containing-Compound** 51:41
- Phosphorus-Ester** 50:B39
- Physical-Method** 67:167
- Physical-Presence** 56:B15
- Physical-System** 57:67
- Pickling** 59:287
- Piggery-Manure** 66:65
- Pilot-Plant** 45:B67
- Pilot-Plant-Data** 59:1
- Pinene** | α - 50:115
- Pipe** 45:43
- Pipeline** 44:89
- Pplant**
- Animal 62:121
- Cultivation 62:121
- Dynamic-Modeling 57:B37
- Hydrodynamic-Shear 62:121
- Lemna-Gibba 57:B37
- Microbial-Cell 62:121
- Recycle 61:1
- Robust-Control 61:1
- Role 62:121
- System-Design 61:1
- Waste-Water-Treatment 57:B37
- Plasma-Enhanced** 58:1
- Plasma-Separation** 48:B1
- Platinum** 50:165
- Platinum-Aluminum** 63:27
- Plug-Flow-Reactor** 60:111
- Plunging** 44:157
- Pneumatically-Pulsed** 45:111
- Poisoning** 49:45
- Poland** 58:vii
- Polar-Substance** 55:139
- Policy** 51:83
- Pollutant** 54:B41
- Poly-(18-Dibenzo-6-Crown)** 53:137
- Polyacrylamide-Gel** 45:B5
- Polyarylate** 47:63
- Polycarbonate** 47:63
- Polyclonal-Antibody**
- Antigen-Coupled 54:B33
- Characterization 54:B33
- Homogeneous 54:B33, 62:169
- Immunoassay 54:B33, 62:169
- Liposome 54:B33, 62:169
- Peptide-Coupled 62:169
- Protein 62:169
- Polyethylene-Glycol-Maltodextrin-System** 46:B75
- Polygalacturonase** 65:219
- Polyhydroxyalcohol** 60:123
- Polymer**
- Control 50:95
- Dispersion 67:45
- Mass-Transfer 67:45
- Modeling 50:95, 67:45

- Organic-Compound 67:45
- Polyethylene-Glycol-Malto-dextrin-System 46:B75
- Protein-Extraction 46:B75
- Reaction-Engineering 50:95
- Spray-Column 46:B75
- Two-Phase-System 46:B75
- Volatile 67:45
- Polymer-Thickened** 67:65
- Polymerization-Reaction** 64:141
- Polyphenol** 65:27
- Population-Dynamics** 65:213
- Population-Selection** 45:B57
- Pore** 64:77
- Pore-Size**
 - Acidity 64:255
 - Behavior 43:11
 - Catalyst 43:11
 - Change 43:11
 - Deactivation 43:11
 - Mesoporous 64:255
 - Mixture 43:11
 - Model 43:11
 - Molecular-Sieve 64:255
 - Reaction 43:11
 - Single-Pellet 43:11
 - Stability 64:255
 - Support 43:11
 - Supported-Catalyst 43:11
- Porous**
 - Catalyst 57:101
 - Coal 58:53
 - Forced-Convection 57:101
 - Hydrogenation 58:53
 - Influence 58:53
 - Kinetics 58:53
 - Liquid-Chromatography 61:191
 - Mo-Catalyzed 58:53
 - Mole-Change 57:101
 - Nature 58:53
 - Particle 61:191
 - Permeability 61:191
 - Protein 61:191
 - Reaction 57:101
 - Separation 61:191
- Porous-Electrode** 53:137
- Porous-Medium**
 - Chemical-Reaction 57:115
 - Correlated 64:7
 - Darcy 50:33
 - Description 57:115
 - Dusty-Gas 57:115
 - Forced-Convection 50:33
 - Free-Convection 50:33
 - Geometrical 62:1
 - Heat-Transfer 50:33
 - Inelastic-Fluid 50:33
 - Mass-Transport 57:115
 - Material 62:1
 - Mixed-Convection 50:33
 - Model 57:115, 62:1, 64:7
 - Non-Darcy 50:33
 - Non-Newtonian-Fluid 50:33
 - Permeability 64:7
 - Prediction 64:7
 - Random 62:1
 - Saturated 50:33
 - Two-Phase 62:1
 - Unified-Similarity-Transformation 50:33
- Porous-Solid** 57:91
- Position** 60:155
- Positron-Camera** 56:119
- Potassium** 66:137
- Potassium-Carbonate** 46:1
- Potassium-Chloride** 50:47
- Potassium-Sulfate**
 - Ammonia 67:1
 - Catalysis 67:1
 - Double-Salt 52:89
 - Glaserite 67:1
 - Gypsum 67:1
 - Magnesium-Chloride-Rich 52:89
 - Magnesium-Sulfate 52:89
 - Production 67:1
 - Seawater 52:89
 - Solution 52:89
 - Sylvinit 67:1
- Potato-Pulp** 52:B13
- Potential** 57:B31
- Powder**
 - Bubble-Column 47:91
 - Heat-Transfer 47:91
 - Hydrodynamic-Investigation 47:91
 - Level 56:119
 - Mixer 56:119
 - Performance 56:119
 - Positron-Camera 56:119
 - Small-Particle 47:91
 - Viscous-Liquid 47:91
- Powdered** 56:B87
- Power**
 - Heterogeneous-Reaction 50:27
 - Input 51:29
 - Necessary 51:29
 - Scale-Up 51:29
 - Stirred-Vessel 51:29
 - Suspension 51:29
 - Ultrasound-Emitter 50:27
- Power-Consumption**
 - Agitator 52:9
 - Dual-Turbine 67:215
 - Helical 52:9
 - Helical-Ribbon-Impeller-Mixer 67:215
 - Highly-Viscous-Fluid 52:9
 - Liquid-Mixing 48:135
 - Mixer 48:135, 52:13
 - Mixing 52:13
 - Mixing-Time 48:135, 52:13
 - Newtonian-Liquid 52:13
 - Non-Newtonian-Liquid 52:13
 - Pseudoplastic-Fluid 52:9
 - Ribbon 48:135, 52:9, 52:13
 - Screw 52:9
 - Ungassed-Condition 67:215
- Power-Law**
 - Arbitrary 56:33
 - Bioreactor 55:B73
 - Catalytic-Wall-Reaction 62:51
 - Convective-Diffusion 62:51
 - Cross-Section 56:33
 - Cylindrical-Duct 56:33
 - Design 55:B73
 - Duct 62:51
 - Equation 55:B73
 - Flow 56:33
 - Fluid 55:B73, 56:33, 62:51
 - Generalized-Reynolds-Number 56:33
 - Hollow-Fiber 55:B73
 - Homogeneous 62:51
 - Inside 62:51
 - Single 62:51
- Practical-Approach** 64:179
- Prediction**
 - Acetate-Ion 51:1
 - Anaerobic-Stratified-Biofilm 65:37
 - Approximate-Method 59:293
 - Aqueous-Solution 51:1
 - Bubble-Column-Reactor 50:1
 - Calculation 61:21
 - Cell 59:1
 - Chemical-Equilibrium 54:187
 - Column 59:1
 - Comparison 61:21
 - Control 50:159
 - Convex-Hull 54:187
 - Correlated 64:7
 - Electrodialysis 51:1
 - Equation-of-State 52:93
 - Extended-Thomas-Method 44:173
 - Fast-Reaction 59:293
 - Flotation 59:1
 - Fluorinated-Hydrocarbon 44:173
 - Gas-Liquid-Flow 45:55
 - Gas-Hold-Up 50:1
 - Gibbs'-Free-Energy 54:187
 - Group-Contribution-Method 50:9
 - High 59:153
 - Hold-Up 43:49, 45:55
 - Inclined 45:55
 - Large-Scale 59:1
 - Liquid 44:173, 51:41
 - Low-Reynolds-Number 59:153
 - Mass-Transfer 59:153
 - Methane-Production 65:37
 - Model 50:159, 59:153, 61:21, 64:7
 - Modeling 65:37
 - Molar-Volume 48:167
 - Multiple-Steady-State 65:37
 - Newtonian-Fluid 50:1
 - Nitrate-Ion 51:1
 - Non-Newtonian-Fluid 50:1
 - Normal-Boiling-Point 48:167
 - Organic-Liquid 50:9, 59:181
 - Performance 59:1
 - Permeability 64:7
 - Permselectivity 51:1
 - Phase 54:187
 - Phosphorus-Containing-Compound 51:41
 - Pilot-Plant-Data 59:1
 - Porous-Medium 64:7
 - Product-Distribution 59:293
 - Pure-Component-Property 52:93
 - Schmidt-Number 59:153
 - Set-Point-Weighting 50:159
 - Simple-Method 59:181
 - Simplified 50:159
 - Simulation 65:37
 - Solid-Fluid-Flow 43:49
 - Souder-Method 51:41
 - Stirred-Tank-Reactor 59:293
 - Subcritical-Mixture 55:115
 - Subcritical-Range 52:93
 - Surface-Tension 59:181
 - Turbulence 59:153
 - Turbulent 59:153
 - Two-Phase 45:55
 - Vapor-Liquid-Equilibrium 55:115, 61:21
 - Viscosity 44:173, 50:9, 51:41
- Preparation**
 - Active 53:13
 - Alkylhydrazine 62:97
 - BHK 58:65
 - Catalyst 53:13, 64:203
 - Catalytic-Property 64:247
 - Cell-Culture 58:65
 - Chemical-Vapor-Deposition 53:13
 - Heteropolyacid 64:247
 - Microcarrier 58:65
 - Modeling 53:13
 - Ni/Al₂O₃-Catalyst 49:45
 - Oxide 64:203
 - Phase 53:13
 - Phase-Transfer 62:97
 - Poisoning 49:45
 - Profile 53:13
 - Recent-Advances 64:203
 - Salt 64:247
 - Silicone-Based 58:65
 - Support 64:203
 - Supported 64:247
 - Technique 53:13
 - Thiophene 49:45
- Presence**
 - Active-Carbon 44:43
 - Catalytic-Reaction 49:79
 - Distribution 67:83
 - Eddy 67:83

- Gas 44:43
- H₂O 46:79
- H₂S 46:79
- Hydrodenitrogenation 46:79
- Influence 67:83
- Integral-Flow-Reactor 46:79
- Kinetics 46:79
- Liquid 67:83
- Liquid–Solid-Flow 67:83
- Microwave-Radiation 49:79
- NH₃ 46:79
- Non-Maintained 67:83
- Quinoline 46:79
- Solid 67:83
- Staying-Time 67:83
- Thermal-Conductivity-Measurement 44:43
- Pressure**
- Carbon-Dioxide 52:B29
- Characteristics 54:63
- Elevated 54:63
- Ethanol 54:63
- Gas 54:63
- Inactivation 52:B29
- Leuconostoc-Dextranicum 52:B29
- Mass-Transfer 54:63
- Methanol 54:63
- Temperature 54:63
- Pressure-Driven** 58:175
- Pressure-Drop**
- Air-Non-Newtonian-Liquid-Flow 59:277
- Air–Water-Pipe-Flow 48:197
- Atmospheric-Condition 48:197
- Bubble-Column-Reactor 48:153
- Conical 51:53
- Design 61:203
- Dry 61:203
- Flow-Pattern 48:197
- Gas–Liquid-Cocurrent-Downflow 51:19
- Hold-Up 48:197
- Horizontal 48:197
- Importance 61:203
- Model 51:19
- Packed-Bed 51:19
- Spouted-Bed 51:53
- Static-Mixer 59:277
- Surface-Tension 48:197
- Transport-Phenomena 48:153
- Two-Phase 59:277
- Venturi-Scrubber 61:203
- Pressure-Fluctuation** 64:149
- Pressure-Measurement** 47:113
- Pressure-Swing** 48:173
- Primary-Amine** 55:53
- Process**
- 2-Propyl-Pentane-Nitrile 59:121
- 4-Cyanopyridine 56:B49
- 4-Picoline 56:B49
- Acid 67:55
- Aerosol 64:239
- Alginate-Bead 55:B29
- Application 56:109, 56:127
- Autoinductive 61:139
- Bone-Powder 67:55
- Characterization 64:239
- Condition 56:B49
- Connectionist-System 54:125
- Continuous-Fluidized-Bed 55:B29
- Copper-Modified 64:239
- Deacidification 55:B29
- Decomposition 64:239
- Discontinuous-Microfiltration-Backwash 57:247
- Elaboration 67:55
- Electrical-Tomography 56:127
- Emission-Tomography 56:109
- Engineering 56:127
- Entrapped 55:B29
- Environmental 56:159
- Experimental-Study 67:55
- Fed-Batch 61:139
- Fermentation 61:139
- Gelatin-Production 67:55
- Grape 55:B29
- High-Temperature 64:239
- High-Yield 56:B49
- Higher-Alcohol 64:239
- Inconsistent-Data 54:125
- Intermittent-Operation 52:73
- Kinetics 67:55
- Microfiltration 52:73
- Modeling 67:55
- Must 55:B29
- Nonlinear-Control 61:139
- Observer-Based 61:139
- Optimization 52:73, 57:247
- Overall-Scheme 67:55
- Reconcile 54:125
- Schizosaccharomyces 55:B29
- Synthesis 59:121, 64:239
- Technique 56:127
- Tomography 56:vii, 56:159
- Ultrasonic-Irradiation 59:121
- United-States 56:159
- Zinc-Chromite 64:239
- Process-Integration** 61:53
- Process-Monitoring** 67:181
- Process-Optimization** 53:B1
- Process-Parameter** 43:B1
- Processing** 54:B25
- Product-Distribution**
- Approximate-Method 59:293
- Catalysis 43:33
- Cobalt-Salt 43:33
- Fast-Parallel-Reactions 58:15
- Fast-Reaction 59:293
- Influence 58:15
- Liquid-Phase 43:33
- Normal-Octane 43:33
- Overall-Kinetics 43:33
- Oxidation 43:33
- Prediction 59:293
- Stirred-Tank-Reactor 59:293
- Viscosity 58:15
- Product-Inhibition**
- Correlation 43:B43
- Effectiveness-Factor 59:309
- Experimental-Data 43:B43
- Immobilized-Cell-Aggregate 59:309
- Linear-Type 43:B43
- Mathematical-Model 43:B43
- Michaelis–Menten-Kinetics 43:B43
- Pattern 59:309
- Ultrafiltration-Membrane-Reactor 43:B43
- Production**
- Affecting 61:13
- Ammonia 67:1
- Batch 52:B35
- Block 61:233
- Bromine 61:13
- Carrier 61:233
- Catalysis 67:1
- Complex-Selective-Medium 52:B35
- Continuous-Flow-Stirred-Tank-Reactor 62:143
- Electrochemical-Reactor 61:13
- Ethanol 61:233
- Ethene 61:13
- Factor 61:13
- Fermentation 52:B35
- Fructose 61:233
- Glaserite 67:1
- Glyceraldehyde-3-Phosphate-Dehydrogenase 52:B35
- Growth 62:143
- Gypsum 67:1
- Mathematical-Model 61:13
- Modeling 52:B35
- Optimum-Design 62:143
- Oxide 61:13
- Potassium-Sulfate 67:1
- Recombinant-Escherichia-Coli 52:B35, 62:143
- Relative-Concentration 61:13
- Saccharomyces-Cerevisiae 61:233
- Sieve-Plate 61:13
- Stage 62:143
- Sylvinit 67:1
- Tryptophan-Synthetase-Subunit 62:143
- Two-Stage 62:143
- Wood 61:233
- Profile**
- A-Priori-Information 56:167
- Active 53:13
- Catalyst 53:13
- Chemical-Vapor-Deposition 53:13
- Elution 65:209
- Flow 56:167
- Glucose–Fructose-Mixtures 65:209
- Imaging 56:167
- Inclined 56:167
- Modeling 53:13, 56:167
- Multiphase-Flow 56:167
- Phase 53:13
- Preparation 53:13
- Separation 65:209
- Technique 53:13
- Velocity 56:167
- Progress** 59:39
- Promoter** 43:107
- Propene**
- Adsorption 54:115
- Alkylation 53:173
- BF₃H₃PO₄ 53:173
- Catalyst 53:173
- Cracking 54:115
- Deactivation 54:115
- Diffusion 54:115
- Hexane 54:115
- Mordenite 54:115
- Naphthalene 53:173
- Oligomerization 54:115
- Three-Phase-System 53:173
- Zeolite 54:115
- Property**
- Bacillus-Macerans-314 61:247
- β-Cyclodextrin 61:247
- Biosynthesis 61:247
- Crude-Enzyme 61:247
- Cyclodextrin 61:247
- Determination 63:19
- End-Use 63:19
- Glucosyltransferase 61:247
- Operating-Condition 63:19
- Optimization 63:19
- Sequential-Method 63:19
- Terpolymer 63:19
- Protein**
- Adsorption 62:73
- Aphron 65:1
- Aqueous-Phase 59:297
- Back-Extraction 59:297
- Batch 65:187, 65:195
- Change 62:73
- Characterization 65:1
- Charge 62:73
- Chromatographic-Behavior 49:B29
- Colloidal 65:1
- Comparison 65:195
- Competing-Reaction 61:41
- Cost 61:41
- Denaturation 49:B29
- Dialysis 62:73
- Displacement 49:B29
- Enrichment 59:297
- Enzymatic-Hydrolysis 65:187, 65:195

- Enzymatic-Kinetics 65:187
- Gas 65:1
- Homogeneous 62:169
- Hydrolysis 65:187
- Immunoassay 62:169
- Influence 61:41
- Ion 62:73
- Liposome 62:169
- Liquid-Chromatography 61:191
- Membrane 62:73
- Particle 61:191
- Partitioning-Behavior 59:297
- Peptide-Coupled 62:169
- Performance 65:195
- Permeability 61:191, 62:73
- Polyclonal-Antibody 62:169
- Porous 61:191
- Recovery 65:1
- Refolding 61:41
- Reversed-Micelle 59:297
- Separation 61:191
- Stirred-Reactor 65:187, 65:195
- Strategy 61:41
- Subsequent 65:1
- Torus-Reactor 65:195
- Wheat 65:187, 65:195
- Protein-Adsorption** 48:B1
- Protein-Extraction** 46:B75
- Protein-Mixture** 55:B19
- Protein-Product** 58:197
- Proteolysis** 65:87
- Pseudoadiabatic-Operation** 58:33
- Pseudomonas-Dacunhae** 65:109
- Pseudomonas-Oleovorans** 53:B13
- Pseudoplastic-Fluid** 52:9
- Pt-Sn/Al₂O₃** 46:109
- Pulsatile** 52:107
- Pulsed** 53:137
- Pulsed-Baffled-Reactor** 63:157
- Pumping-Characteristics** 66:73
- Pure-Component-Property** 52:93
- Pure-Compound** 59:101
- Pure-Gase** 57:285
- Pure-Liquid** 48:211
- Pure-Substance** 59:127
- Purification**
 - Aliquat-336 59:303
 - Anaerobic 54:B25
 - Bacillus-Subtilis 59:303
 - Batch 51:B43
 - Biosynthesis 51:B43
 - Chemo-Autotrophic-Biogas 58:71
 - Concentration 59:303
 - Concomitant-Product 46:B53
 - Continuous-Chromatography 51:B43
 - Cosolvent 59:303
 - Dextran 51:B43
 - Dextranucrase 51:B43
 - Dry-Moldy-Bran 46:B53
 - Enrichment 58:71
 - Enzyme 59:303
 - Fluidized-Bed-System 54:B25
 - Fruit 54:B25
 - Gibberellic-Acid 46:B53
 - Kinetics 54:B25, 58:71
 - Large-Scale 51:B43
 - Leuconostoc-Mesenteriodes 51:B43
 - Mechanism 58:71
 - Methane 58:71
 - Processing 54:B25
 - Reversed-Micelle 59:303
 - Separation 59:303
 - Solid-State-Fermentation 46:B53
 - Supercritical-Fluid-Extraction 46:B53
 - Waste-Water 54:B25
- PVC** 55:87
- Pyrolysis**
 - High-Conversion 55:87
 - Kinetics 55:87, 67:123
 - Methylcyclohexane 67:123
 - Modeling 67:123
 - PVC 55:87
 - Waste 55:87
- Quantized-Solution** 68:1
- Quaternization** 53:107
- Quinary-System** 49:167
- Quinoline** 46:79
- Rackett-Equation** 49:27
- Radial-Flow** 68:51
- Radial-Profile** 53:115
- Radial-Spreading** 48:61
- Radiative** 45:75
- Random**
 - Gas-Flow 61:95
 - Geometrical 62:1
 - Liquid 61:95
 - Material 62:1
 - Model 62:1
 - Packing 61:95
 - Pattern 61:95
 - Porous-Medium 62:1
 - Two-Phase 62:1
- Range** 62:67
- Raschig-Process** 57:61
- Raschig-Ring** 62:61
- Rate**
 - Absorption 59:243
 - Capacity 59:243
 - Carbon-Monoxide 59:243
 - Cosorb-Solution 59:243
 - Energy-Balance-Approach 63:105
 - Energy-Dissipation 63:105
 - Gas-Sparging 47:187
 - Mass-Transfer 47:187
 - Measurement 63:105
 - Oscillating-Grid 63:105
 - Single-Sphere 47:187
- Rate-Equation** 44:B87
- Rate-Function** 53:125
- Rate-Parameter** 48:71
- Rational-Description**
 - Distributor 48:49
 - Liquid 48:61
 - Liquid-Distribution 48:49
 - Packed-Bed 48:49, 48:61
 - Radial-Spreading 48:61
 - Trickle-Flow 48:49, 48:61
- Reaction**
 - Analogy 61:113
 - Anthraquinone 63:37
 - Application 63:79
 - Behavior 43:11
 - Calcined 47:1
 - Calcined-Limestone 47:11
 - Carbon-Dioxide 44:107
 - Catalyst 43:11, 57:101, 61:113
 - Change 43:11
 - Convection 61:113
 - Cylinder 61:113
 - Deactivation 43:11
 - Determination 47:1
 - Diffusion 61:113
 - Diglycolamine 44:107
 - Falling-Film 49:119
 - Forced-Convection 57:101
 - Gas 47:1
 - Gas-Solid-Reaction 63:79
 - Geometry 61:113
 - Half-Order 63:79
 - HCl-Gas 47:11
 - Heat-Transfer 49:119
 - Hydrogen-Chloride 47:1
 - Kinetic-Parameter 47:1
 - Kinetics 44:107
 - Laminar 49:119
 - Limestone 47:1
 - Liquid 49:119
 - Mass-Transfer 49:119
 - Mixture 43:11
 - Model 43:11, 63:79
 - Mole-Change 57:101
 - Morpholine 44:107
 - Moving-Boundary-Problem 63:79
 - Multicomponent 49:119
 - Particle 61:113
 - Particle-Size 47:11
 - Pore-Size 43:11
 - Porous 57:101
 - Simultaneous 49:119
 - Single-Pellet 43:11
 - Slab 61:113
 - Sodium 63:37
 - Sulfide 63:37
 - Support 43:11
 - Supported-Catalyst 43:11
 - Thermogravimetry 47:1
 - Volume 63:79
- Reaction-Distillation-Column** 66:227
- Reaction-Engineering** 50:95
- Reaction-Generated** 57:B15
- Reaction-Kinetics**
 - Alcoholic-Solution 55:53
 - Catalyst 53:1
 - Controlled-Hydrolysis 44:133
 - Design 53:1
 - Diffusion 53:1
 - Ethanol 44:133
 - Factor 53:1
 - Formation 44:133
 - Intraparticle 53:1
 - Monosized 44:133
 - Particle 53:1
 - Primary-Amine 55:53
 - Secondary-Amine 55:53
 - Silica-Sphere 44:133
 - Size-Control 44:133
 - Tetraethyl-Orthosilicate 44:133
- Reaction-Rate**
 - Chlorine-Dioxide 60:101
 - Diffusivity 61:7
 - Evaluation 61:7
 - Hydrogen-Peroxide 60:101
 - Inversion 61:7
 - Ion-Exchange 61:7
 - Solution 61:7
 - Sucrose 61:7
- Reactive**
 - Amine 65:47
 - Boundary-Value-Problem 57:27
 - Distillation-Column 57:219
 - Equilibrium 65:47
 - Ether-Production 57:219
 - Extractant 65:47
 - Extraction 65:47
 - Fuel 57:219
 - Gas-Absorption 57:27
 - Lactic-Acid 65:47
 - Oscillatory 57:219
 - Packed 57:219
 - Transport-Phenomena 57:219
 - Vapor-Liquid 57:219
- Reactive-Distillation-Process** 66:181
- Reactive-Intermediate-Species** 66:231
- Reaction**
 - Attainable-Region 54:175
 - Continuous-Transport 53:B1
 - Design 53:B1
 - Immobilized-Enzyme 53:B1
 - Mixing 54:175
 - Multiple-Rate-Process 54:175
 - Optimal-Structure 54:175
 - Process-Optimization 53:B1
 - Strategy 53:B1
 - System 54:175

- Reactor-Hydrodynamics** 56:B23
- Reactor-Wall** 45:9
- Real-Time** 56:95
- Recent-Advances** 64:203
- Reciprocating-Plate-Column** 54:7
- Recombinant-Cultures** 65:213
- Recombinant-Escherichia-Coli**
- Batch 52:B35
 - Complex-Selective-Medium 52:B35
 - Continuous-Flow-Stirred-Tank-Reactor 62:143
 - Fermentation 52:B35
 - Glyceraldehyde-3-Phosphate-Dehydrogenase 52:B35
 - Growth 62:143
 - Modeling 52:B35
 - Optimum-Design 62:143
 - Production 52:B35, 62:143
 - Stage 62:143
 - Tryptophan-Synthetase-Subunit 62:143
 - Two-Stage 62:143
- Reconcile** 54:125
- Reconsideration** 58:223
- Recovery**
- Aphron 65:1
 - Carbon-Dioxide 61:227
 - Characterization 65:1
 - Colloidal 65:1
 - Comparison 61:227
 - Conventional 61:227
 - Extraction 61:227
 - Gas 65:1
 - Grape 61:227
 - Liquid 61:227
 - Oil 61:227
 - Protein 65:1
 - Seed 61:227
 - Solvent-Extraction 61:227
 - Subsequent 65:1
 - Supercritical 61:227
- Recycle**
- Axial 44:B57
 - Backmixing-Effect 44:B57
 - Biological 44:B57
 - Loop-Reactor 44:B57
 - Modeling 44:B57
 - Packed-Bed 44:B57
 - Plant 61:1
 - Robust-Control 61:1
 - System-Design 61:1
- Recycle-System** 65:151
- Redox-Potential** 49:73
- Reducing-Agent** 49:73
- Reduction** 56:B43
- Refining-Power** 60:169
- Refolding** 61:41
- Reforming**
- Aging 66:51
 - Autothermal-Reactor-System 62:103
 - Catalyst 66:51
 - Hydrogen-Production 62:103
 - Methanol-Steam 62:103
 - Simulation 62:103
 - Steam 66:51
- Refrigeration-System** 45:99
- Regenerated** 63:189
- Regeneration** 54:35
- Regime** 58:33
- Relationship**
- 1-Butene 64:265
 - Acid 64:265
 - Al₂O₃ 64:265
 - Bronsted-Type 64:265
 - Catalyst 64:265
 - Downcomer 57:B7
 - Gas-Liquid-Separator 57:B7
 - Gas-Hold-Up 57:B7
 - Internal-Loop-Airlift-Reactor 57:B7
 - Isomerization 64:265
 - Mixed-Oxide 64:265
 - Riser 57:B7
 - Silicon-Dioxide 64:265
 - Site 64:265
 - Solid 64:265
 - Surface-Active 64:265
 - Titanium-Dioxide 64:265
 - Zirconium-Dioxide 64:265
- Relative-Concentration** 61:13
- Removal**
- Activated 52:37
 - Adsorption 66:223
 - Amberlite-252 66:137
 - Aqueous-Solution 52:37, 66:223
 - Basic-Dye 66:223
 - Bunch 66:223
 - Calcium 66:171
 - Carbon 52:37
 - Different 66:223
 - Fly-Ash 66:171
 - Hydroxide 66:171
 - Ion-Exchange 66:137
 - Lemna-Gibba 54:B41
 - Maximum 66:171
 - Mixture 66:137, 66:171
 - Palm-Fruit 66:223
 - Particle 66:223
 - Pollutant 54:B41
 - Potassium 66:137
 - Structural-Property 66:171
 - Sulphur-Dioxide 66:171
 - Tannic-Acid 52:37
 - Water 54:B41
 - Water-Methanol-Polyol 66:137
 - Yield 66:171
- Residence-Time**
- Calculation 47:141
 - Distribution 59:259
 - Equipped 56:51
 - Evaporator 56:51
 - Liquid 56:51
 - Liquid-Film 59:259
 - Mixer 47:141
 - Motionless 47:141
 - Spiral-Element 56:51
 - Thin-Layer 56:51
 - Trajectory 47:141
 - Wiped 59:259
- Residence-Time-Distribution**
- Continuous-Couette-Flow-Device 48:101
 - Fluid 45:43
 - Laminar-Flow 45:43
 - Pipe 45:43
- Residual** 47:B35
- Residual-Function-Method** 59:101
- Residue-Curve-Map** 66:181
- Resin** 52:B71
- Resistance** 43:41
- Respect** 55:143
- Reticulated** 52:63
- Reverse-Phase-Column** 49:B41
- Reversed-Displacement-Chromatography** 46:B93
- Reversed-Micellar-Extraction** 46:B69
- Reversed-Micelle**
- Aliquat-336 59:303
 - Aqueous-Phase 59:297
 - Bacillus-Subtilis 59:303
 - Back-Extraction 59:297
 - Concentration 59:303
 - Cosolvent 59:303
 - Enrichment 59:297
 - Enzyme 59:303
 - Partitioning-Behavior 59:297
 - Protein 59:297
 - Purification 59:303
 - Separation 59:303
- Revitalization** 54:155
- Reynolds-Number**
- Generalized-> 56:33
- Rheological-Property** 53:B35
- Rheology**
- α -Amylase 44:B51
 - Aqueous 67:97
 - Creosote-Based 45:B13
 - Dispersion 67:97
 - Emulsion 45:B13
 - Fermentation 44:B51
 - High-Temperature 44:B51
 - Influence 67:97
 - Oxygen-Transfer 44:B51
 - pH 67:97
 - Stability 67:97
 - Starch-Suspension 44:B51
 - Temperature 67:97
 - Titanium-Dioxide 67:97
 - Wood-Preservative 45:B13
- Rhizopus-Arrhizus** 58:265
- Ribbon**
- Agitator 52:9
 - Helical 52:9
 - Highly-Viscous-Fluid 52:9
 - Liquid-Mixing 48:135
 - Mixer 48:135, 52:13
 - Mixing 52:13
 - Mixing-Time 48:135, 52:13
 - Newtonian-Liquid 52:13
 - Non-Newtonian-Liquid 52:13
 - Power-Consumption 48:135, 52:9, 52:13
 - Pseudoplastic-Fluid 52:9
 - Screw 52:9
- Rice-Straw** 49:B17
- Rinsing-Process** 49:161
- Riser** 57:B7
- Rising-Bubble** 64:191
- Robust-Control** 61:1
- Role**
- Ag(I)/Ag(II) 56:1
 - Animal 62:121
 - Anodic-Oxidation 56:1
 - Biotechnology 50:B9
 - Cavitation 55:B67
 - Chemical-Engineering 50:B9
 - Chemical-Reaction 57:205
 - Cultivation 62:121
 - Disruption 55:B67
 - Hydrodynamic-Shear 62:121
 - Interfacial 57:205
 - Mass-Transfer 57:205
 - Mediator 56:1
 - Microbial-Cell 55:B67, 62:121
 - Nonideal-Phenomena 57:205
 - Plant 62:121
 - Toluene 56:1
- Rotary** 58:145
- Rotating-Disk** 65:227
- Rotating-Mixer** 62:23
- Round-Jet** 66:207
- Rule-of-Thumb** 46:97
- Rushton-Turbine** | Modified-> 61:83
- Saccharification** 45:B27
- Saccharomyces Cerevisiae**
- Optimization 65:219
 - Synthesis 65:219
- Saccharomyces-Cerevisiae**
- Batch-Culture 44:B69
 - Block 61:233
 - Carrier 61:233
 - Continuous-Ethanol-Production 50:B17
 - Ethanol 44:B69, 54:221, 61:233
 - Experimental-Study 54:221
 - Fermentation 54:221
 - Fluidized 50:B17
 - Fructose 61:233
 - Glucose 50:B17
 - High-Concentration 44:B69
 - Immobilized 50:B17
 - Kinetics 54:221

- Low-Frequency 65:145
- Macroapproach 54:221
- Mathematical-Modeling 54:221
- Microcarrier 50:B17
- Modified-Ghose-Model 44:B69
- Production 61:233
- Suspension 65:145
- Temperature 65:145
- Thermo-Ultrasonication 65:145
- Ultrasonic-Power 65:145
- Wood 61:233
- Salt** 64:247
- Salt-Polyethylene-Glycol-System** 46:B31
- Salt-Effect** 60:97
- Saturated** 50:33
- Scalar** 64:21
- Scale-Up**
 - Correlation 63:157
 - Input 51:29
 - Mass-Transfer-Coefficient 63:157
 - Necessary 51:29
 - Power 51:29
 - Pulsed-Baffled-Reactor 63:157
 - Stirred-Vessel 51:29
 - Suspension 51:29
- Scaling-Law** 64:21
- Scheduling** 44:167
- Schizosaccharomyces** 55:B29
- Schmidt-Number** 59:153
- Screw** 52:9
- Screw-Agitator** 66:73
- Seawater** 52:89
- Secondary-Amine** 55:53
- Section**
 - Boundary-Layer-Separation 49:55
 - Conical 62:113
 - Cylindrical 49:55
 - Diffuser 49:55
 - Gas-Liquid-Flow 49:55
 - Geometry 62:113
 - Hydrodynamics 62:113
 - Influence 62:113
 - Shallow 62:113
 - Spouted-Bed 62:113
 - Venturi-Scrubber 49:55
- Seed** 61:227
- Seeding** 59:143
- Segmental-Orifice-Meter** 63:59
- Segregation**
 - Biological-Growth-Process 51:B25
 - Distribution 60:89
 - Fluidized 60:89
 - Gas 60:89
 - High-Pressure 60:89
 - Micromixing 51:B25
 - Order 51:B25
 - Particle-Size 60:89
 - Solid 60:89
 - Stirred-Tank-Reactor 51:B25
 - Wide 60:89
- Selection** 49:73
- Selectivity**
 - Activity 46:61
 - Behavior 46:91
 - Carbon-Dioxide 68:63
 - Carbon-Monoxide 68:63
 - Consecutive-Reaction 46:91
 - Difference 68:63
 - Heavy-Oil-Processing 46:61
 - Methanation 68:63
 - Miscibility-to-Extraction-Temperature-Ratio 60:169
 - Nonuniform-Catalyst 46:91
 - Overall-Processing 60:169
 - Refining-Power 60:169
 - Solvent-Extraction 60:169
 - Solvent-Index 60:169
 - Stable-Catalyst 46:61
- Self-Aspirating** 58:59
- Self-Inhibitory-Substrate** 47:B11
- Semi-Continuous-Operation** 65:201
- Semicontinuous-Multi-Tank-Culture** 65:123
- Semicontinuous-Operation** 56:B109
- Semiempirical-Equation-of-State** 48:111
- Semisynthetic-Waste-Water** 52:B21
- Sensitivity-Coefficient** 44:129
- Separation**
 - Adsorption 48:173, 49:B41
 - Aliquat-336 59:303
 - Application 57:145
 - Bacillus-Subtilis 59:303
 - Bioreaction 50:B23
 - Blowdown-Policy 48:173
 - Chromatography 50:B23
 - Concentration 59:303
 - Continuous-Annular-Chromatography 55:B19
 - Continuous-System 50:B23
 - Cosolvent 59:303
 - Dipeptide 49:B41
 - Effect 49:B41
 - Elution 55:B19, 65:209
 - Enzyme 59:303
 - Equilibrium 48:173
 - Fine 58:45
 - Functional-Transformation-Method 51:63
 - Generalized-Maxwell-Stefan-Equation 57:145
 - Glucose-Fructose-Mixtures 65:209
 - Higher-Molecular-Weight 67:191
 - Inversion 58:45
 - Light-Hydrocarbon 57:145
 - Liquid-Liquid-Dispersion 58:45
 - Liquid-Chromatography 61:191
 - Membrane 57:145
 - Method 58:45
 - Nonlinear-Analysis 48:173
 - Nonlinear-Kinetics 49:B41
 - Organic-Compound 67:191
 - Particle 61:191
 - Permeability 61:191
 - Permeation 57:145
 - Pervaporation 67:191
 - Phase 58:45
 - Porous 61:191
 - Pressure-Swing 48:173
 - Profile 65:209
 - Protein 61:191
 - Protein-Mixture 55:B19
 - Purification 59:303
 - Reverse-Phase-Column 49:B41
 - Reversed-Micelle 59:303
 - Silicalite-1 57:145
 - Steady-State 51:63
- Separator** 56:135
- Sequence** 45:149
- Sequential-Method** 63:19
- Series-Analysis** 58:265
- Series-Parallel-Reaction** 51:167
- Set-Point-Weighting** 50:159
- Setting** 47:119
- Settling** 54:1
- Shallow**
 - Conical 62:113
 - Cylindrical-Geometry 64:353
 - Dead-Zone 64:353
 - Geometry 62:113
 - Hydrodynamics 62:113
 - Influence 62:113
 - Section 62:113
 - Spout-Diameter 64:353
 - Spouted-Bed 62:113, 64:353
- Shape** 59:177
- Shear-Stress** 62:155
- Short-Time** 62:43
- Shrinking** 55:135
- Sieve-Plate**
 - Affecting 61:13
 - Bromine 61:13
 - Coefficient 55:B1
 - Column 55:B1
 - Electrochemical-Reactor 61:13
 - Enzyme 55:B1
 - Ethene 61:13
 - Extraction 55:B1
 - Factor 61:13
 - Mass-Transfer 55:B1
 - Mathematical-Model 61:13
 - Oxide 61:13
 - Production 61:13
 - Relative-Concentration 61:13
- Silica-Alumina**
 - 1-Butene 60:147
 - Adsorption-Enthalpy 60:147
 - Catalyst 58:7, 60:147
 - Commercial 58:7
 - Cracking 58:7
 - Deactivation 58:7
 - Direct-Test 60:147
 - Isomerization 60:147
 - Isopropylbenzene 58:7
 - Kinetic-Modeling 58:7
- Silica-Gel** 61:133
- Silica-Sphere** 44:133
- Silicalite-1** 57:145
- Silicon-Dioxide** 64:265
- Silicone-Based** 58:65
- Silicone-Putty** 51:113
- Simple**
 - Construction 56:B75
 - Electroporator 56:B75
 - Escherichia-Coli 56:B75
 - Gas 56:67
 - Generalization 56:67
 - High-Efficiency 56:B75
 - Low-Cost 56:B75
 - Low-Pressure 56:67
 - Mixture 56:67
 - Strain 56:B75
 - Transformation 56:B75
 - Viscosity 56:67
- Simple-Method**
 - Crude-Oil 45:83
 - Estimation 45:83
 - Fraction 45:83
 - Organic-Liquid 59:181
 - Petroleum 45:83
 - Prediction 59:181
 - Surface-Tension 59:181
 - Viscosity 45:83
- Simplified**
 - Chromatography 64:307
 - Control 50:159
 - Economical-Optimization 64:307
 - Extraction 64:307
 - Fluidized 64:307
 - Ion-Exchange 64:307
 - Model 50:159
 - Modeling 64:307
 - Prediction 50:159
 - Set-Point-Weighting 50:159
 - Whey-Protein 64:307
- Simulation**
 - Activated-Carbon-Column 58:239
 - Adsorption-Process 56:59
 - Anaerobic-Stratified-Biofilm 65:37
 - Application 65:133
 - Artificial 64:63
 - Aspergillus-Niger 52:B1
 - Autothermal-Reactor-System 62:103

- Baffle 59:33
- Batch-Distillation 54:95
- Behavior 59:33
- Biofilter 65:133
- Butanol 46:B11
- Catalytic-Reaction 64:63
- Cell 46:B11
- Cellulose 45:B27
- Comparison 56:59
- Complex 52:B13
- Continuous-Fermentation 46:B11
- Continuous-Stirred-Tank-Reactor 58:239
- Countercurrent 56:59
- Denitrification 65:133
- Development 48:17, 54:95
- Devils-Comb 64:63
- Disk 45:87
- Doughnut-Column 45:87
- Dynamic-Modeling 65:133
- Enzymatic-Hydrolysis 52:B13
- Enzyme 52:B13
- Estimation 58:239
- Ethanol 45:B27
- Experiment 58:239
- Fermentation 45:B27
- Flexible 59:33
- Flotation-Column 59:33
- Flow-Pattern 45:87
- Fractal 64:63
- Free- β -Galactosidase 52:B1
- Generalized-Approach 65:133
- High-Performance-Affinity-Chromatography 65:175
- Hydrogen-Production 62:103
- Hydrolysis 52:B1
- Immobilized 46:B11
- Immobilized- β -Galactosidase 52:B1
- Integration 46:B11
- Intraparticle-Kinetic-Parameter 58:239
- Lactose 52:B1
- Liquid-Liquid-Extraction-Column 45:111
- Mathematical-Modeling 46:B11
- Methane-Production 65:37
- Methanol-Steam 62:103
- Mixture 52:B13
- Model 48:17
- Modeling 46:9, 52:B1, 52:B13, 56:59, 65:37
- Multiple-Steady-State 65:37
- Multistage-Crystallizer 46:9
- Non-Porous-Adsorbent 65:175
- Nonisothermal-Water-Gas-Shift-Reactor 48:17
- Pervaporation 46:B11
- pH-Elution 65:175
- Pneumatically-Pulsed 45:111
- Potato-Pulp 52:B13
- Prediction 65:37
- Reforming 62:103
- Saccharification 45:B27
- Simultaneous 45:B27
- Solid-Liquid-Adsorption 58:239
- Strategy 56:59
- Trend 54:95
- Verification 48:17
- Waste-Water 65:133
- Simultaneous**
 - Cellulose 45:B27
 - Ethanol 45:B27
 - Falling-Film 49:119
 - Fermentation 45:B27
 - Heat-Transfer 49:119
 - Laminar 49:119
 - Liquid 49:119
 - Mass-Transfer 49:119
 - Multicomponent 49:119
 - Reaction 49:119
 - Saccharification 45:B27
 - Simulation 45:B27
- Sinapine** 65:27
- Single**
 - Catalytic-Wall-Reaction 62:51
 - Circulating 45:9
 - Convective-Diffusion 62:51
 - Cyclone-Reactor 45:9
 - Duct 62:51
 - Efficiency 45:9
 - Fluid 62:51
 - Gas 45:9
 - Heat-and-Mass-Transfer 45:9
 - Homogeneous 62:51
 - Inside 62:51
 - Power-Law 62:51
 - Reactor-Wall 45:9
- Single-Drop** 44:27
- Single-Drop-Experiment** 46:137
- Single-Pellet**
 - Behavior 43:11
 - Catalyst 43:11
 - Change 43:11
 - Convective-Coefficient 57:285
 - Deactivation 43:11
 - Determination 57:285
 - Effective-Diffusivity 57:285
 - Mixture 43:11
 - Model 43:11
 - Pore-Size 43:11
 - Pure-Gase 57:285
 - Reaction 43:11
 - Support 43:11
 - Supported-Catalyst 43:11
- Single-Phase-System** 51:B1
- Single-Sphere** 47:187
- Single-Stage-Reactor** 44:53
- Singular** 68:35
- Sinusoidal-Perturbations** 65:165
- Site** 64:265
- Size** 56:B23
- Size-Control** 44:133
- Size-Dependent**
 - Assessment 55:69
 - Crystal-Growth 53:125
 - Crystal-Growth-Rate-Function 55:69
 - Crystallization-Kinetics-Data 55:69
 - Crystallizer 53:125
 - Estimation 53:125
 - Modeled 55:69
 - Rate-Function 53:125
 - System 55:69
- Slab** 61:113
- Slowly-Varying** 60:141
- Sludge** 55:B55
- Slug** 56:B79
- Slugging-Fluidized-Bed** 52:99
- Slurry** 51:99
- Slurry-Bubble-Column**
 - Boundary-Condition 57:299, 57:303
 - Cylindrical-Probe 44:141
 - Determination 54:1
 - Draft-Tube 60:155
 - Gas-Hold-Up 49:151
 - Heat-Transfer 44:141, 52:49, 52:51
 - Hydrodynamics 60:155
 - Immersed 44:141
 - Nonparametric-Method 54:1
 - Outlet 57:299, 57:303
 - Particle 54:1
 - Position 60:155
 - Settling 54:1
 - Solid 57:299, 57:303
 - Three-Phase 44:141
 - Three-Phase-System 49:151
 - Two-Phase-System 49:151
 - Velocity 54:1
- Slurry-Pumparound** 44:119
- Small-Packing** 62:237
- Small-Particle** 47:91
- Sodium** 63:37
- Sodium-Perborate** 50:87
- Sodium-Perborate-Tetrahydrate** 48:119
- Solid**
 - 1-Butene 64:265
 - Acid 64:265
 - Al₂O₃ 64:265
 - Autoclave-Reactor 67:175
 - Axial-Dispersion 64:345
 - Axial-Mixing 44:1
 - Bioreactor 56:B15
 - Boundary-Condition 57:299, 57:303
 - Bronsted-Type 64:265
 - Catalyst 64:265
 - Cell 56:B15
 - Concentration 60:161, 67:175
 - Dissolution 66:57
 - Distribution 60:89, 67:83
 - Draft-Tube 66:105
 - Eddy 67:83
 - Effect 56:B15
 - Entrainment 66:105
 - Flow-Direction 64:345
 - Fluidized 60:89
 - Fluidized-Bed 44:1, 51:135, 66:105
 - Gas 60:89
 - Gas-Solid-Cocurrent-Downflow-System 64:345
 - Gas-Solid-Cocurrent-Upflow-System 64:345
 - High-Pressure 60:89
 - High-Temperature 67:175
 - Influence 67:83
 - Internal-Circulation 66:105
 - Isomerization 64:265
 - Liquid 51:135, 67:83
 - Liquid-Solid-Flow 67:83
 - Mass-Transfer 66:57
 - Measurement 60:161
 - Mixed-Oxide 64:265
 - Movement 51:135
 - Non-Maintained 67:83
 - Outlet 57:299, 57:303
 - Oxygen-Transfer 56:B15
 - Particle 51:135, 56:B15
 - Particle-Size 60:89
 - Physical-Presence 56:B15
 - Presence 67:83
 - Relationship 64:265
 - Segregation 60:89
 - Silicon-Dioxide 64:265
 - Site 64:265
 - Slurry-Bubble-Column 57:299, 57:303
 - Staying-Time 67:83
 - Surface-Active 64:265
 - Three-Phase-Reactor 60:161
 - Titanium-Dioxide 64:265
 - Turbulent 44:1
 - Ultrasonic-Measurement 67:175
 - Ultrasonic-Technique 60:161
 - Wide 60:89
 - Zirconium-Dioxide 64:265
- Solid-Fluid-Flow** 43:49
- Solid-Liquid-Adsorption**
 - Activated-Carbon-Column 58:239
 - Adsorbent 51:159
 - Continuous-Stirred-Tank-Reactor 58:239
 - Estimation 58:239
 - Experiment 58:239
 - Heterogeneity 51:159
 - Intraparticle-Kinetic-Parameter 58:239
 - Modeling 51:159
 - Simulation 58:239
- Solid-Liquid-Dispersion** 49:141
- Solid-Liquid-Mass-Transfer** 52:131

- Solid-Liquid-Mixing** 56:101
Solid-Solid-Dispersion 49:141
Solid-Phase 48:83
Solid-State
 · Amyloglucosidase 51:B17
 · Bed 51:B17
 · Depth 51:B17
 · Different 51:B17
 · Fermentation 51:B17, 60:189, 60:199
 · Heat-Transfer 60:199
 · Inert-Support 60:189
 · Level 51:B17
 · Mathematical-Model 60:189
 · Multidimensional 60:199
 · Mycelial-Fungi 60:189
 · Temperature-Variation 51:B17
 · Transient 60:199
Solid-State-Fermentation 46:B53
Solid-Surface 64:85
Solubility
 · Alcohol 43:25
 · Aliphatic-Ether 43:25
 · Alkanolamine 48:31
 · Carbon-Dioxide 43:25, 52:55
 · Cryogenic-Liquid 43:25
 · Dinitrogen-Oxide 48:31
 · Mixed-Solvent 48:31
 · Nitrous-Oxide 43:25
 · Normal-Paraffin 52:55
 · Water 43:25
Solution
 · Absorption 66:123
 · Cadmium 53:183
 · Calcium-Sulfite 66:123
 · Chelated 53:183
 · Diffusivity 61:7
 · Double-Salt 52:89
 · Evaluation 61:7
 · Homogeneous 64:215
 · Inversion 61:7
 · Ion-Exchange 61:7
 · Kinetic-Behavior 53:183
 · Magnesium-Chloride-Rich 52:89
 · Magnesium-Sulfate 52:89
 · Mass-Transfer 53:183
 · Model 66:123
 · Multicomponent 64:215
 · NMR 64:215
 · Oxygen 66:123
 · Potassium-Sulfate 52:89
 · Reaction-Rate 61:7
 · Seawater 52:89
 · Sucrose 61:7
 · Vanadium-Oxide 64:215
Solution-Method 50:79
Solvent 55:61
Solvent-Extraction
 · Carbon-Dioxide 61:227
 · Comparison 61:227
 · Conventional 61:227
 · Extraction 61:227
 · Grape 61:227
 · Liquid 61:227
 · Miscibility-to-Extraction-Temperature-Ratio 60:169
 · Oil 61:227
 · Overall-Processing 60:169
 · Recovery 61:227
 · Refining-Power 60:169
 · Seed 61:227
 · Selectivity 60:169
 · Solvent-Index 60:169
 · Supercritical 61:227
Solvent-Index 60:169
Sonochemical-Reactor 66:21
Soot 64:295
Sorption
 · Anionic-Species 66:85
 · Blend 47:63
 · Hydrus-Tin-Dioxide 66:85
 · Polyarylate 47:63
 · Polycarbonate 47:63
 · Sulfur-Dioxide 47:63
 · Transport 47:63
Souder-Method 51:41
Sound 66:131
South-Africa 54:ix
Soybean-Oil 51:B51
Space-Time-Trajectory 47:105
Sparged 67:71
Spatiotemporal-Dynamics 64:191
Specific-Energy 57:295
Speed
 · Air-Water-Flow 66:131
 · Biological-Batch-Reactor 56:B43
 · Cod 56:B43
 · Impeller 56:B43
 · Kinetics 56:B43
 · Measurement 66:131
 · Reduction 56:B43
 · Sound 66:131
 · Submergence 56:B43
Sphere 59:111
Spherical
 · 1-Propanol 51:129
 · Alkoxide 55:93
 · Controlled 51:129, 55:93
 · Fine 51:129, 55:93
 · High-Temperature-Range 55:93
 · Hydrolysis 51:129, 55:93
 · Particle 51:129, 55:93
 · Synthesis 51:129, 55:93
 · Tetrabutoxide 51:129
 · Zirconia 51:129, 55:93
 · Zirconium 51:129, 55:93
Spherical-Matrix 46:B21
Spherical-Particle 44:B41
Spiral 62:89
Spiral-Element 56:51
Spiral-Fin 50:169
Spout-Diameter 64:353
Spouted-Bed
 · Bidimensional 47:135, 50:143
 · Conical 51:45, 51:53, 56:19, 62:113
 · Contactor 51:45
 · Cylindrical-Geometry 64:353
 · Dead-Zone 64:353
 · Expansion 51:45
 · Flat-Base 55:27
 · Gas-Flow 56:19
 · Gas-Hold-Up 47:135, 50:143
 · Geometry 62:113
 · Hydrodynamics 55:27, 62:113
 · Influence 62:113
 · Pressure-Drop 51:53
 · Section 62:113
 · Shallow 62:113, 64:353
 · Simplified-Model 56:19
 · Spout-Diameter 64:353
 · Three-Phase 50:143
 · Two-Phase 47:135
Spray-Column 46:B75
Spray-Drying 58:123
Stability
 · Acidity 64:255
 · Analysis 50:59, 68:41
 · Aqueous 67:97
 · Characteristics 55:B47
 · Chemical-Vapor-Deposition-Reactor 54:137
 · Composite 50:59
 · Composite-Phase 50:59
 · Compressible 54:137
 · Continuous-Stirred-Tank-Bioreactor 55:B47, 62:67
 · Degrading 62:67
 · Development 68:7
 · Dispersion 67:97
 · Dynamic-Control 68:41
 · Energy-Density 50:59
 · Fed 55:B47
 · Fluid 54:137
 · Fluidization 68:7
 · Fluidized-Bed 68:7
 · Horizontal 54:137
 · Influence 67:97
 · Inhibitory-Substrate 55:B47
 · Magnetized-Fluidized-Bed 50:59
 · Mesoporous 64:255
 · Mini-Tapered 68:7
 · Molecular-Sieve 64:255
 · Neural-Network 68:41
 · Nonlinear-System 68:41
 · Optimal-Structure 68:41
 · Particle 68:7
 · pH 67:97
 · Phenol 62:67
 · Pore-Size 64:255
 · Range 62:67
 · Rheology 67:97
 · System 68:7
 · Temperature 67:97
 · Thermogravimetric-Analyzer 68:7
 · Titanium-Dioxide 67:97
 · Transport-Property 54:137
 · Upper-Limit 55:B47
 · Variable 54:137
Stable 49:B13
Stable-Catalyst 46:61
Stage 62:143
Stalactite 56:B79
Starch-Suspension 44:B51
State 61:35
State-Estimation 50:B45
Static-Mixer
 · Air-Non-Newtonian-Liquid-Flow 59:277
 · Mixing 63:117
 · Numerical-Simulation 63:117
 · Pressure-Drop 59:277
 · Two-Phase 59:277
Staying-Time 67:83
Steady-State
 · Control 67:103
 · Cross-Flow 61:171
 · Dynamics 67:103
 · Filtration 61:171
 · Flux 61:171
 · Functional-Transformation-Method 51:63
 · Nonlinear-System 67:103
 · Particle 61:171
 · Permeation 61:171
 · Separation 51:63
 · Unstable 67:103
Steady-State-Behavior 53:B47
Steady-State-Flux
 · Calculating 56:27
 · Cutting 56:27
 · Inorganic-Membrane 48:11
 · Microfiltration 48:11
 · Model 48:11, 56:27
 · Oil-Emulsion 56:27
 · Organic-Ultrafiltration-Membrane 56:27
Steam 66:51
Steam-Jet 45:99
Steel 59:287
Stiff 58:109
Stimulus-Response 65:81
Stirred-Bioreactor 51:B11
Stirred-Crystallizer 55:45
Stirred-Reactor
 · Batch 65:187, 65:195
 · Comparison 65:195
 · Enzymatic-Hydrolysis 65:187, 65:195
 · Enzymatic-Kinetics 65:187
 · Hydrolysis 65:187
 · Performance 65:195
 · Protein 65:187, 65:195
 · Torus-Reactor 65:195
 · Wheat 65:187, 65:195

Stirred-Tank

- Absorption 67:131
- Adsorption 52:B71
- Bubbling 67:131
- Carbon-Dioxide 67:131
- Cephalosporin-C 52:B71
- Influence 67:131
- Modeling 52:B71
- Modified 52:B71
- Resin 52:B71
- Surfactant 67:131

Stirred-Tank-Reactor

- Aerated 46:B83
- Approximate-Method 59:293
- Batch 52:107
- Biological-Growth-Process 51:B25
- Bubble-Column-Reactor 53:B35
- Capacitance-Probe 52:1
- Characterization 52:1
- Chemical-Reaction 52:107
- Citric-Acid 53:B35
- Conventional 59:253
- Fast-Reaction 59:293
- Fermentation 46:B83
- Fermentation-Broth 53:B35
- Flow 52:107
- Gas-Bubble 52:1
- Heat-Transfer 46:B83
- Hydrolysis 59:253
- Micromixing 51:B25
- Microwave-Heating 59:253
- Morphological-Property 53:B35
- Mycelial-System 46:B83
- Non-aerated 46:B83
- Order 51:B25
- Prediction 59:293
- Product-Distribution 59:293
- Pulsatile 52:107
- Rheological-Property 53:B35
- Segregation 51:B25
- Submerged 53:B35
- Sucrose 59:253

Storage-Loss-Modulus 67:37**Strain**

- Construction 56:B75
- Electroporator 56:B75
- Escherichia-Coli 56:B75
- Experimental-Data 65:99
- Heated 65:99
- High-Efficiency 56:B75
- Inactivation 65:99
- Kinetic-Model 65:99
- Low-Cost 56:B75
- Simple 56:B75
- Strawberry-Product 65:99
- Thermal 65:99
- Transformation 56:B75
- Yeast 65:99

Strategy

- Adsorption-Process 56:59

- Biocatalytic-Transformation 51:B1
- Biphasic-System 51:B1
- Chemical-Equilibrium-Analysis 51:B1
- Comparison 56:59
- Competing-Reaction 61:41
- Continuous-Transport 53:B1
- Cost 61:41
- Countercurrent 56:59
- Design 53:B1
- Immobilized-Enzyme 53:B1
- Influence 61:41
- Medium 51:B1
- Modeling 56:59
- Process-Optimization 53:B1
- Protein 61:41
- Reactor 53:B1
- Refolding 61:41
- Simulation 56:59
- Single-Phase-System 51:B1

Strawberry-Product 65:99**Stress 53:B41****Stretching 67:65****Stripping 43:B67****Strontium-Chloride 49:167****Structural-Property 66:171****Structure**

- Axial-Dispersion 52:63
- Core-Annulus 68:51
- Description 61:73
- Different 52:63
- Fixed-Bed 52:63
- Fluidized-Bed 61:73, 68:51
- Global 61:73
- Liquid-Solid-Circulating 68:51
- Liquid-Flow 52:63
- Local 61:73
- Metallic-Foam 52:63
- Model 68:51
- Modeling 61:73
- Packed 52:63
- Radial-Flow 68:51
- Reticulated 52:63
- Turbulent 61:73

Structure-Analysis 56:187**Structured**

- Characteristics 58:251
- Corrugated-Sheet 53:55
- Distribution 53:55
- Gas-Flow 53:55
- Liquid-Side 58:251
- Mass-Transfer 58:251
- Measurement 53:55
- Modeling 53:55
- Packing 53:55, 58:251

Subcritical-Mixture 55:115**Subcritical-Range 52:93****Sublimation 62:13****Submerged**

- Acetobacter-Aceti 54:B15
- Bubble-Column-Reactor 53:B35

- Citric-Acid 53:B35
- Culture 54:B15
- Fermentation-Broth 53:B35
- Growth 54:B15
- Kinetic-Model 54:B15
- Morphological-Property 53:B35
- Rheological-Property 53:B35
- Stirred-Tank-Reactor 53:B35

Submergence 56:B43**Subsequent 65:1****Substrate**

- Consumption 62:149
- Effectiveness-Factor 62:149
- Gas 59:195
- Hollow-Fiber-Biofilm-Reactor 62:149
- Limitation 59:195
- Mass-Transfer 59:195
- Maximum 62:149
- Microbial-System 59:195
- Uncoupling 59:195

Substrate-Inhibition 65:117**Sucrose**

- Continuous-Crystallizer 46:B35
- Conventional 59:253
- Crystal-Size-Distribution 46:B35
- Diffusivity 61:7
- Evaluation 61:7
- Hydrolysis 59:253
- Inversion 61:7
- Ion-Exchange 61:7
- Microwave-Heating 59:253
- Monte-Carlo-Simulation 46:B35
- Reaction-Rate 61:7
- Solution 61:7
- Stirred-Tank-Reactor 59:253

Sugar 43:B1**Sugar-Juice-Softening 43:B53****Suitable 66:35****Sulfide 63:37****Sulfur-Dioxide**

- Absorption 51:99
- Blend 47:63
- Limestone 51:99
- Polyarylate 47:63
- Polycarbonate 47:63
- Slurry 51:99
- Sorption 47:63
- Transport 47:63

Sulfur-Promoted 67:199**Sulphur-Dioxide**

- Calcium 66:171
- Fly-Ash 66:171
- Hydroxide 66:171
- Maximum 66:171
- Mixture 66:171
- Oxidation 43:121
- Removal 66:171
- Steady-State-Model 43:121

- Structural-Property 66:171
- Trickle-Bed-Reactor 43:121
- Yield 66:171

Supercritical 61:227**Supercritical-Fluid-Extraction 46:B53****Support**

- Behavior 43:11
- Catalyst 43:11, 57:273, 64:203
- Change 43:11
- Copper(II) 57:273
- Deactivation 43:11
- γ -Alumina 57:273
- Industrial 57:273
- Intrinsic-Kinetics 57:273
- Methane 57:273
- Mixture 43:11
- Model 43:11
- Oxidation 57:273
- Oxide 57:273, 64:203
- Pore-Size 43:11
- Preparation 64:203
- Reaction 43:11
- Recent-Advances 64:203
- Single-Pellet 43:11
- Supported-Catalyst 43:11

Supported

- Catalytic-Property 64:247
- Europium 57:253
- Extraction 57:253
- Heteropolyacid 64:247
- Liquid 57:253
- Membrane 57:253
- Mobile-Carrier 57:253
- Preparation 64:247
- Salt 64:247
- Trivalent 57:253

Supported-Catalyst

- Behavior 43:11
- Catalyst 43:11
- Change 43:11
- Cyclohexane 50:165
- Cyclohexene 50:165
- Deactivation 43:11
- Dehydrogenation 50:165
- Mixture 43:11
- Model 43:11
- Nickel 50:165
- Platinum 50:165
- Pore-Size 43:11
- Reaction 43:11
- Single-Pellet 43:11
- Support 43:11

Surface 59:187**Surface-Active 64:265****Surface-Active-Agent 65:263****Surface-Diffusivity 43:41****Surface-Tension**

- Air-Water-Pipe-Flow 48:197
- Atmospheric-Condition 48:197
- Flow-Pattern 48:197
- Hold-Up 48:197

- Horizontal 48:197
- Organic-Liquid 59:181
- Prediction 59:181
- Pressure-Drop 48:197
- Simple-Method 59:181
- Surfactant** 67:131
- Suspended-Growth-System** 44:B15
- Suspension**
 - Agitated 62:23
 - Application 65:21
 - Breakage 62:23
 - Concentration 65:21
 - Critical-Condition 55:45
 - Cross-Flow 60:31
 - Dense 64:99
 - Dilute 60:31
 - Draft-Tube 59:273
 - Floc 62:23
 - Fractal 64:99
 - Input 51:29
 - Internal-Fouling 60:31
 - Latex 60:31
 - Liquid 62:23
 - Low-Frequency 65:145
 - Membrane 60:31
 - Microporous-Filtration 60:31
 - Mini-Hydrocyclone 65:21
 - Mixing 59:273
 - Necessary 51:29
 - Power 51:29
 - Rheological-Modeling 64:99
 - Rotating-Mixer 62:23
 - Saccharomyces-Cerevisiae 65:145
 - Scale-Up 51:29
 - Stirred-Crystallizer 55:45
 - Stirred-Vessel 51:29
 - Tall-Vessel 59:273
 - Temperature 65:145
 - Thermo-Ultrasonication 65:145
 - Ultrasonic-Power 65:145
 - Vibrating-Mixer 62:23
 - Yeast 65:21
- Suspension-Culture** 57:B31
- Swelling** 55:B35
- Sylvinite** 67:1
- Synergy** 59:315
- Synthesis**
 - 1-Propanol 51:129
 - 2-Propyl-Pentane-Nitrile 59:121
 - Aerosol 64:239
 - Alkoxide 55:93
 - Bubbling-Bed-Reactor 66:193
 - Catalyst 64:225
 - Catalytic-Partial-Oxidation 66:193
 - Cerium-Oxide 64:225
 - Characteristics 64:225
 - Characterization 64:239
 - Controlled 51:129, 55:93
 - Copper-Modified 64:239
 - Decomposition 64:239
 - Electrochemical-Reactor 53:137
 - Experimental-Study 66:193
 - Fed-Batch-Culture 65:219
 - Fine 51:129, 55:93
 - Fungal 65:219
 - Gas 66:193
 - Goethite 59:287
 - Heterogeneously-Catalyzed 66:181
 - High-Temperature 64:239
 - High-Temperature-Range 55:93
 - Higher-Alcohol 64:239
 - Hydrolysis 51:129, 55:93
 - Kinetics 53:137, 57:61, 58:101
 - Liquor 59:287
 - Low-Pressure 58:101
 - Mathematical-Model 59:287
 - Mathematical-Treatment 57:61
 - Methane 66:193
 - Methanol 58:101
 - Methyl-tert-Butyl-Ether 67:199
 - N,N-Dialkylhydrazine 57:61
 - Nanocrystalline 64:225
 - Nonstoichiometric 64:225
 - Optimization 65:219
 - Oxyprecipitation 59:287
 - Particle 51:129, 55:93
 - Percolation 53:137
 - Pickling 59:287
 - Poly-(18-Dibenzo-6-Crown) 53:137
 - Polygalacturonase 65:219
 - Porous-Electrode 53:137
 - Process 59:121, 64:239
 - Pulsed 53:137
 - Raschig-Process 57:61
 - Reactive-Distillation-Process 66:181
 - Residue-Curve-Map 66:181
 - Saccharomyces Cerevisiae 65:219
 - Spherical 51:129, 55:93
 - Steel 59:287
 - Sulfur-Promoted 67:199
 - Tetrabutoxide 51:129
 - Thermodynamics 58:101
 - Ultrasonic-Irradiation 59:121
 - Zinc-Chromite 64:239
 - Zirconia 51:129, 55:93
 - Zirconium 51:129, 55:93
 - Zirconium-Dioxide 67:199
- System**
 - Aqueous-Solution 46:1
 - Assessment 55:69
 - Attainable-Region 54:175
 - Carbon-Dioxide 46:1, 66:217
 - Chemical-Reaction 46:1
 - Correlation 66:217
 - Corresponding-States 66:217
 - Crystal-Growth-Rate-Function 55:69
 - Crystallization-Kinetics-Data 55:69
 - Desorption 46:1
 - Development 68:7
 - Fluidization 68:7
 - Fluidized-Bed 68:7
 - Hydrocarbon 66:217
 - Mini-Tapered 68:7
 - Mixing 54:175
 - Modeled 55:69
 - Multiple-Rate-Process 54:175
 - Optimal-Structure 54:175
 - Particle 68:7
 - Potassium-Carbonate 46:1
 - Reactor 54:175
 - Size-Dependent 55:69
 - Stability 68:7
 - Thermogravimetric-Analyzer 68:7
 - Vapor-Liquid-Equilibrium 66:217
- System-Design** 61:1
- Tangential** 52:137
- Tank**
 - Agitated 63:53
 - Evaporation-Loss 55:61
 - Multiple-Turbine 63:53
 - Solvent 55:61
 - Transitional-Mixing 63:53
- Tank-Electrolyzer** 50:109
- Tannic-Acid** 52:37
- Technique**
 - Active 53:13
 - Adsorption 65:81
 - Adsorption-Data 65:81
 - Application 56:127
 - Calcium-Alginate 65:81
 - Catalyst 53:13
 - Chemical-Vapor-Deposition 53:13
 - Column 65:81
 - Copper 65:81
 - Determination 57:67
 - Dynamic-Approach 65:81
 - Electrical-Tomography 56:127
 - Engineering 56:127
 - Evaluation 65:81
 - Gas-Absorption 57:67
 - Immobilized 65:81
 - Mass-Transfer-Coefficient 57:67
 - Modeling 53:13
 - Moment-Analysis 65:81
 - Packed-Bed 65:81
 - Packed-Column 57:67
 - Phase 53:13
 - Physical-System 57:67
 - Preparation 53:13
 - Process 56:127
 - Profile 53:13
 - Stimulus-Response 65:81
 - Zoogloea-Ramigera 65:81
- Technology** 56:11
- Temperature**
 - 1,2-Ethandiol 52:41
 - 2-Methoxyethanol 52:41
 - 2nd-Virial-Coefficient 56:73
 - Agitated-Reactor 47:33
 - Analysis 47:105
 - Aqueous 67:97
 - Binary-Mixture 52:41
 - Butanol 65:159
 - Catalyst 47:105
 - Characteristics 54:63
 - Combined 47:105
 - Constant 47:105
 - Conversion 47:105
 - Deactivation 51:167, 65:159
 - Decay 47:105
 - Dependence 52:31, 56:73
 - Development 65:27
 - Different 52:41
 - Dispersion 67:97
 - Elevated 54:63
 - Elevated-Pressure 47:33
 - Enzymatic-Transformation 65:27
 - Ethanol 54:63
 - Exit 47:105
 - Fixed-Bed-Reactor 47:105
 - Gas 47:33, 54:63
 - Heat-Capacity 52:31
 - Immobilized 65:159
 - Influence 67:97
 - Kinematic-Viscosity 52:41
 - Lipozyme 65:159
 - Liquid 52:31
 - Low-Frequency 65:145
 - Mass-Transfer 54:63
 - Mass-Transfer-Characteristics 47:33
 - Methanol 54:63
 - Model 65:27
 - Molecular-Structure 52:31
 - Normal-Decane 47:33
 - Oxidase 65:27
 - Palliate 51:167
 - Parallel-Reaction 51:167
 - Parametric-Study 51:167
 - pH 65:27, 67:97
 - Polyphenol 65:27
 - Pressure 54:63
 - Rheology 67:97
 - Saccharomyces-Cerevisiae 65:145
 - Series-Parallel-Reaction 51:167
 - Sinapine 65:27
 - Space-Time-Trajectory 47:105
 - Stability 67:97
 - Suspension 65:145
 - Thermo-Ultrasonication 65:145

- Time-Sequence 51:167
- Titanium-Dioxide 67:97
- Trametes-Versicolor 65:27
- Ultrasonic-Power 65:145
- Water-Content 65:159
- Temperature-Effect** 46:B69
- Temperature-Profile** 49:177
- Temperature-Ramp** 54:35
- Temperature-Variation** 51:B17
- Termolecular-Reaction** 66:231
- Ternary-Mixture** 59:51
- Ternary-System** 44:113
- Terpine** 50:115
- Terpolymer** 63:19
- Tertiary-Amine** 53:107
- Test** 67:65
- Test-Liquid** 48:129
- Tetrabutoxide** 51:129
- Tetraethyl-Orthosilicate** 44:133
- Their** 46:35
- Theoretical-Analysis**
 - Backmixing 48:71
 - Bulk-Copolymerization 48:71
 - Dynamics 48:71
 - Experimental-Study 47:155
 - Gel-Effect 48:71
 - Grid-Generated 47:155
 - Influence 48:71
 - Micromixing 47:155
 - Rate-Parameter 48:71
 - Tubular-Reactor 48:71
 - Turbulence 47:155
- Theoretical-Approach** 49:B23
- Theoretical-Study**
 - Aerosol 58:109
 - Analysis 60:55
 - Balance 60:55
 - Cocurrent 63:93
 - Cross-Flow-Filtration 60:55
 - Cylindrical-Collector 58:109
 - Deposition 58:109
 - Fibrous-Particle 58:109
 - Flexible 58:109
 - Force 60:55
 - Hydrodynamics 63:93
 - Mass-Transfer 63:93
 - Packed-Column 63:93
 - Stiff 58:109
 - Transient 60:55
- Theory** 49:1
- Thermal**
 - Chemical-Vapor-Deposition-Reactor 57:39
 - Configuration-Factor 45:75
 - Determination 45:75
 - Experimental-Data 65:99
 - Heat-Transfer 45:75
 - Heated 65:99
 - Horizontal 57:39
 - Hot-Wall 57:39
 - Inactivation 65:99
 - Kinetic-Model 65:99
 - Low-Pressure 57:39
 - Modeling 57:39
 - Monte-Carlo-Method 45:75
 - Radiative 45:75
 - Strain 65:99
 - Strawberry-Product 65:99
 - Tubular 57:39
 - Yeast 65:99
- Thermal-Conductivity**
 - Estimation 48:211
 - Hydrated 61:133
 - Pure-Liquid 48:211
 - Silica-Gel 61:133
- Thermal-Conductivity-Measurement** 44:43
- Thermal-Measurement** 49:11
- Thermo-Ultrasonication** 65:145
- Thermodynamic-Equilibrium** 43:B93
- Thermodynamic-Interpretation** 60:1
- Thermodynamics** 58:101
- Thermogravimetric-Analyzer** 68:7
- Thermogravimetry** 47:1
- Thermophilic** 55:B55
- Thin-Layer**
 - Dispersion 62:89
 - Element 62:89
 - Equipped 56:51
 - Evaporator 56:51, 62:89
 - Influence 62:89
 - Liquid 56:51, 62:89
 - Longitudinal 62:89
 - Residence-Time 56:51
 - Spiral 62:89
 - Spiral-Element 56:51
- Thin-Layer-Apparatus** 46:69
- Thin-Layer-Evaporator** 50:149
- Thiophene** 49:45
- Thiophilic-Bacteria** 44:B31
- Thomas-Method| Extended-*** 44:173
- Three-Component-Imaging** 56:175
- Three-Dimensional** 67:153
- Three-Parameter** 67:27
- Three-Phase**
 - Bidimensional 50:143
 - Characteristics 43:67
 - Coalescing-Property 55:1
 - Cylindrical-Probe 44:141
 - Fluidized-Bed 43:67, 55:1
 - Gas-Hold-Up 50:143
 - Heat-Transfer 44:141, 55:1
 - Hold-Up 43:67
 - Hydrodynamics 55:1
 - Immersed 44:141
 - Liquid 55:1
 - Mass-Transfer 55:1
 - Phase 43:67
 - Slurry-Bubble-Column 44:141
 - Spouted-Bed 50:143
- Three-Phase-Fixed-Bed-Reactor** 58:83
- Three-Phase-Reactor** 60:161
- Three-Phase-Sparged-Reactor** 44:11
- Three-Phase-System**
 - Alkylation 53:173
 - $\text{BF}_3\text{H}_3\text{PO}_4$ 53:173
 - Catalyst 53:173
 - Gas-Hold-Up 49:151
 - Naphthalene 53:173
 - Propene 53:173
 - Slurry-Bubble-Column 49:151
 - Two-Phase-System 49:151
- Tie-Line** 60:97
- Time-Dependent** 50:B29
- Time-Domain** 65:213
- Time-Sequence** 51:167
- Titanium-Dioxide**
 - 1-Butene 64:265
 - Acid 64:265
 - Al_2O_3 64:265
 - Aqueous 67:97
 - Bronsted-Type 64:265
 - Catalyst 64:265
 - Dispersion 67:97
 - Influence 67:97
 - Isomerization 64:265
 - Mixed-Oxide 64:265
 - pH 67:97
 - Relationship 64:265
 - Rheology 67:97
 - Silicon-Dioxide 64:265
 - Site 64:265
 - Solid 64:265
 - Stability 67:97
 - Surface-Active 64:265
 - Temperature 67:97
 - Zirconium-Dioxide 64:265
- Titer** 65:87
- Toluene**
 - Ag(I)/Ag(II) 56:1
 - Anodic-Oxidation 56:1
 - Isopyrylation 54:79
 - Kinetics 54:79
 - Mediator 56:1
 - Role 56:1
 - Zeolite-Catalyzed 54:79
- Tomographic-Imaging** 59:71
- Tomographic-Technique** 56:101
- Tomography**
 - Environmental 56:159
 - Process 56:vii, 56:159
 - United-States 56:159
- Tool** 61:241
- Torus-Reactor** 65:195
- Total** 52:115
- Tracer**
 - Estimation 53:193
 - Experiment 53:193
 - Fiber-Optic-Probe 61:179
 - Fixed-Bed 53:193
 - Flow 53:193
 - Fluidized-Bed-Reactor 61:179
 - Kinetic-Parameter 53:193
 - Maldistribution 53:193
 - Modeling 61:179
 - Transport 53:193
 - Turbulent 61:179
- Train** 64:191
- Trajectory** 47:141
- Trametes-Versicolor** 65:27
- Transfer** 53:147
- Transfer-Process** 61:83
- Transformation** 56:B75
- Transient**
 - Analysis 60:55
 - Balance 60:55
 - Cross-Flow-Filtration 60:55
 - Fermentation 60:199
 - Force 60:55
 - Heat-Transfer 60:199
 - Multidimensional 60:199
 - Solid-State 60:199
 - Theoretical-Study 60:55
- Transition-Metal-Promoted** 64:283
- Transitional-Mixing** 63:53
- Transport**
 - Binary-Friction-Model 64:319
 - Blend 47:63
 - Estimation 53:193
 - Experiment 53:193
 - Fixed-Bed 53:193
 - Flow 53:193
 - Inert-Membrane 64:319
 - Kinetic-Parameter 53:193
 - Maldistribution 53:193
 - Modified-Maxwell-Stefan-Model 64:319
 - Polyarylate 47:63
 - Polycarbonate 47:63
 - Sorption 47:63
 - Sulfur-Dioxide 47:63
 - Tracer 53:193
- Transport-Phenomena**
 - Bubble-Column-Reactor 48:141, 48:153
 - Disordered-System 49:1
 - Distillation-Column 57:219
 - Ether-Production 57:219
 - Flow-Pattern 48:141
 - Fuel 57:219
 - Oscillatory 57:219
 - Packed 57:219
 - Pressure-Drop 48:153
 - Reactive 57:219
 - Theory 49:1
 - Vapor-Liquid 57:219
- Transport-Process** 64:21
- Transport-Property** 54:137
- Tray**
 - Downcomer 63:167
 - Efficiency 57:237, 63:167
 - Entrainment 57:237
 - Layout 63:167

- Multicomponent 57:237
- Pattern 63:167
- Trend** 54:95
- Trichoderma-Koningii** 59:315
- Trickle** 60:141
- Trickle-Bed-Reactor** 43:121
- Trickle-Flow**
 - Distributor 48:49
 - Liquid 48:61
 - Liquid-Distribution 48:49
 - Packed-Bed 48:49, 48:61
 - Radial-Spreading 48:61
 - Rational-Description 48:49, 48:61
- Triglyceride** 60:117
- Trivalent** 57:253
- Tryptophan-Synthetase-Subunit** 62:143
- Tube**
 - Boundary-Layer 66:201
 - Cross-Flow 66:201
 - Interaction 66:201
 - Particle-Turbulence 66:201
 - Pumping-Characteristics 66:73
 - Screw-Agitator 66:73
 - Turbulent 66:201
- Tubular**
 - Bubble-Size 67:71
 - Chemical-Vapor-Deposition-Reactor 57:39
 - Flux 67:71
 - Frequency 67:71
 - Gas 67:71
 - Horizontal 57:39
 - Hot-Wall 57:39
 - Low-Pressure 57:39
 - Membrane 67:71
 - Modeling 57:39
 - Permeation 67:71
 - Sparged 67:71
 - Thermal 57:39
 - Ultrafiltration 67:71
- Tubular-Column** 54:23
- Tubular-Reactor**
 - Backmixing 48:71
 - Bulk-Copolymerization 48:71
 - Characteristics 51:7
 - Dynamics 48:71
 - Gel-Effect 48:71
 - Heat-Transfer-Rate 51:7
 - Immobilized-Enzyme-System 58:275
 - Influence 48:71
 - Nonisothermal 58:275
 - Operation 51:7
 - Packed 58:275
 - Rate-Parameter 48:71
 - Theoretical-Analysis 48:71
- Turbulence**
 - Capillary-Gap-Cell 43:107
 - Demarcate 57:261
 - Experimental-Study 47:155
 - Fluidization 57:261
 - Grid-Generated 47:155
 - High 59:153
 - Hydrodynamics 43:107
 - Low-Reynolds-Number 59:153
 - Mass-Transfer 43:107, 59:153
 - Measurement 57:261
 - Micromixing 47:155
 - Model 59:153
 - Onset 57:261
 - Prediction 59:153
 - Promoter 43:107
 - Schmidt-Number 59:153
 - Theoretical-Analysis 47:155
 - Turbulent 59:153
 - Velocity 57:261
- Turbulent**
 - Axial-Mixing 44:1
 - Boundary-Layer 66:201
 - Chemical-Reactor 58:183
 - Cross-Flow 66:201
 - Description 61:73
 - Fiber-Optic-Probe 61:179
 - Fluctuation 53:39
 - Fluidized-Bed 44:1, 61:73
 - Fluidized-Bed-Reactor 61:179
 - Global 61:73
 - High 59:153
 - Interaction 66:201
 - Jet-Flame 53:39
 - Local 61:73
 - Low-Reynolds-Number 59:153
 - Mass-Transfer 59:153
 - Micromixing 58:183
 - Model 59:153
 - Modeling 61:73, 61:179
 - Natural-Gas 53:39
 - OH-Concentration 53:39
 - Particle-Dispersion 66:207
 - Particle-Laden 66:207
 - Particle-Turbulence 66:201
 - Prediction 59:153
 - Round-Jet 66:207
 - Schmidt-Number 59:153
 - Solid 44:1
 - Stochastic-Modeling 66:207
 - Structure 61:73
 - Tracer 61:179
 - Tube 66:201
 - Turbulence 59:153
- Turbulent-Jet** 43:127
- Tuyere** 60:75
- Two-Film-Theory** 60:105
- Two-Phase**
 - Air-Non-Newtonian-Liquid-Flow 59:277
 - Bidimensional 47:135
 - Coaxial 63:11
 - Flow-Measurement 63:59
 - Fluid-System 57:189
 - Gas-Liquid-Flow 45:55
 - Gas-Hold-Up 47:135
 - Geometrical 62:1
 - Hold-Up 45:55
 - Inclined 45:55
 - Jet 63:11
 - Mass-Transfer-Reaction-Coupling 57:189
 - Material 62:1
 - Model 62:1
 - Multicomponent 57:189
 - Oil-Water-Emulsion 63:59
 - Particle-Laden 63:11
 - Porous-Medium 62:1
 - Prediction 45:55
 - Pressure-Drop 59:277
 - Random 62:1
 - Segmental-Orifice-Meter 63:59
 - Spouted-Bed 47:135
 - Static-Mixer 59:277
 - Velocity-Measurement 63:11
 - Wedge-Meter 63:59
- Two-Phase-Extraction** 46:B31
- Two-Phase-Flow**
 - Accumulation-Effect 59:281
 - Analysis 45:137
 - Experimental-Investigation 59:281
 - Gas 59:281
 - Gas-Liquid-Controlling 62:61
 - Gas-Solids-Injector 45:137
 - Liquid 59:281
 - Liquid-Solid-Mass-Transfer 62:61
 - Metering 59:281
 - Orifice 59:281
 - Packed-Bed 62:61
 - Raschig-Ring 62:61
- Two-Phase-System**
 - Gas-Hold-Up 49:151
 - Polyethylene-Glycol-Malto-dextrin-System 46:B75
 - Polymer 46:B75
 - Protein-Extraction 46:B75
 - Slurry-Bubble-Column 49:151
 - Spray-Column 46:B75
 - Three-Phase-System 49:151
- Two-Reactor-Arrangement** 58:1
- Two-Stage** 62:143
- Two-Step** 58:21
- Two-Substrate** 43:B93
- Ultrafiltration**
 - Batch 61:157
 - Bubble-Size 67:71
 - Chaperonin 65:151
 - Enzyme-Refolding 65:151
 - Flux 67:71
 - Frequency 67:71
 - Gas 67:71
 - Membrane 67:71
 - Modeling 61:157
 - Operation-Condition 65:151
 - Permeation 67:71
 - Recycle-System 65:151
 - Sparged 67:71
 - Tubular 67:71
- Ultrafiltration-Membrane-Reactor** 43:B43
- Ultrasonic-Bath** 57:53
- Ultrasonic-Irradiation** 59:121
- Ultrasonic-Measurement** 67:175
- Ultrasonic-Power** 65:145
- Ultrasonic-Technique** 60:161
- Ultrasound-Emitter** 50:27
- Ultrasound-Imaging** 56:183
- Unbaffled** 66:1
- Uncoupling** 59:195
- Unfavorable** 46:B93
- Ungassed-Condition** 67:215
- Uniaxial-Stretching** 51:113
- Unicellular**
 - Cadmium 62:81, 65:13
 - Cell-Surface-Area 65:13
 - Green 62:81
 - Green-Microalgae 65:13
 - Microalgae 62:81
 - Uptake 62:81, 65:13
- Unified-Similarity-Transformation** 50:33
- United-States** 56:159
- Unstable** 67:103
- Unsteady-State** 60:131
- Unstirred** 51:B57
- Upflow** 65:165
- Upper-Limit** 55:B47
- Uptake**
 - Cadmium 62:81, 65:13
 - Cell-Surface-Area 65:13
 - Green 62:81
 - Green-Microalgae 65:13
 - Microalgae 62:81
 - Unicellular 62:81, 65:13
- Value** 46:35
- Vanadium-Oxide** 64:215
- Vapor-Liquid** 57:219
- Vapor-Liquid-Equilibrium**
 - Application 61:27
 - Applied 48:111
 - Calculation 48:111, 61:21, 61:27
 - Carbon-Dioxide 66:217
 - Comparison 61:21
 - Computation 60:1
 - Correlation 66:217
 - Corresponding-States 66:217
 - High-Pressure 60:1, 61:27
 - Hydrocarbon 66:217
 - Model 61:21, 61:27
 - Prediction 55:115, 61:21
 - Semiempirical-Equation-of-State 48:111
 - Subcritical-Mixture 55:115
 - System 66:217
 - Thermodynamic-Interpretation 60:1
- Vapor-Liquid-Separation** 59:51
- Vapor-Pressure** 55:139
- Vaporization** 59:127

- Vaporization- Heat** 59:101
- Variable**
- Chemical-Vapor-Deposition-Reactor 54:137
 - Choice 52:B59
 - Compressible 54:137
 - Control 52:B59
 - Fed-Batch 52:B59
 - Fermentation 52:B59
 - Fluid 54:137
 - Horizontal 54:137
 - Optimization 52:B59
 - Stability 54:137
 - Transport-Property 54:137
- Variable-Density-System** 47:17
- Variation** 58:223
- Variouly-Shaped** 63:1
- Varying-Size** 44:B1
- Vat-Dye** 49:73
- Vector** 64:21
- Velocity**
- A-Priori-Information 56:167
 - Demarcate 57:261
 - Determination 54:1
 - Flow 56:167
 - Fluidization 57:261
 - Imaging 56:167
 - Inclined 56:167
 - Measurement 57:261
 - Modeling 56:167
 - Multiphase-Flow 56:167
 - Nonparametric-Method 54:1
 - Onset 57:261
 - Particle 54:1
 - Profile 56:167
 - Settling 54:1
 - Slurry-Bubble-Column 54:1
 - Turbulence 57:261
- Velocity-Field** 67:139
- Velocity-Measurement** 63:11
- Venturi-Injector** 57:B1
- Venturi-Scrubber**
- Boundary-Layer-Separation 49:55
 - Cylindrical 49:55
 - Design 61:203
 - Diffuser 49:55
 - Dry 61:203
 - Gas-Liquid-Flow 49:55
 - Importance 61:203
 - Modeling 67:9
 - Performance 67:9
 - Pressure-Drop 61:203
 - Section 49:55
- Verification** 48:17
- Vertical-Misalignment** 53:151
- Vertical-Tube** 55:103
- Vessel| Agitated-»**
- Application 48:41
 - Baffle 58:135
 - Equipped 58:135
 - Experimental-Technique 48:41
 - Gas-Bubble 48:41
 - Heat-Transfer 58:135
 - Highly-Viscous-Liquid 48:41
 - Jacketed 58:135
 - Liquid 48:41
 - Mass-Transfer 48:41
 - Measurement 48:41
 - Nonstandard 58:135
- Vessel| Conical-»** 46:15
- Vessel| Large-»** 56:183
- Vessel| Liquid-»** 61:107
- Vessel| Mixing-»**
- Agitator 61:83
 - Axially-Agitated 67:139
 - Gas-Liquid-Dispersion 61:83
 - Hydrodynamic 61:83
 - Macro-Instability 67:139
 - Modified-Rushton-Turbine 61:83
 - Transfer-Process 61:83
 - Velocity-Field 67:139
- Vessel| Stirred-»**
- Computational 59:39
 - Fluid 59:39
 - Input 51:29
 - Mixing 59:39
 - Necessary 51:29
 - Power 51:29
 - Progress 59:39
 - Scale-Up 51:29
 - Suspension 51:29
- Vessel| Tall-»** 59:273
- Vessel| Tapered-»**
- Fluidization» 51:121
 - Slugging-Fluidized-Bed 52:99
- Vibrating-Element** 50:149
- Vibrating-Mixer** 62:23
- Vibratory-Agitator** 61:107
- Virial-Expansion** 46:35
- Viscometer** 45:B49
- Viscosity**
- Alcohol-Solution 60:117
 - Application 60:117
 - Coarse 67:37
 - Crude-Oil 45:83
 - Emulsion 67:37
 - Estimation 45:83
 - Extended-Thomas-Method 44:173
 - Fast-Parallel-Reactions 58:15
 - Fine 67:37
 - Fluorinated-Hydrocarbon 44:173
 - Fraction 45:83
 - Gas 56:67
 - Generalization 56:67
 - Group-Contribution-Method 50:9
 - Influence 47:51, 58:15
 - Krone-Doolittle-Equation 60:117
 - Liquid 44:173, 51:41
 - Liquid-Phase 47:51
 - Low-Pressure 56:67
 - Macedo-Litovitz-Equation 60:117
 - Mass-Transfer-Resistance 47:51
 - Mixture 56:67, 67:37
 - Nonpolar-Liquid 47:163
 - Organic-Liquid 50:9
 - Packed-Column 47:51
 - Petroleum 45:83
 - Phosphorus-Containing-Compound 51:41
 - Prediction 44:173, 50:9, 51:41
 - Product-Distribution 58:15
 - Semitheoretical-Model 47:163
 - Simple 56:67
 - Simple-Method 45:83
 - Souder-Method 51:41
 - Storage-Loss-Modulus 67:37
 - Triglyceride 60:117
- Viscous**
- Airlift-Bioreactor 56:B101
 - Bubble-Growth 63:149
 - Direct-Measurement 47:B35
 - Dynamic-Measurement 47:B35
 - Fermentation-Broth 47:B35
 - Flow 60:141
 - Gas-Liquid-Circulation 56:B101
 - Gas-Hold-Up 47:B35
 - Incline 60:141
 - Mass-Transfer 56:B101
 - Newtonian-Liquid 63:149
 - Non-Newtonian-Fluid 56:B101
 - Non-Newtonian-Liquid 63:149
 - Residual 47:B35
 - Slowly-Varying 60:141
 - Trickle 60:141
- Viscous-Liquid** 47:91
- Visible-Light-Tomography** 56:187
- Voidage** 53:115
- Volatile** 67:45
- Volume** 63:79
- Volumetric** 49:49
- Vortex** 62:175
- Wall** 48:83
- Wall-Reaction** 61:63
- Waste** 55:87
- Waste-Fraction** 56:B37
- Waste-Treatment** 52:B49
- Waste-Water**
- Anaerobic 54:B25
 - Application 65:133
 - Biofilter 65:133
 - Denitrification 65:133
 - Dynamic-Modeling 65:133
 - Fluidized-Bed-System 54:B25
 - Fruit 54:B25
 - Generalized-Approach 65:133
 - Kinetics 54:B25
 - Processing 54:B25
 - Purification 54:B25
 - Simulation 65:133
- Waste-Water-Scrubber-System** 43:B67
- Waste-Water-Treatment**
- Biokinetics 49:B1
 - Dynamic-Modeling 57:B37
 - High-Performance-Compact-Reactor 49:B1
 - Lemna-Gibba 57:B37
 - Plant 57:B37
- Water**
- Alcohol 43:25
 - Aliphatic-Ether 43:25
 - α -Pinene 50:115
 - Amberlite 62:231
 - Carbon-Dioxide 43:25
 - Cryogenic-Liquid 43:25
 - Diffusivity 66:111
 - Distribution 62:231
 - Equilibrium 62:231
 - Hydration 50:115
 - Isobutanol 50:115
 - Kinetic-Modeling 50:115
 - Lemna-Gibba 54:B41
 - Nitrous-Oxide 43:25
 - Organic-Electrolyte 66:111
 - Organic-Solution 62:231
 - Penicillin-G 62:231
 - Phase-Equilibrium 50:115
 - Pollutant 54:B41
 - Removal 54:B41
 - Solubility 43:25
 - Terpene 50:115
- Water-Content** 65:159
- Water-Methanol-Polyol** 66:137
- Wave** 62:175
- Wavy-Walled-Pipe** 55:15
- Wedge-Meter** 63:59
- Wet-Air** 67:115
- Wetted-Butterfly-Valve** 43:B67
- Wheat**
- Batch 65:187, 65:195
 - Comparison 65:195
 - Enzymatic-Hydrolysis 65:187, 65:195
 - Enzymatic-Kinetics 65:187
 - Hydrolysis 65:187
 - Performance 65:195
 - Protein 65:187, 65:195
 - Stirred-Reactor 65:187, 65:195
 - Torus-Reactor 65:195
- Whey-Protein** 64:307
- Wide** 60:89
- Wiped** 59:259
- Wong-Sandler-Mixing-Rule** 67:27
- Wood** 61:233
- Wood-Preservative** 45:B13
- Woodburn-T.** 59:v
- Xanthan-Fermentation** 56:B37
- Xanthan-Gum-Solution**
- Apparent-Yield 53:B41
 - Apparent-Yield-Stress 45:B49

- Estimation 45:B49
- Fermentation-Broth 45:B49
- Flow 59:111
- Low-Concentration 53:B41
- Low-Cost 45:B49
- Non-Viscous-Effect 59:111
- Packed-Bed 59:111
- Sphere 59:111
- Stress 53:B41
- Viscometer 45:B49
- Yeast**
 - Application 65:21
 - Concentration 65:21
 - Experimental-Data 65:99
 - Heated 65:99
 - Inactivation 65:99
 - Kinetic-Model 65:99
 - Mini-Hydrocyclone 65:21
 - Strain 65:99
 - Strawberry-Product 65:99
 - Suspension 65:21
 - Thermal 65:99
- Yeast-Cell-Column**
 - Effectiveness-Factor 49:B23
 - Entrapped 47:B1, 49:B23
 - Ethanol-Production 47:B1
 - Evaluation 49:B23
 - Theoretical-Approach 49:B23
- Yeast-Flocs** 43:B13
- Yield**
 - Aspergillus-Niger 62:215
 - Calcium 66:171
 - Citric-Acid-Production 62:215
 - Determination 62:215
 - Fly-Ash 66:171
 - Hydroxide 66:171
 - Maintenance-Coefficient 62:215
 - Maximum 66:171
 - Membrane-Process 58:175
 - Mixture 66:171
 - Pressure-Driven 58:175
 - Removal 66:171
 - Structural-Property 66:171
 - Sulphur-Dioxide 66:171
- Zeolite**
 - Adsorption 54:115
 - Anaerobic-Digestion 54:B9
 - Biomass 54:B9
 - Cow-Manure 54:B9
 - Cracking 54:115
 - Deactivation 54:115
 - Diffusion 54:115
 - Hexane 54:115
 - Immobilized 54:B9
 - Kinetics 54:B9
 - Mass-Transport 57:155
 - Maxwell-Stefan-Description 57:155
 - Membrane 57:155
 - Mordenite 54:115
 - Oligomerization 54:115
 - Propene 54:115
- Zeolite-Catalyzed** 54:79
- Zero-Order-Limit** 51:B63
- Zinc** 47:B23
- Zinc-Chromite** 64:239
- Zirconia**
 - 1-Propanol 51:129
 - Alkoxide 55:93
 - Controlled 51:129, 55:93
 - Fine 51:129, 55:93
 - High-Temperature-Range 55:93
 - Hydrolysis 51:129, 55:93
 - Particle 51:129, 55:93
 - Spherical 51:129, 55:93
 - Synthesis 51:129, 55:93
 - Tetrabutoxide 51:129
 - Zirconium 51:129, 55:93
- Zirconia-Silica-Sulfate** 64:273
- Zirconium**
 - 1-Propanol 51:129
 - Alkoxide 55:93
 - Controlled 51:129, 55:93
 - Fine 51:129, 55:93
 - High-Temperature-Range 55:93
 - Hydrolysis 51:129, 55:93
 - Particle 51:129, 55:93
 - Spherical 51:129, 55:93
 - Synthesis 51:129, 55:93
 - Tetrabutoxide 51:129
 - Zirconia 51:129, 55:93
- Zirconium-Dioxide**
 - 1-Butene 64:265
 - Acid 64:265
 - Al₂O₃ 64:265
 - Bronsted-Type 64:265
 - Catalyst 64:265
 - Isomerization 64:265
 - Methyl-tert-Butyl-Ether 67:199
 - Mixed-Oxide 64:265
 - Relationship 64:265
 - Silicon-Dioxide 64:265
 - Site 64:265
 - Solid 64:265
 - Sulfur-Promoted 67:199
 - Surface-Active 64:265
 - Synthesis 67:199
 - Titanium-Dioxide 64:265
- Zoogloea-Ramigera**
 - Adsorption 65:81
 - Adsorption-Data 65:81
 - Adsorption-Isotherm 60:181
 - Biosorption 60:181
 - Calcium-Alginate 65:81
 - Characteristics 60:181
 - Column 65:81
 - Comparison 60:181
 - Copper 65:81
 - Dynamic-Approach 65:81
 - Evaluation 65:81
 - Heavy-Metal 60:181
 - Immobilized 65:81
 - Moment-Analysis 65:81
 - Packed-Bed 65:81
 - Stimulus-Response 65:81
 - Technique 65:81